## **Chapter 4 – New Exercises and Solutions**

**E4.1(c)** The vapour pressure of a substance at 50.0°C is 43.0 kPa and its enthalpy of vaporization is 42.2 kJ mol<sup>-1</sup>. Estimate the temperature at which its vapour pressure is 96.0 kPa.

**E4.1(c)** Assume vapour is a perfect gas and  $\Delta_{\text{vap}}H$  is independent of temperature

$$\ln \frac{p^*}{p} = + \frac{\Delta_{\text{vap}} H}{R} \left( \frac{1}{T} - \frac{1}{T^*} \right)$$

$$\frac{1}{T} = \frac{1}{T^*} + \frac{R}{\Delta_{\text{vap}} H} \ln \frac{p^*}{p}$$

$$= \frac{1}{323.2 \text{ K}} + \frac{8.314 \text{ J K}^{-1} \text{ mol}^{-1}}{42.2 \times 10^3 \text{ J mol}^{-1}} \times \ln \left( \frac{43.0}{96.0} \right)$$

$$= 2.936 \times 10^{-3} \text{ K}^{-1}$$

$$T = \frac{1}{2.936 \times 10^{-3} \text{ K}^{-1}} = 341 \text{ K} = \boxed{68^{\circ} \text{ C}}$$

**E4.2(c)** The molar volume of a certain solid is 122.0 cm<sup>3</sup> mol<sup>-1</sup> at 1.00 atm and 483.15 K, its melting temperature. The molar volume of the liquid at this temperature and pressure is 142.6 cm<sup>3</sup> mol<sup>-1</sup>. At 1.29 MPa the melting temperature changes to 485.34 K. Calculate the enthalpy and entropy of fusion of the solid.

**E4.2(c)** 
$$\frac{\mathrm{d}p}{\mathrm{d}T} = \frac{\Delta S_{\mathrm{m}}}{\Delta V_{\mathrm{m}}}$$

$$\Delta_{\mathrm{fus}}S = \Delta V_{\mathrm{m}} \left(\frac{\mathrm{d}p}{\mathrm{d}T}\right) \approx \Delta V_{\mathrm{m}} \frac{\Delta p}{\Delta T}$$

assuming  $\Delta_{\mbox{\tiny fus}} S$  and  $\Delta V_{\mbox{\tiny m}}$  independent of temperature.

$$\begin{split} &\Delta_{\text{fus}} S = \left(142.6\,\text{cm}^3\,\text{mol}^{-1} - 122.0\,\text{cm}^3\,\text{mol}^{-1}\right) \times \frac{\left(1.26 \times 10^6\,\text{Pa}\right) - \left(1.01 \times 10^5\,\text{Pa}\right)}{485.34\,\text{K} - 483.15\,\text{K}} \\ &= \left(20.6\,\text{cm}^3\,\text{mol}^{-1}\right) \times \left(\frac{1\,\text{m}^3}{10^6\,\text{cm}^3}\right) \times \left(5.29 \times 10^5\,\text{Pa}\,\text{K}^{-1}\right) \\ &= 10.90\,\text{Pa}\,\text{m}^3\,\text{K}^{-1}\,\text{mol}^{-1} = \boxed{10.9\,\text{J}\,\text{K}^{-1}\,\text{mol}^{-1}} \\ &\Delta_{\text{fus}} H = T_{\text{f}} \Delta S = \left(483.15\,\text{K}\right) \times \left(10.9\overline{0}\,\text{J}\,\text{K}^{-1}\,\text{mol}^{-1}\right) \\ &= \boxed{5.27\,\text{kJ}\,\text{mol}^{-1}} \end{split}$$

**E4.3(c)** The vapour pressure of a liquid in the temperature range 200 K to 260 K was found to fit the expression  $\ln(p/\text{Torr}) = 20.465 - 3339.8/(T/K)$ . Calculate the enthalpy of vaporization of the liquid.

**E4.3(c)** The expression for  $\ln p$  is the indefinite integral of eqn 4.11

$$\int d \ln p = \int \frac{\Delta_{\text{vap}} H}{RT^2} dT; \quad \ln p = \text{constant} - \frac{\Delta_{\text{vap}} H}{RT}$$

Therefore,  $\Delta_{\text{vap}}H = (3339.8 \text{ K}) \times R = (3339.8 \text{ K}) \times (8.314 \text{ J } K^{-1} \text{ mol}^{-1}) = \boxed{+29.77 \text{ kJ mol}^{-1}}$ 

- **E4.4(c)** The vapour pressure of hexane between -10°C and +90°C fits the expression  $\log(p/\text{Torr}) = 7.724 1655/(T/\text{K})$ . Calculate (a) the enthalpy of vaporization and (b) the normal boiling point of hexane.
- **E4.4(c)** (a) The indefinitely integrated form of eqn 4.11 is used as in Exercise 4.3(a).

$$\ln p = \text{constant} - \frac{\Delta_{\text{vap}} H}{RT}$$
, or  $\log p = \text{constant} - \frac{\Delta_{\text{vap}} H}{2.303 \ RT}$ 

Therefore.

$$\Delta_{\text{vap}} H = (2.303) \times (1655 \,\text{K}) \times R = (2.303) \times (1655 \,\text{K}) \times (8.314 \,\text{J} \,\text{K}^{-1} \,\text{mol}^{-1})$$
$$= \boxed{+31.69 \,\text{kJ} \,\text{mol}^{-1}}$$

(b) The boiling point corresponds to p = 1.000 atm = 760 Torr.

$$\log 760 = 7.724 - \frac{1655 \,\mathrm{K}}{T_{\mathrm{b}}}$$

$$T_{\rm b} = 341.7 \, \rm K$$

- **E4.5(c)** When water freezes at 0.00°C its density changes from 1.000 g cm<sup>-3</sup> to 0.917 g cm<sup>-3</sup>. Its enthalpy of fusion is 6.01 kJ mol<sup>-1</sup>. Estimate the freezing point of water at 1000 atm.
- E4.5(c)

$$\begin{split} \Delta T &\approx \frac{\Delta_{\text{fus}} V}{\Delta_{\text{fus}} S} \times \Delta p \ [4.6, \text{and Exercise } 4.2(\text{a})] \\ &\approx \frac{T_{\text{f}} \Delta_{\text{fus}} V}{\Delta_{\text{fus}} H} \times \Delta p = \frac{T_{\text{f}\Delta pM}}{\Delta_{\text{fus}} H} \times \Delta \left(\frac{1}{\rho}\right) \ [V_{\text{m}} = M/\rho] \\ &\approx \left(\frac{(273.2 \text{ K}) \times (999) \times (1.013 \times 10^5 \text{ Pa}) \times (18.02 \times 10^{-3} \text{ kg mol}^{-1})}{6.01 \times 10^3 \text{ J mol}^{-1}}\right) \\ &\times \left(\frac{1}{1000 \text{ kg m}^{-3}} - \frac{1}{917 \text{ kg m}^{-3}}\right) \approx -10.14 \text{ K} \end{split}$$

Therefore, at 1000 atm ,  $T_f \approx (273.2 - 10.1) \text{ K} = 263.1 \text{ K} [-10.1 ^{\circ}\text{C}]$ 

**E4.6(c)** In the Sahara Desert the incident sunlight at ground level has a power density of 1.44 kW m<sup>-2</sup> in July at noon. What is the maximum rate of loss of water from a pond in an oasis of area 12 m<sup>2</sup>. Assume that all the radiant energy is absorbed.

E4.6(c) 
$$\frac{dm}{dt} = \frac{dn}{dt} \times M_{\text{H}_2\text{O}} \text{ where } n = \frac{q}{\Delta_{\text{vap}}H}$$

$$\frac{dn}{dt} = \frac{dq/dt}{\Delta_{\text{vap}}H} = \frac{\left(1.44 \times 10^3 \text{ W m}^{-2}\right) \times \left(10^4 \text{ m}^2\right)}{44.0 \times 10^3 \text{ J mol}^{-1}}$$

$$= 327 \text{ J s}^{-1} \text{ J}^{-1} \text{ mol}$$

$$= 327 \text{ mol s}^{-1}$$

$$\frac{dm}{dt} = \left(327 \text{ mol s}^{-1}\right) \times \left(18.02 \text{ g mol}^{-1}\right)$$

$$= \boxed{5.90 \text{ kg s}^{-1}}$$

**E4.8(c)** The normal boiling point of heptane is 98.4°C. Estimate (a) its enthalpy of vaporization and (b) its vapour pressure at 37°C and 84°C.

$$\Delta_{\text{vap}} H = \left(85 \,\text{J K}^{-1} \,\text{mol}^{-1}\right) \times T_{\text{b}} = \left(85 \,\text{J K}^{-1} \,\text{mol}^{-1}\right) \times \left(371.6 \,\text{K}\right) = \boxed{31.\overline{6} \,\text{kJ} \,\text{mol}^{-1}}$$

(b) Use the Clausius-Clapeyron equation [Exercise 4.8(a)]

$$\ln\left(\frac{p_2}{p_1}\right) = \frac{\Delta_{\text{vap}}H}{R} \times \left(\frac{1}{T_1} - \frac{1}{T_2}\right)$$

At  $T_2 = 371.6 \text{ K}$ ,  $p_2 = 1.000 \text{ atm}$ ; thus at  $37^{\circ}\text{C}$ 

$$\ln p_1 = -\left(\frac{31.\overline{6} \times 10^3 \text{ J mol}^{-1}}{8.314 \text{ J K}^{-1} \text{ mol}^{-1}}\right) \times \left(\frac{1}{310.2 \text{ K}} - \frac{1}{371.6 \text{ K}}\right) = -2.02\overline{45}$$

$$p_1 = \overline{0.13\overline{2} \text{ atm}} = 10\overline{0} \text{ Torr}$$

At 60°C.

$$\ln p_1 = -\left(\frac{31.\overline{6} \times 10^3 \,\mathrm{J \, mol^{-1}}}{8.314 \,\mathrm{J \, K^{-1} \, mol^{-1}}}\right) \times \left(\frac{1}{357.2 \,\mathrm{K}} - \frac{1}{371.6 \,\mathrm{K}}\right) = -0.41\overline{23}$$

$$p_1 = \boxed{0.66\overline{2} \text{ atm}} = 50\overline{3} \text{ Torr}$$

**E4.9(c)** Calculate the melting point of ice under a pressure of 500 bar. Assume that the density of ice under these conditions is approximately  $0.925 \text{ g cm}^{-3}$  and that of liquid water is  $1.024 \text{ g cm}^{-3}$ .

**E4.9(c)** 
$$\Delta T = T_{\rm f} (500 \, \text{bar}) - T_{\rm f} (1 \, \text{bar}) \approx \frac{T_{\rm f} \Delta p M}{\Delta_{\rm fus} H} \Delta \left(\frac{1}{P}\right) [\text{Exercise 4.5(a)}]$$
  
$$\Delta_{\rm fus} H = 6.01 \, \text{kJ mol}^{-1} [\text{Table 2.3}]$$

$$\Delta T = \left(\frac{(273.15 \,\mathrm{K}) \times (499 \times 10^5 \,\mathrm{Pa}) \times (18.02 \times 10^{-3} \,\mathrm{kg \,mol^{-1}})}{6.01 \times 10^3 \,\mathrm{J \,mol^{-1}}}\right) \times \left(\frac{1}{1.024 \times 10^3 \,\mathrm{kg \,m^{-3}}} - \frac{1}{9.25 \times 10^2 \,\mathrm{kg \,m^3}}\right) = -4.27 \,\mathrm{K}$$

$$T_{\rm f}(50 \,\mathrm{bar}) = (273.15 \,\mathrm{K}) - (4.27 \,\mathrm{K}) = \boxed{268.88 \,\mathrm{K}}$$

**E4.10(c)** What fraction of the enthalpy of vaporization of benzene is spent on expanding its vapour?

$$\begin{split} \mathbf{E4.10(c)} & \quad \Delta_{\text{vap}} H = \Delta_{\text{vap}} U + \Delta_{\text{vap}} \left( \, pV \right) \\ & \quad \Delta_{\text{vap}} H = 82.93 \, \text{kJ mol}^{-1} \\ & \quad \Delta_{\text{vap}} \left( \, pV \right) = p \Delta_{\text{vap}} V = p \left( V_{\text{gas}} - V_{\text{liq}} \right) = p V_{\text{gas}} = RT \big[ \text{per mole, perfect gas} \big] \\ & \quad \Delta_{\text{vap}} \left( \, pV \right) = \left( 8.314 \, \text{J K}^{-1} \, \text{mol}^{-1} \right) \times \left( 353.2 \, \text{K} \right) = 293\overline{6} \, \text{J mol}^{-1} \\ & \quad Fraction = \frac{\Delta_{\text{vap}} \left( \, pV \right)}{\Delta_{\text{vap}} H} = \frac{2.93\overline{6} \, \text{kJ mol}^{-1}}{82.93 \, \text{kJ mol}^{-1}} \\ & \quad = \overline{3.54 \times 10^{-2}} = 3.54 \, \text{per cent} \end{split}$$