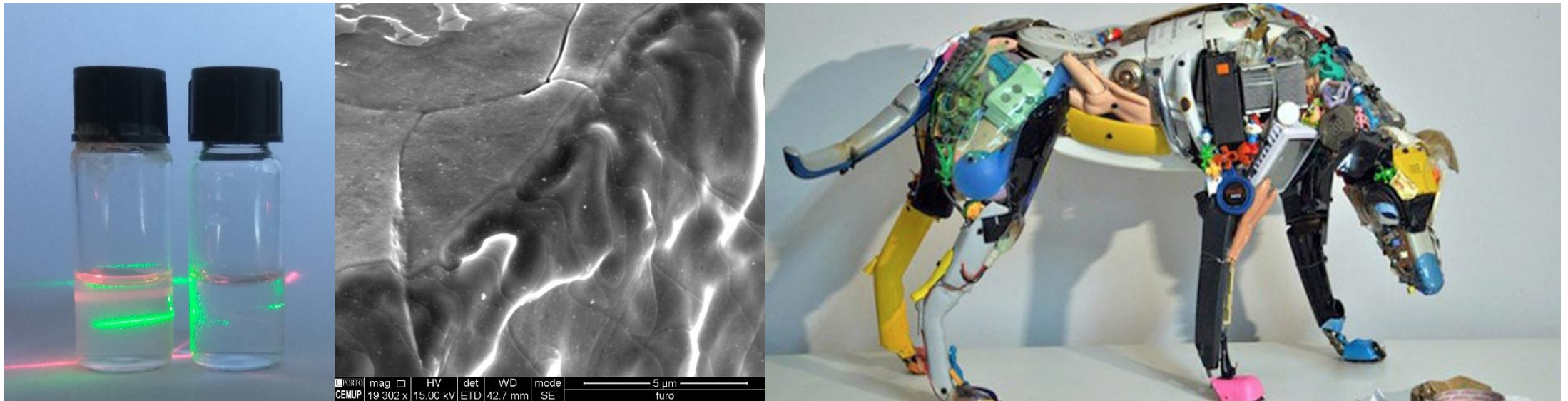


Physical Chemistry

... iremos explorar, refletir, aprender ?..

Area of chemistry concerned with the **application of the techniques and theories of physics** to the study of chemical systems.

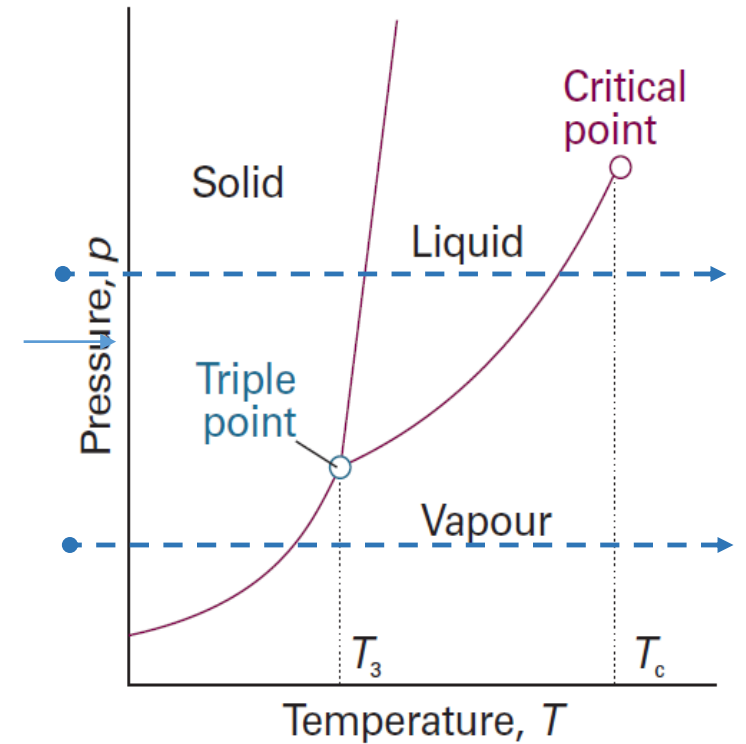
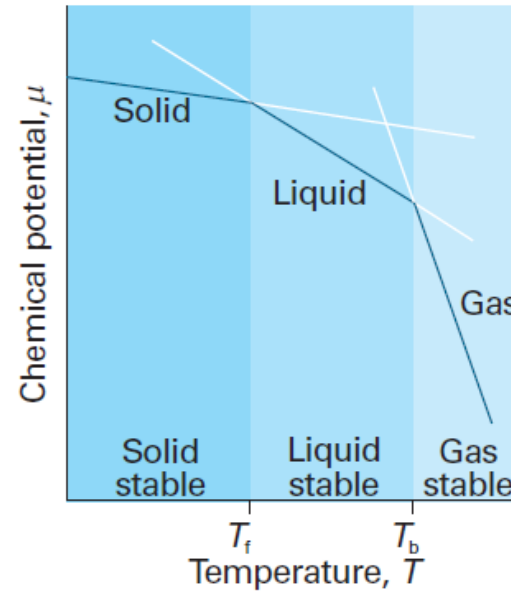
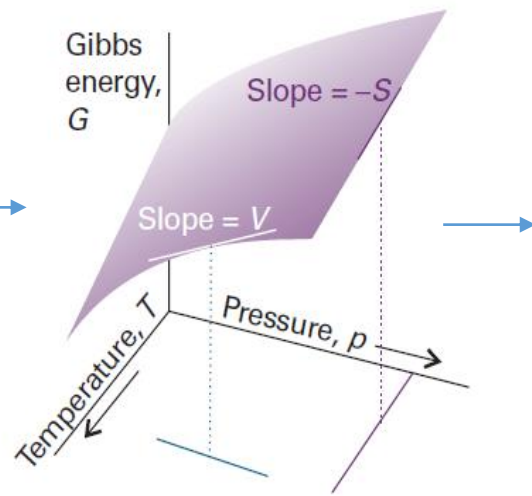
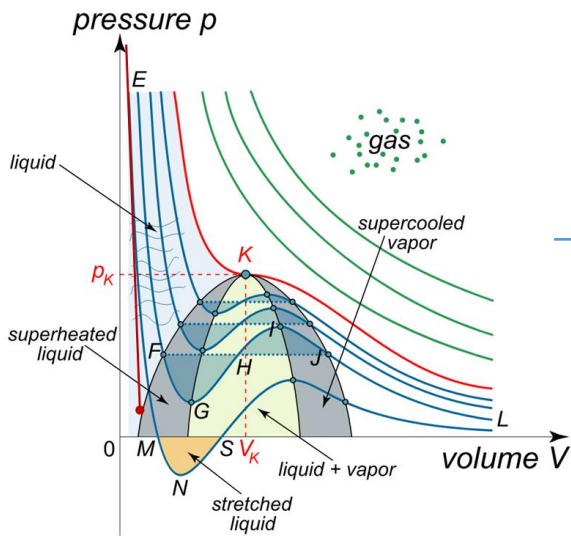


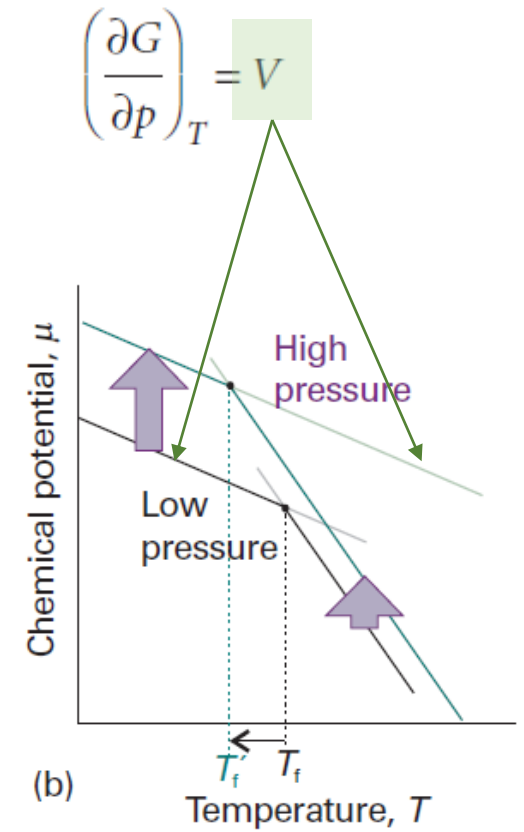
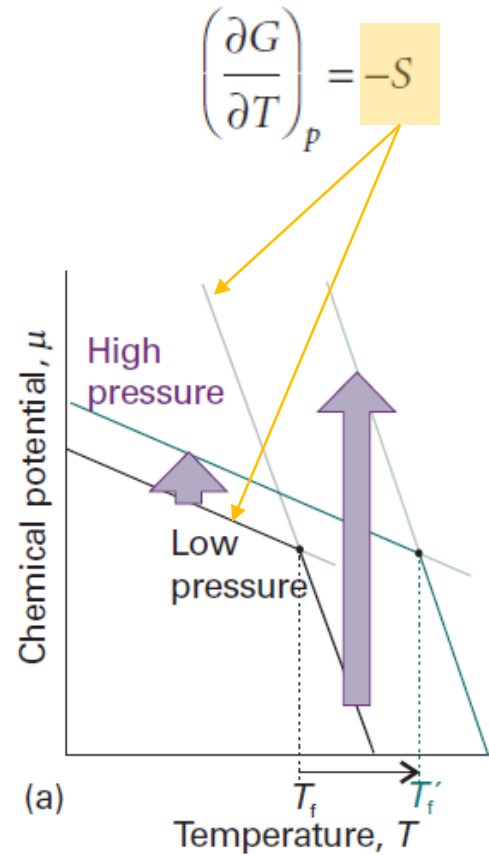
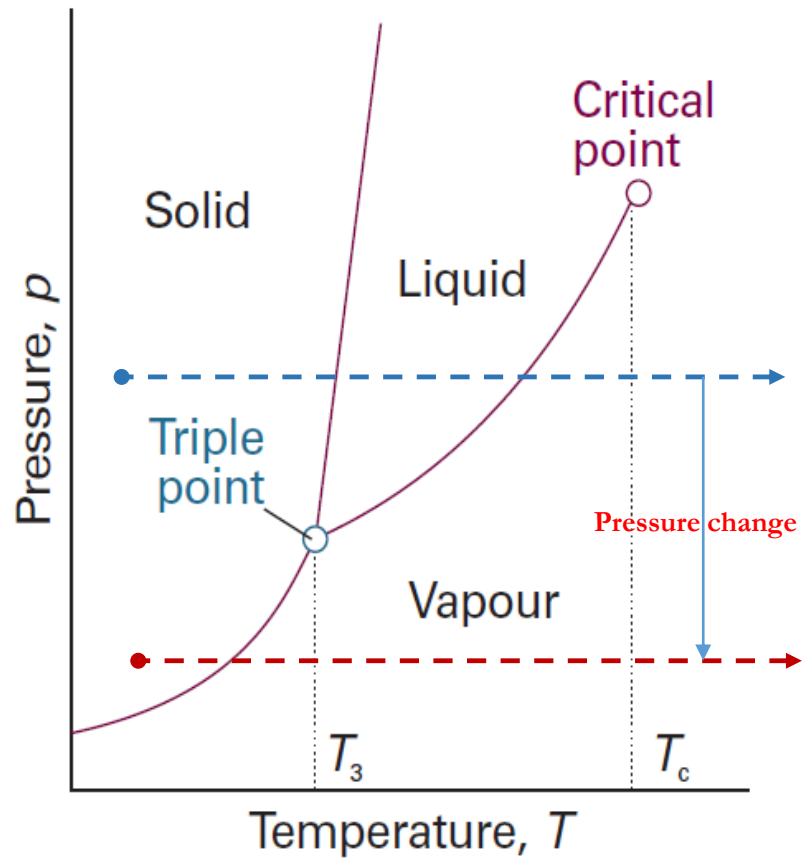
Physical transformations of pure substances

EoS

$$\left(\frac{\partial G}{\partial T}\right)_p = -S$$

$$\left(\frac{\partial G}{\partial p}\right)_T = V$$





$$\left(\frac{\partial G}{\partial T}\right)_p = -S$$

$$\left(\frac{\partial G}{\partial p}\right)_T = V$$

Phase equilibrium !

$$dG = Vdp - SdT$$

$$G_\alpha(p, T) = G_\beta(p, T)$$

$$dG_\alpha(p, T) = dG_\beta(p, T)$$

$$\mu_\alpha(p, T) = \mu_\beta(p, T)$$



$$V_m(\alpha) \qquad V_m(\beta)$$

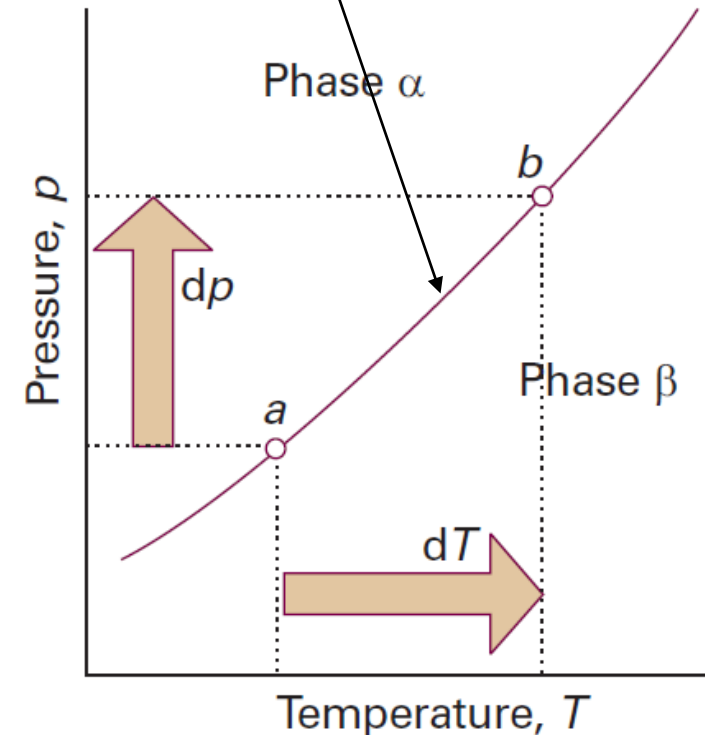
$$S_m(\alpha) \qquad S_m(\beta)$$

$$-S_{\alpha,m}dT + V_{\alpha,m}dp = -S_{\beta,m}dT + V_{\beta,m}dp$$

$$(V_{\beta,m} - V_{\alpha,m})dp = (S_{\beta,m} - S_{\alpha,m})dT$$

Clapeyron equation
Shape of the curve!

$$\frac{dp}{dT} = \frac{\Delta_{\text{trs}} S}{\Delta_{\text{trs}} V}$$



Physical transformations of pure substances

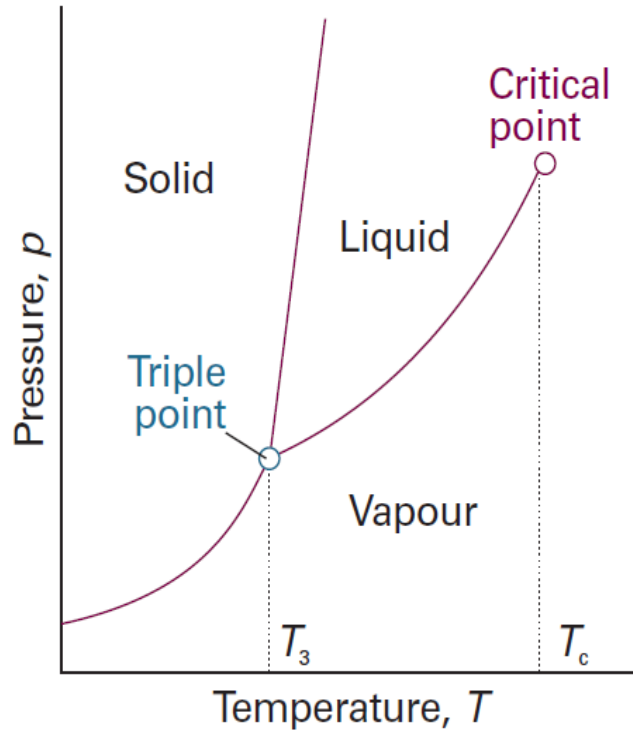
CHAP . #4

$$\frac{dp}{dT} = \frac{\Delta_{\text{trs}} S}{\Delta_{\text{trs}} V}$$

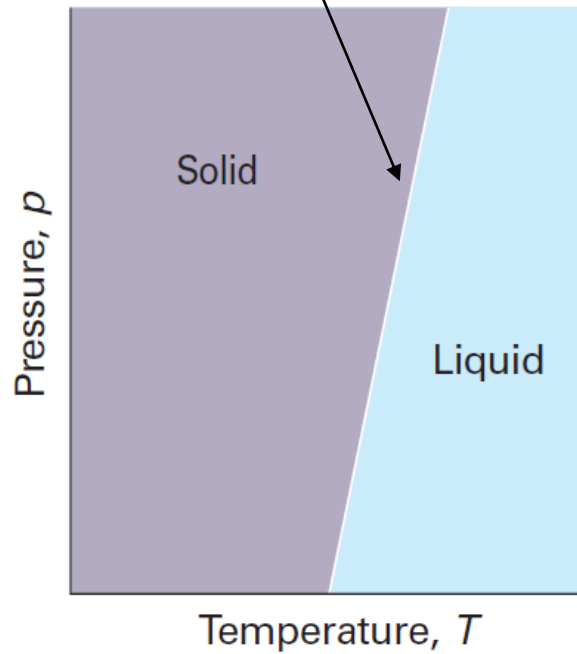
Clapeyron equation

Solid -Liquid ..condensed phases

$$\left(\frac{\partial G}{\partial T}\right)_p = -S \quad \left(\frac{\partial G}{\partial p}\right)_T = V$$



Slope could be **positive** or **negative!!**



$$\frac{dp}{dT} = \frac{\Delta_{\text{trs}} S}{\Delta_{\text{trs}} V} \quad \Delta_{\text{fus}} S = S_m(l) - S_m(s)$$

$$\Delta_{\text{fus}} V = V_m(l) - V_m(s)$$

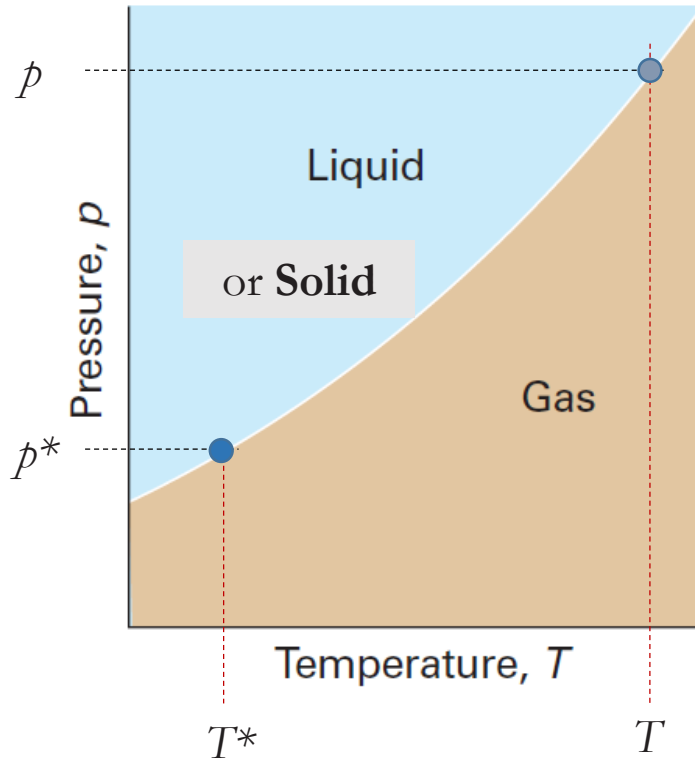
$$\Delta_{\text{fus}} S = \Delta_{\text{fus}} H / T_{\text{fus}}$$

$$\frac{dp}{dT} = \frac{\Delta_{\text{fus}} H}{T \Delta_{\text{fus}} V}$$

$$\Delta_{\text{fus}} V$$

Could be **positive** or **negative!!**

The liquid–vapour boundary



Clapeyron equation

$$\frac{dp}{dT} = \frac{\Delta_{\text{trs}} S}{\Delta_{\text{trs}} V}$$

$$\frac{dp}{dT} = \frac{\Delta_{\text{vap}} H}{T \Delta_{\text{vap}} V}$$

$$\Delta_{\text{vap}} V \approx V_m(\text{g})$$

$$\frac{dp}{dT} = \frac{\Delta_{\text{vap}} H}{T(RT/p)}$$

$$V_m(\text{g}) = RT/p$$

$$\frac{d \ln p}{dT} = \frac{\Delta_{\text{vap}} H}{RT^2}$$

$$\int_{\ln p^*}^{\ln p} d \ln p = \frac{\Delta_{\text{vap}} H}{R} \int_{T^*}^T \frac{dT}{T^2} = -\frac{\Delta_{\text{vap}} H}{R} \left(\frac{1}{T} - \frac{1}{T^*} \right)$$

$$p = p^* e^{-\chi} \quad \chi = \frac{\Delta_{\text{vap}} H}{R} \left(\frac{1}{T} - \frac{1}{T^*} \right)$$

$$\left(\frac{\partial G}{\partial T} \right)_p = -S \quad \left(\frac{\partial G}{\partial p} \right)_T = V$$

Liquid–Vapour and Solid–Vapour phase boundaries

Clausius–Clapeyron equation
(liquid (or solid) / gas)

Gibbs–Helmholtz equation

$$G = H - TS$$

$$\frac{G}{T} = \frac{H}{T} - S$$

$$\left(\frac{\partial G}{\partial T}\right)_p = \frac{H}{T} - dS$$



$$\left(\frac{\partial G}{\partial T}\right)_p = -\frac{H}{T^2}$$

$$\left(\frac{\partial \Delta G}{\partial T}\right)_p = -\frac{\Delta H}{T^2}$$

$$\Delta G = \Delta H - T\Delta S$$

$$\Delta G/T = \Delta H/T - \Delta S$$

$$\left(\frac{\partial \Delta G}{\partial T}\right)_p = -\frac{\Delta H}{T^2}$$

The Gibbs–Helmholtz equation

$$G_m(p) = G_m^\ominus + RT \ln \frac{p}{p^\ominus}$$

$$\Delta G = -RT \ln(p)$$

$$\Delta G/T = -R \ln(p)$$

$$\frac{d \ln p}{dT} = \frac{\Delta_{\text{vap}} H}{RT^2}$$

The liquid–vapour boundary

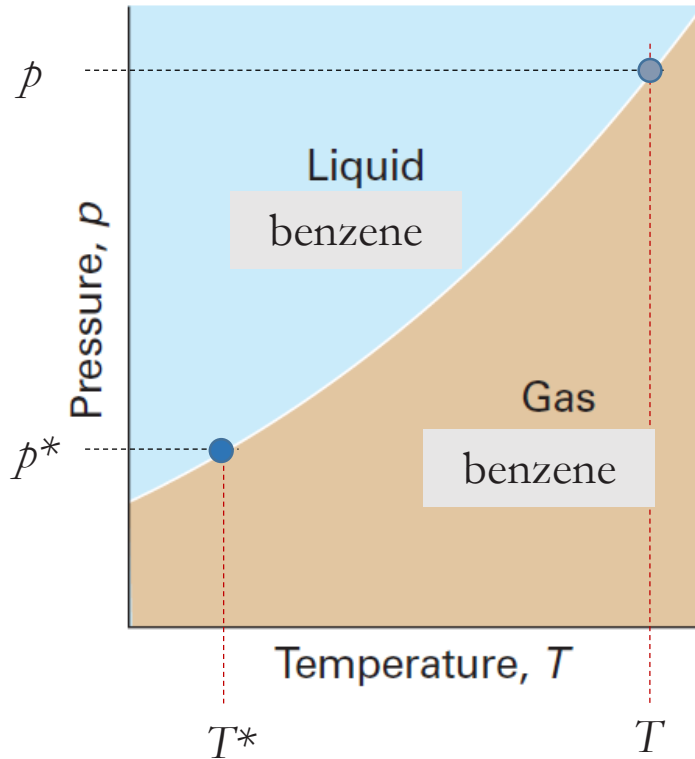


Illustration 4.2 The effect of temperature on the vapour pressure of a liquid

Equation 4.12 can be used to estimate the vapour pressure of a liquid at any temperature from its normal boiling point, the temperature at which the vapour pressure is 1.00 atm (101 kPa). Thus, because the normal boiling point of benzene is 80°C (353 K) and (from Table 2.3), $\Delta_{\text{vap}}H^\ominus = 30.8 \text{ kJ mol}^{-1}$, to calculate the vapour pressure at 20°C (293 K), we write

$$\chi = \frac{3.08 \times 10^4 \text{ J mol}^{-1}}{8.3145 \text{ J K}^{-1} \text{ mol}^{-1}} \left(\frac{1}{293 \text{ K}} - \frac{1}{353 \text{ K}} \right) = \frac{3.08 \times 10^4}{8.3145} \left(\frac{1}{293} - \frac{1}{353} \right)$$

with $p^* = 101 \text{ kPa}$. (1 atm)

The result is 12 kPa. The experimental value is 10 kPa. (0.1 atm)

$$\frac{d \ln p}{dT} = \frac{\Delta_{\text{vap}}H}{RT^2}$$

Clausius–Clapeyron equation
(liquid (or solid) /gas)

$$\int_{\ln p^*}^{\ln p} d \ln p = \frac{\Delta_{\text{vap}}H}{R} \int_{T^*}^T \frac{dT}{T^2} = -\frac{\Delta_{\text{vap}}H}{R} \left(\frac{1}{T} - \frac{1}{T^*} \right) \quad p = p^* e^{-\chi} \quad \chi = \frac{\Delta_{\text{vap}}H}{R} \left(\frac{1}{T} - \frac{1}{T^*} \right)$$

First & Second ORDER Phase transitions

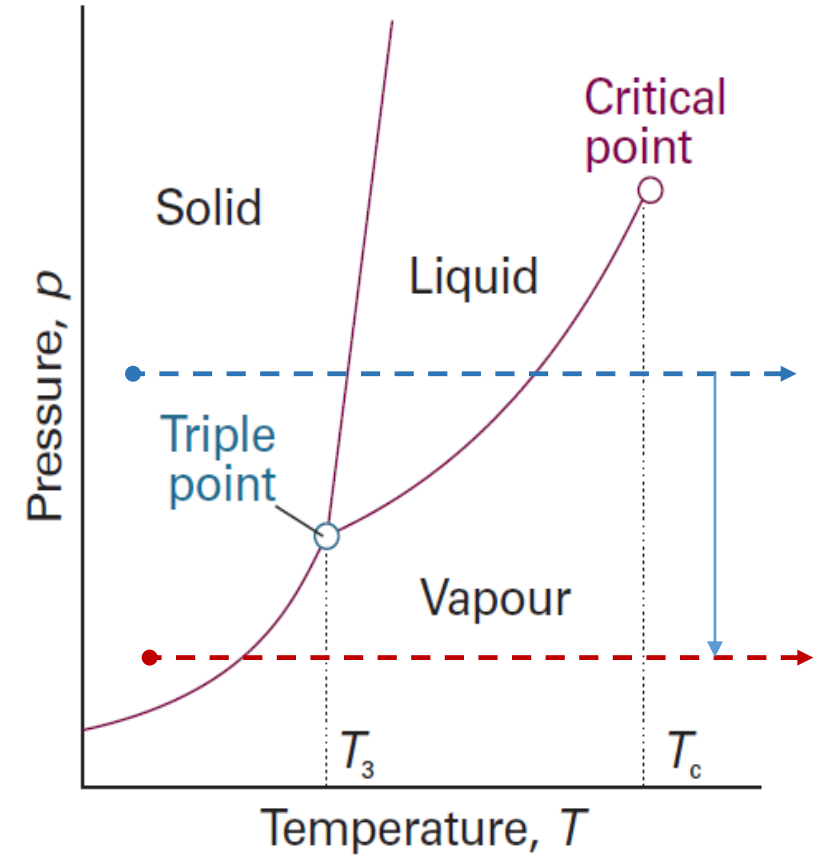
First-order phase transition

A transition for which the first derivative of the μ , with respect to *temperature is discontinuous*

e.g... fusion, vaporization ..etc

Second-order phase transition the first derivative of μ , with respect to temperature is continuous but its second derivative is discontinuous.

e.g... some solid- solid ..etc



First & Second ORDER Phase transitions

First-order phase

e.g... fusion, vaporization ..etc

Second-order

e.g... some solid- solid ..etc

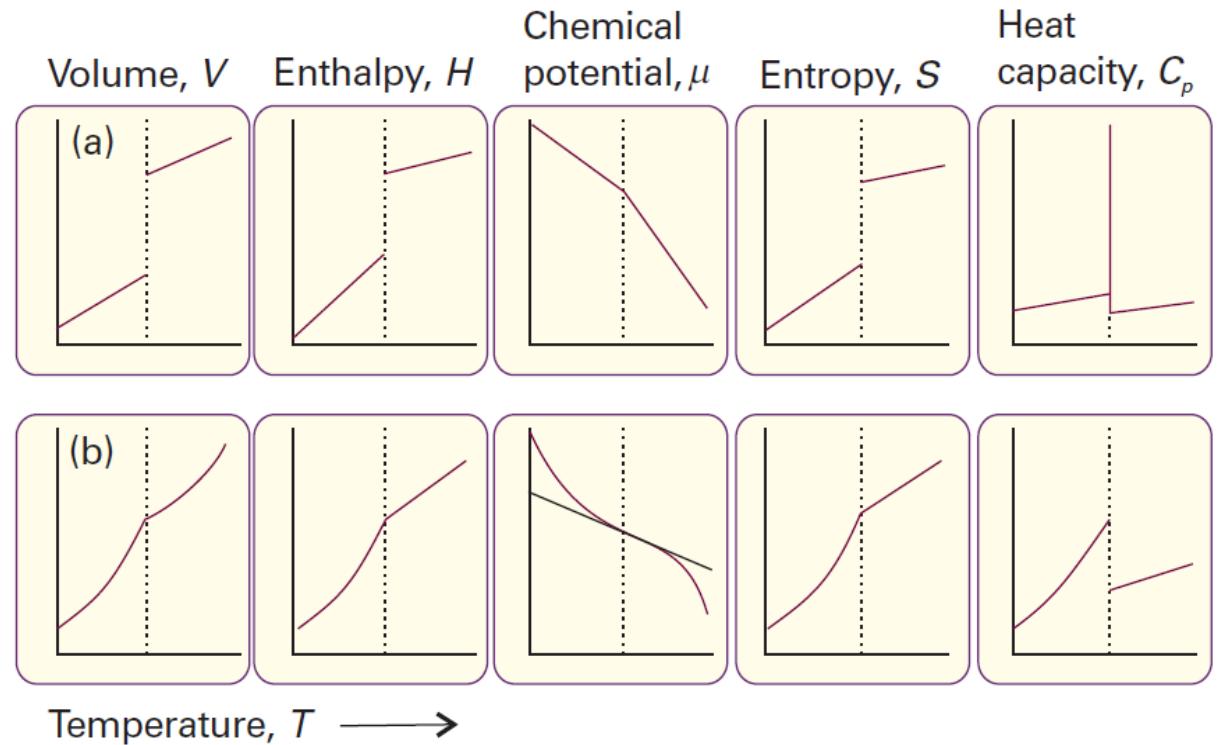


Fig. 4.16 The changes in thermodynamic properties accompanying (a) first-order and (b) second-order phase transitions.

First & Second ORDER Phase transitions

IL, [C_nmim][PF₆]

