

Escola Politécnica da
Universidade de São Paulo

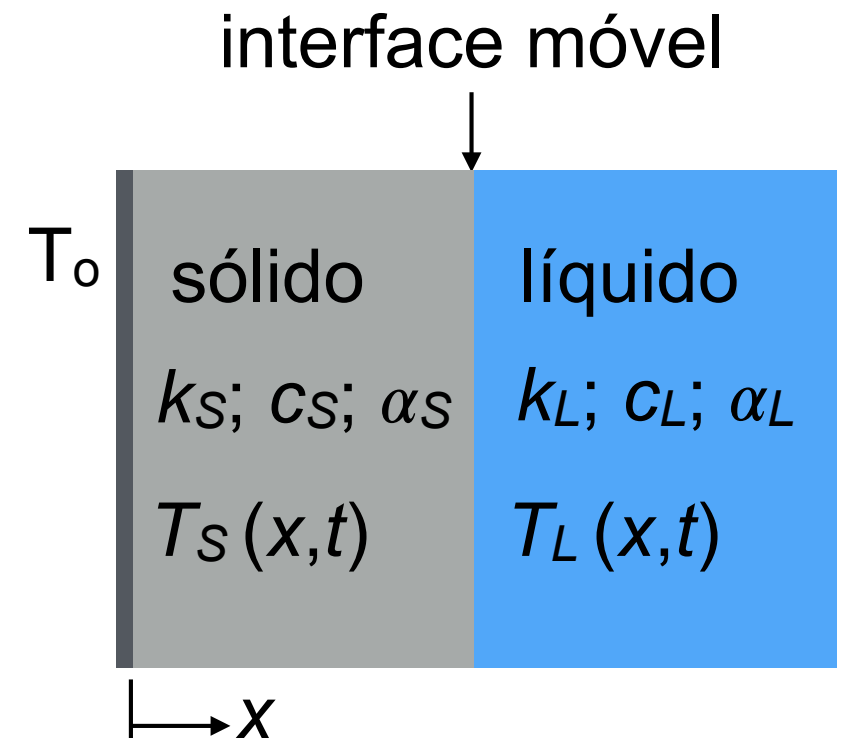
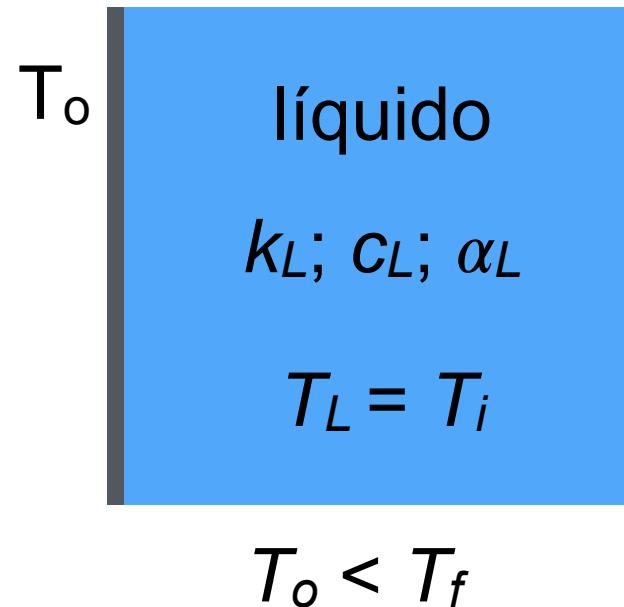
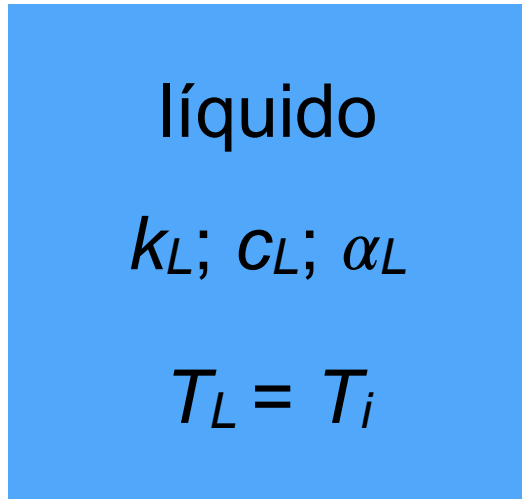


Transferência de calor e massa em sistemas biológicas

Criocirurgia



Problema 1: parede plana a T_o , sem circulação e geração

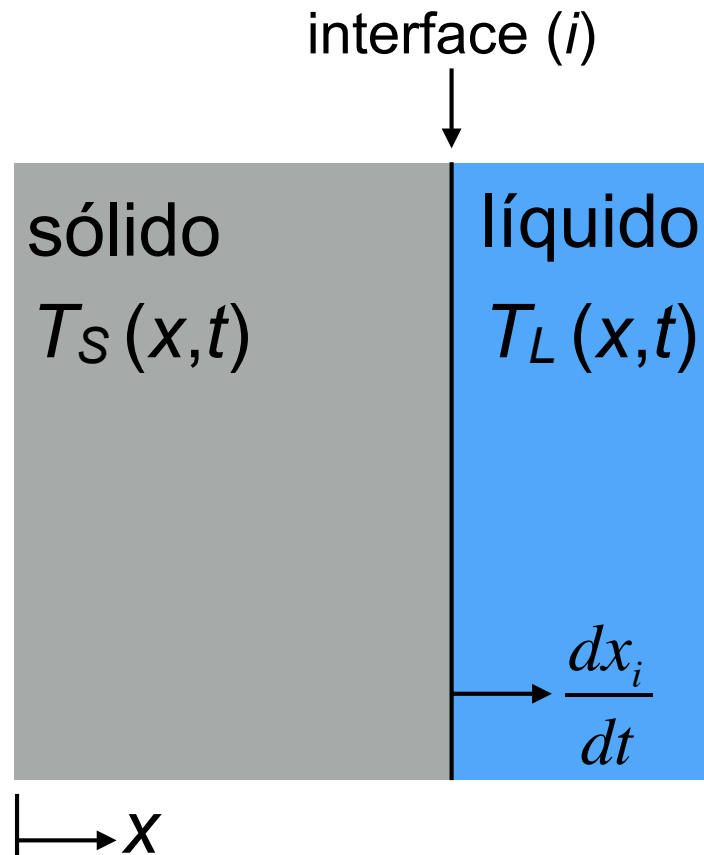




Hipóteses:

1. As propriedades em cada fase são uniformes e permanecem constantes;
2. O movimento na fase líquida oriundo da diferença de densidade é desprezível;
3. A condução de calor é unidimensional;
4. A geração de energia térmica é desprezível;
5. A transferência de calor entre sangue e tecido é desprezível;
6. O processo se dá a pressão constante.

Condições de contorno na interface

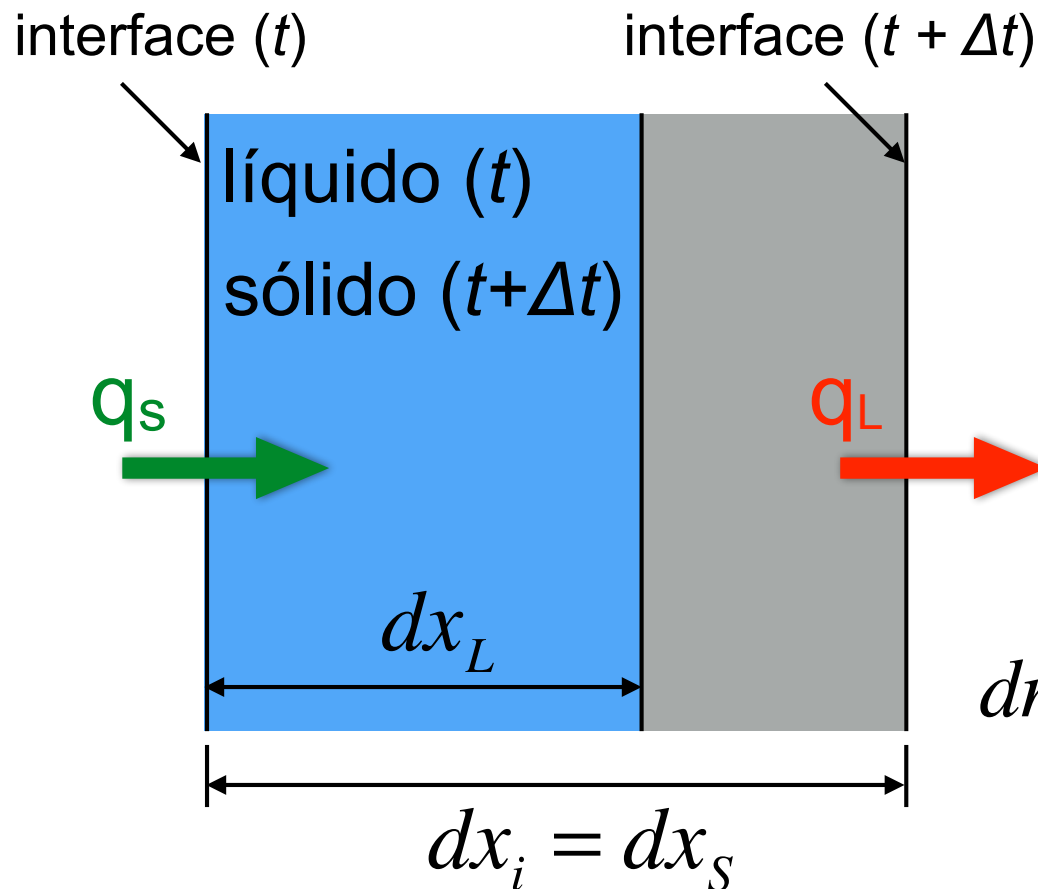


EDP:

$$\frac{1}{\alpha_s} \frac{\partial T_S}{\partial t} = \frac{\partial^2 T_S}{\partial x^2} \quad 0 < x < x_i, \quad (1)$$

$$\frac{1}{\alpha_L} \frac{\partial T_L}{\partial t} = \frac{\partial^2 T_L}{\partial x^2} \quad x > x_i, \quad (2)$$

Elemento líquido infinitesimal
que se solidificará

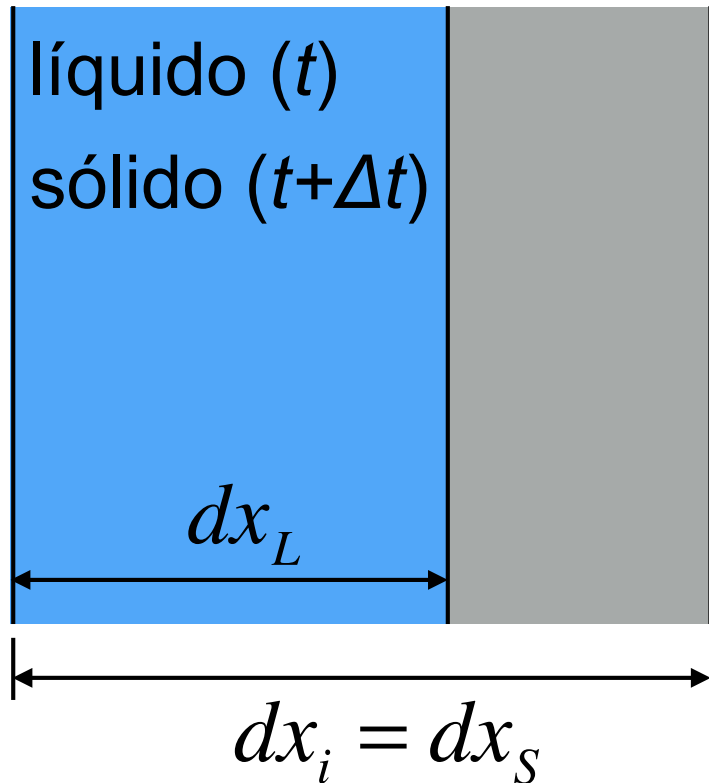


Continuidade da temperatura:

$$T_s(x_i, t) = T_L(x_i, t) = T_f \quad (3)$$

1ª lei para o sistema:

$$dm_S(u_S - u_L) = (q_s - q_L)dt - pd\forall$$



1ª lei para o sistema:

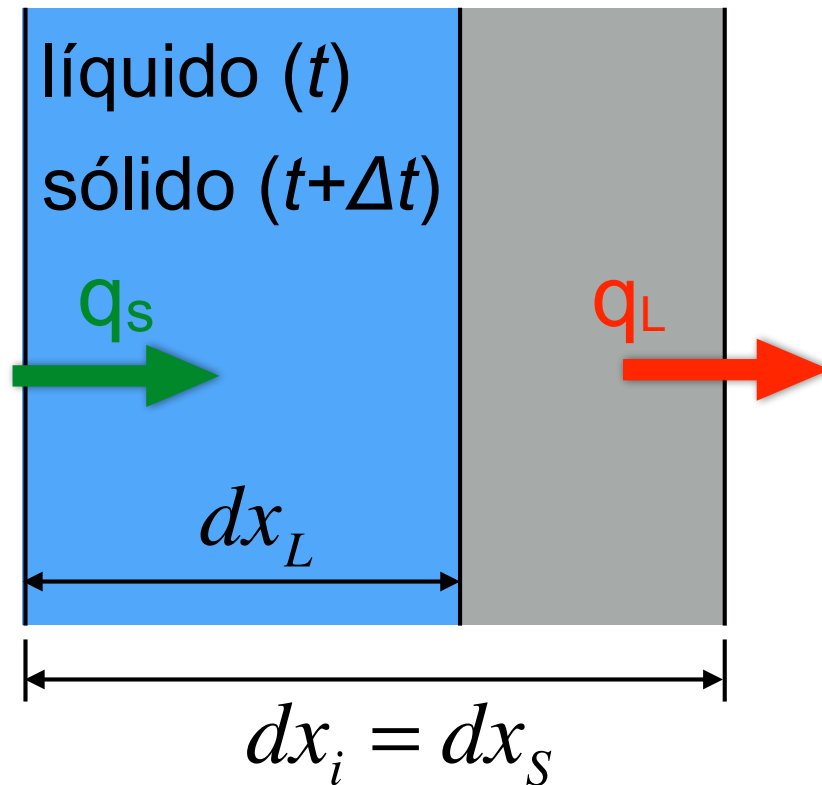
$$dm_S (u_S - u_L) = (q_S - q_L) dt - p d\forall$$

$$dm_S (u_S - u_L) = (q_S - q_L) dt - p dm_S (v_S - v_L)$$

$$dm_S [(u_S + pv_S) - (u_L + pv_L)] = (q_S - q_L) dt$$

$$\frac{dm_s}{dt} (h_S - h_L) = q_S - q_L \quad (4)$$

$$\frac{dm_s}{dt}(h_s - h_L) = q_s - q_L \quad (4)$$



Lei de Fourier:

$$q_s = -k_s A \frac{\partial T_s(x_i, t)}{\partial x} \quad (5)$$

$$q_L = -k_L A \frac{\partial T_L(x_i, t)}{\partial x} \quad (6)$$

Combinando as equações 4, 5 e 6:

$$\frac{dm_s}{dt}(h_S - h_L) = -k_S A \frac{\partial T_S(x_i, t)}{\partial x} + k_L A \frac{\partial T_L(x_i, t)}{\partial x}$$

$$\rho_S A \frac{dx_i}{dt}(h_S - h_L) = -k_S A \frac{\partial T_S(x_i, t)}{\partial x} + k_L A \frac{\partial T_L(x_i, t)}{\partial x}$$

$$\rho_S \frac{dx_i}{dt}(h_L - h_S) = k_S \frac{\partial T_S(x_i, t)}{\partial x} - k_L \frac{\partial T_L(x_i, t)}{\partial x} \quad (7)$$



$$\rho_S \frac{dx_i}{dt} (h_L - h_S) = k_S \frac{\partial T_S(x_i, t)}{\partial x} - k_L \frac{\partial T_L(x_i, t)}{\partial x} \quad (7)$$

A eq. 7 é válida na solidificação e na fusão;

Na fusão ρ_S deve ser substituída por ρ_L ;

$h_L - h_S = h_{SL}$ é a entalpia de fusão.

EDP:

$$\frac{1}{\alpha_S} \frac{\partial T_S}{\partial t} = \frac{\partial^2 T_S}{\partial x^2} \quad 0 \leq x < x_i, \quad (1)$$

$$\frac{1}{\alpha_L} \frac{\partial T_L}{\partial t} = \frac{\partial^2 T_L}{\partial x^2} \quad x > x_i, \quad (2)$$

C.C.:

$$T_S(x_i, t) = T_L(x_i, t) = T_f \quad (3)$$

$$\rho_S \frac{dx_i}{dt} h_{SL} = k_S \frac{\partial T_S(x_i, t)}{\partial x} - k_L \frac{\partial T_L(x_i, t)}{\partial x} \quad (7)$$



Variáveis adimensionais:

$$\theta_s = \frac{T_s - T_f}{T_f - T_o}$$

$$\theta_L = \frac{k_L}{k_S} \frac{T_L - T_f}{T_f - T_o}$$

$$\xi = \frac{x}{L}$$

$$\tau = Ste \frac{\alpha_s}{L^2} t$$

Número de Stefan:

$$Ste = \frac{c_s (T_f - T_o)}{h_{SL}}$$



Variáveis adimensionais:

$$d\theta_s = \frac{dT_s}{T_f - T_o} \quad \Rightarrow \quad dT_s = (T_f - T_o) d\theta_s$$

$$d\theta_L = \frac{k_L}{k_S} \frac{dT_L}{T_f - T_o} \quad \Rightarrow \quad dT_L = \frac{k_S}{k_L} (T_f - T_o) d\theta_L$$

$$d\xi = \frac{dx}{L} \quad \Rightarrow \quad dx = L d\xi$$

$$d\xi^2 = \frac{dx^2}{L} \quad \Rightarrow \quad dx^2 = L^2 d\xi^2$$

$$d\tau = Ste \frac{\alpha_s}{L^2} dt \quad \Rightarrow \quad dt = \frac{1}{Ste} \frac{L^2}{\alpha_s} d\tau$$

Adimensionalização das EDPs:

$$\partial T_S = (T_f - T_o) \partial \theta_S$$

$$\partial T_L = \frac{k_S}{k_L} (T_f - T_o) \partial \theta_L$$

$$\partial x = L \partial \xi$$

$$\partial x^2 = L^2 \partial \xi^2$$

$$\partial t = \frac{1}{Ste} \frac{L^2}{\alpha_S} \partial \tau$$

$$\frac{1}{\alpha_S} \frac{\partial T_S}{\partial t} = \frac{\partial^2 T_S}{\partial x^2} \quad 0 \leq x < x_i, \quad (1)$$

$$Ste \frac{\cancel{\alpha_S} (T_f - T_o)}{\cancel{\alpha_S} L^2} \frac{\partial \theta_S}{\partial \tau} = \frac{(T_f - T_o)}{L^2} \frac{\partial^2 \theta_S}{\partial \xi^2} \quad 0 < \xi < \xi_i$$

$$Ste \frac{\partial \theta_S}{\partial \tau} = \frac{\partial^2 \theta_S}{\partial \xi^2} \quad 0 \leq \xi < \xi_i, \quad (1a)$$

Adimensionalização das EDPs:

$$\partial T_S = (T_f - T_o) \partial \theta_S \quad \frac{1}{\alpha_L} \frac{\partial T_L}{\partial t} = \frac{\partial^2 T_L}{\partial x^2} \quad x > x_i, \quad (2)$$

$$\partial T_L = \frac{k_S}{k_L} (T_f - T_o) \partial \theta_L$$

$$\partial x = L \partial \xi$$

$$\partial x^2 = L^2 \partial \xi^2$$

$$\partial t = \frac{1}{Ste} \frac{L^2}{\alpha_S} \partial \tau$$

$$Ste \frac{k_S}{k_L} \frac{\alpha_S}{\alpha_L} \frac{(T_f - T_o)}{L^2} \frac{\partial \theta_L}{\partial \tau} = \frac{k_S}{k_L} \frac{(T_f - T_o)}{L^2} \frac{\partial^2 \theta_L}{\partial \xi^2} \quad \xi > \xi_i$$

$$Ste \frac{\partial \theta_L}{\partial \tau} = \frac{\alpha_L}{\alpha_S} \frac{\partial^2 \theta_L}{\partial \xi^2} \quad \xi > \xi_i, \quad (2a)$$



$$\rho_s \frac{dx_i}{dt} h_{SL} = k_s \frac{\partial T_s(x_i, t)}{\partial x} - k_L \frac{\partial T_L(x_i, t)}{\partial x} \quad (7)$$

$$Ste \alpha_s \rho_s \frac{L}{L^2} \frac{d\xi_i}{d\tau} h_{SL} = k_s \frac{(T_f - T_o)}{L} \frac{\partial \theta_s(\xi_i, t)}{\partial \xi} - \cancel{k_L} \frac{k_s}{k_L} \frac{(T_f - T_o)}{L} \frac{\partial \theta_L(\xi_i, t)}{\partial \xi}$$

$$\frac{Ste h_{SL} \alpha_s}{c_s (T_f - T_o)} \frac{c_s \rho_s}{k_s} \frac{d\xi_i}{d\tau} = \frac{\partial \theta_s(\xi_i, t)}{\partial \xi} - \frac{\partial \theta_L(\xi_i, t)}{\partial \xi}$$

$$\frac{d\xi_i}{d\tau} = \frac{\partial \theta_s(\xi_i, t)}{\partial \xi} - \frac{\partial \theta_L(\xi_i, t)}{\partial \xi}, \quad (7a)$$



EDPs:

$$Ste \frac{\partial \theta_S}{\partial \tau} = \frac{\partial^2 \theta_S}{\partial \xi^2} \quad 0 < \xi < \xi_i, \quad (1a)$$

$$Ste \frac{\partial \theta_L}{\partial \tau} = \frac{\alpha_L}{\alpha_S} \frac{\partial^2 \theta_L}{\partial \xi^2} \quad \xi > \xi_i, \quad (2a)$$

C.C.:

$$\theta_S(\xi_i, \tau) = \frac{k_S}{k_L} \theta_L(\xi_i, \tau) = 0, \quad (3a)$$

$$\frac{d\xi_i}{d\tau} = \frac{\partial \theta_S(\xi_i, t)}{\partial \xi} - \frac{\partial \theta_L(\xi_i, t)}{\partial \xi}, \quad (7a)$$

Simplificação: regime quase-permanente



Para $Ste \rightarrow 0$: $Ste = \frac{c_s (T_f - T_o)}{h_{SL}}$

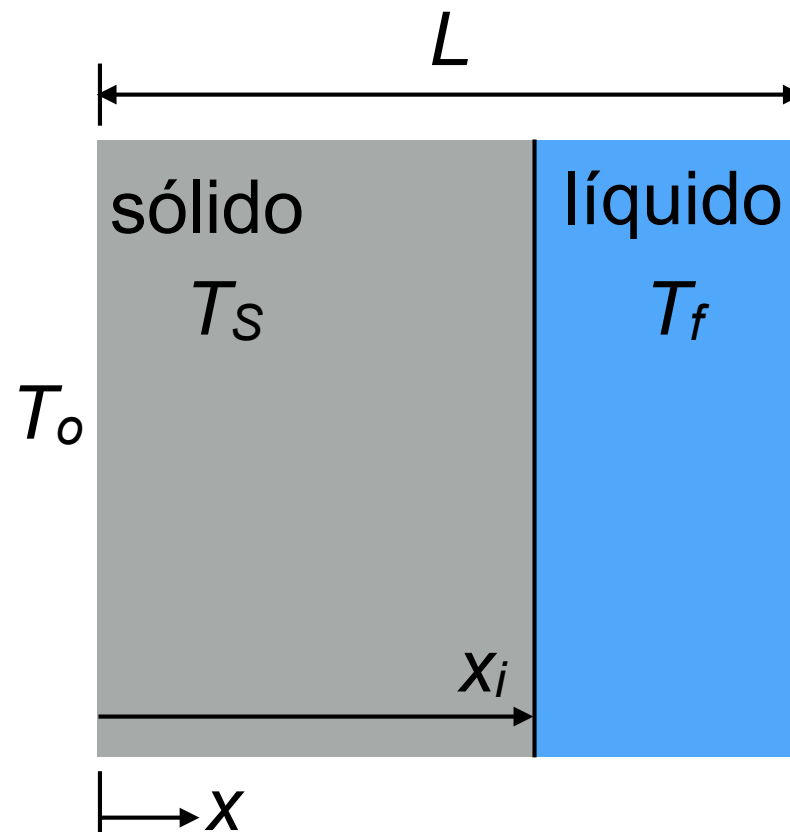
$$Ste \frac{\partial \theta_s}{\partial \tau} = \frac{\partial^2 \theta_s}{\partial \xi^2} \quad \longrightarrow \quad \frac{\partial^2 \theta_s}{\partial \xi^2} = 0 \quad \longrightarrow \quad \frac{d^2 \theta_s}{d\xi^2} = 0$$

$$Ste \frac{\partial \theta_L}{\partial \tau} = \frac{\alpha_L}{\alpha_s} \frac{\partial^2 \theta_L}{\partial \xi^2} \quad \longrightarrow \quad \frac{\partial^2 \theta_L}{\partial \xi^2} = 0 \quad \longrightarrow \quad \frac{d^2 \theta_L}{d\xi^2} = 0$$

Ex. 1 - solidificação de um bloco a T_f



Determinar o tempo necessário para solidificar todo o bloco de espessura L .



Ex. 1 - solidificação de um bloco a T_f



EDOs:

$$\frac{d^2 T_S}{dx^2} = 0$$

$$\frac{d^2 T_L}{dx^2} = 0$$

CCs e CI:

$$T_S(0, t) = T_o \quad (1)$$

$$T_S(x_i, t) = T_f \quad (2)$$

$$T_L(x_i, t) = T_f \quad (3)$$

$$T_L(L, t) = T_f \quad (4)$$

$$\rho_S \frac{dx_i}{dt} h_{SL} = k_S \frac{\partial T_S(x_i, t)}{\partial x} - k_L \frac{\partial T_L(x_i, t)}{\partial x} \quad (5)$$

Ex. 1 - solidificação de um bloco a T_f



Integração das EDOs:

$$\frac{\partial^2 T_S}{\partial x^2} = 0 \quad T_S = Ax + B$$

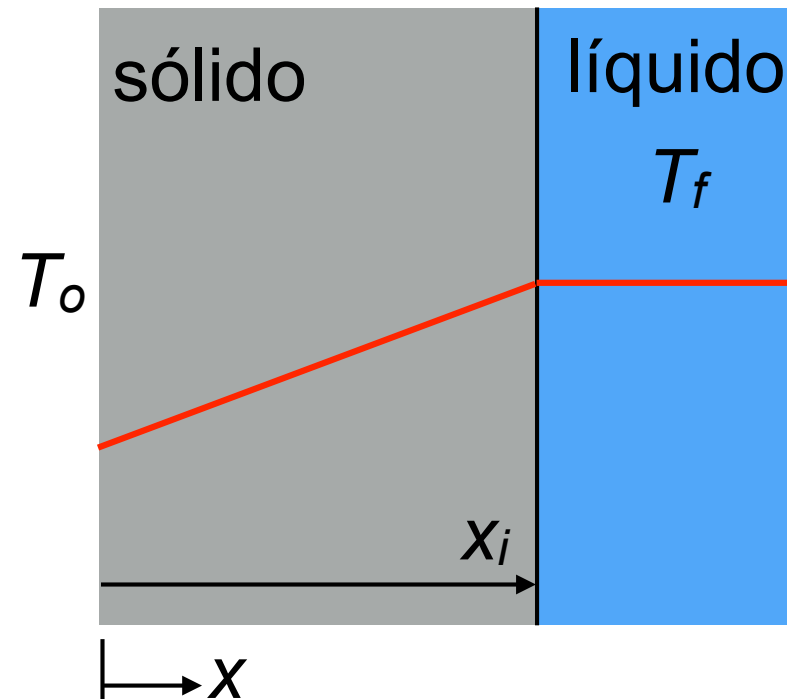
$$\frac{\partial^2 T_L}{\partial x^2} = 0 \quad T_L = Cx + D$$

de (1) e (2):

$$T_S(x,t) = (T_f - T_o) \frac{x}{x_i} + T_o \quad (6)$$

de (3) e (4):

$$T_L(x,t) = T_f \quad (7)$$



Ex. 1 - solidificação de um bloco a T_f



Determinação da frente de congelamento:

$$\rho_S \frac{dx_i}{dt} h_{SL} = k_S \frac{dT_S(x_i, t)}{\partial x} - k_L \frac{dT_L(x_i, t)}{\partial x} \quad (5)$$

Substituindo (6) e (7) em (5), obtemos:

$$\rho_S \frac{dx_i}{dt} h_{SL} = k_S \frac{T_f - T_o}{x_i} - k_L 0 \quad \longrightarrow \quad x_i dx_i = k_S \frac{T_f - T_o}{\rho_S h_{SL}} dt$$


$$\int_0^{x_i} x_i dx_i = \int_0^t k_S \frac{T_f - T_o}{\rho_S h_{SL}} dt \quad \longrightarrow \quad x_i = \sqrt{\frac{2k_S (T_f - T_o) t}{\rho_S h_{SL}}}$$

Ex. 1 - solidificação de um bloco a T_f



Para completa solidificação, $x_i = L$:

$$L = \sqrt{\frac{2k_S(T_f - T_o)t^*}{\rho_S h_{SL}}}$$

 $t^* = \frac{\rho_S h_{SL} L^2}{2k_S(T_f - T_o)}$

Solução para um sólido semi-infinito.

Fase sólida:

$$\frac{1}{\alpha_s} \frac{\partial T_s}{\partial t} = \frac{\partial^2 T_s}{\partial x^2} \quad 0 \leq x < x_i, \quad (1)$$

$$T_s(0, t) = T_o \quad (2)$$

$$T_s(x_i, t) = T_f \quad (3)$$

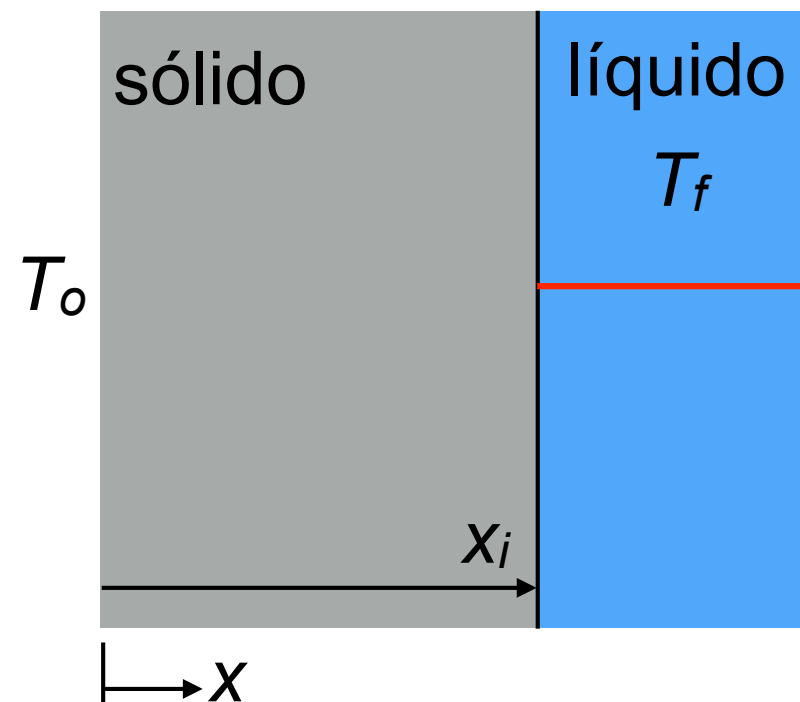
Interface:

$$\rho_s \frac{dx_i}{dt} h_{SL} = k_s \frac{\partial T_s(x_i, t)}{\partial x} \quad (5)$$

$$x_i(0) = 0 \quad (6)$$

Fase líquida:

$$T_L(x, t) = T_f \quad (4)$$





Solução por similaridade, $\eta = \eta(x, t)$

$$\eta = \frac{x}{\sqrt{4\alpha_s t}}, \quad T_s = T_s(\eta)$$

Utilizando a variável de similaridade transformamos a Eq. (1):

$$\frac{d^2 T_s}{dx^2} + 2\eta \frac{dT_s}{d\eta} = 0 \quad \longrightarrow \quad T_s = A \operatorname{erf}(\eta) + B$$

Determinamos as constantes pelas condições (2) e (3):

$$T_s(0, t) = T_o \quad \longrightarrow \quad \eta = 0 \quad \longrightarrow \quad \operatorname{erf}(\eta) = 0 \quad \longrightarrow \quad B = T_o$$

$$T_s(x_i, t) = T_f \quad \longrightarrow \quad T_f = A \operatorname{erf}\left(\frac{x_i}{\sqrt{4\alpha_s t}}\right) + T_o$$



$$T_f = A \operatorname{erf} \left(\frac{x_i}{\sqrt{4\alpha_s t}} \right) + T_o$$

Note que, como não conhecemos x_i , não podemos determinar A !

Note, entretanto, que para qualquer x_i , $\operatorname{erf}()$ deve ser constante, logo:

$$x_i \propto \sqrt{t} \quad \rightarrow \quad x_i = \lambda \sqrt{4\alpha_s t}$$

Podemos escrever:

$$T_f = A \operatorname{erf}(\lambda) + T_o \quad \rightarrow \quad A = \frac{T_f - T_o}{\operatorname{erf}(\lambda)}$$



Assim, a solução para a EDP (1) é:

$$T_s = \frac{T_f - T_o}{\operatorname{erf}(\lambda)} \operatorname{erf}\left(\frac{x}{\sqrt{4\alpha_s t}}\right) + T_o$$

A constante λ pode ser determinada a partir de (5):

$$\rho_s \frac{dx_i}{dt} h_{SL} = k_s \frac{\partial T_s(x_i, t)}{\partial x} \quad (5)$$

Precisamos determinar a derivada que aparece em (5):

$$\frac{\partial T_s}{\partial x} = \frac{\partial T_s}{\partial \eta} \frac{\partial \eta}{\partial x}$$



$$T_s = \frac{T_f - T_o}{\text{erf}(\lambda)} \text{erf}\left(\frac{x}{\sqrt{4\alpha_s t}}\right) + T_o$$

$$\frac{\partial T_s}{\partial x} = \frac{\partial T_s}{\partial \eta} \frac{\partial \eta}{\partial x} \quad \rightarrow \quad \frac{\partial T_s}{\partial x} = \frac{T_f - T_o}{\text{erf}(\lambda)} \frac{\partial(\text{erf}\eta)}{\partial \eta} \frac{\partial \eta}{\partial x}$$

$$\rightarrow \quad \frac{\partial T_s}{\partial x} = \frac{T_f - T_o}{\text{erf}(\lambda)} \frac{2}{\sqrt{\pi}} e^{-\eta^2} \frac{1}{\sqrt{4\alpha_s t}}$$

Calculando em x_i e t :

$$\frac{\partial T_s(x_i, t)}{\partial x} = \frac{T_f - T_o}{\text{erf}(\lambda)} \frac{2}{\sqrt{\pi}} e^{-\lambda^2} \frac{1}{\sqrt{4\alpha_s t}}$$



Temos, então:

$$\rho_s \frac{dx_i}{dt} h_{SL} = k_s \frac{\partial T_s(x_i, t)}{\partial x} \quad (5) \quad \frac{\partial T_s(x_i, t)}{\partial x} = \frac{T_f - T_o}{\operatorname{erf}(\lambda)} \frac{2}{\sqrt{\pi}} e^{-\lambda^2} \frac{1}{\sqrt{4\alpha_s t}}$$

$$\rightarrow \rho_s \frac{dx_i}{dt} h_{SL} = k_s \frac{T_f - T_o}{\operatorname{erf}(\lambda)} \frac{2}{\sqrt{\pi}} e^{-\lambda^2} \frac{1}{\sqrt{4\alpha_s t}}$$

$$\rightarrow \rho_s \frac{d(\lambda \sqrt{4\alpha_s t})}{dt} h_{SL} = k_s \frac{T_f - T_o}{\operatorname{erf}(\lambda)} \frac{2}{\sqrt{\pi}} e^{-\lambda^2} \frac{1}{\sqrt{4\alpha_s t}}$$

$$\rightarrow \rho_s \lambda \frac{\sqrt{4\alpha_s}}{2\sqrt{t}} h_{SL} = k_s \frac{T_f - T_o}{\operatorname{erf}(\lambda)} \frac{2}{\sqrt{\pi}} e^{-\lambda^2} \frac{1}{\sqrt{4\alpha_s t}}$$



Devemos isolar λ da equação:

$$\rho_s \lambda \frac{\sqrt{4\alpha_s}}{2\sqrt{t}} h_{SL} = k_s \frac{T_f - T_o}{\operatorname{erf}(\lambda) \sqrt{\pi}} e^{-\lambda^2} \frac{1}{\sqrt{4\alpha_s t}}$$

$$\rightarrow \lambda \operatorname{erf}(\lambda) e^{\lambda^2} = \frac{c_s (T_f - T_o)}{h_{SL} \sqrt{\pi}}, \quad (7)$$



$$\lambda \operatorname{erf}(\lambda) e^{\lambda^2} = \frac{c_s (T_f - T_o)}{h_{SL} \sqrt{\pi}}, \quad (7)$$

A Eq. (7) não pode ser resolvida explicitamente. Podemos obter uma solução aproximada para pequenos λ :

$$e^{\lambda^2} = 1 + \frac{\lambda^2}{1!} + \frac{\lambda^4}{2!} \dots \approx 1$$

$$\operatorname{erf} \lambda = \frac{2}{\sqrt{\pi}} \left(\lambda - \frac{\lambda^3}{3 \cdot 1!} + \frac{\lambda^5}{5 \cdot 2!} \dots \right) \approx \frac{2}{\sqrt{\pi}} \lambda$$

Substituindo em (7):

$$\frac{2}{\sqrt{\pi}} \lambda^2 = \frac{c_s (T_f - T_o)}{h_{SL} \sqrt{\pi}} \quad \rightarrow \quad \lambda = \sqrt{\frac{c_s (T_f - T_o)}{2h_{SL}}}$$



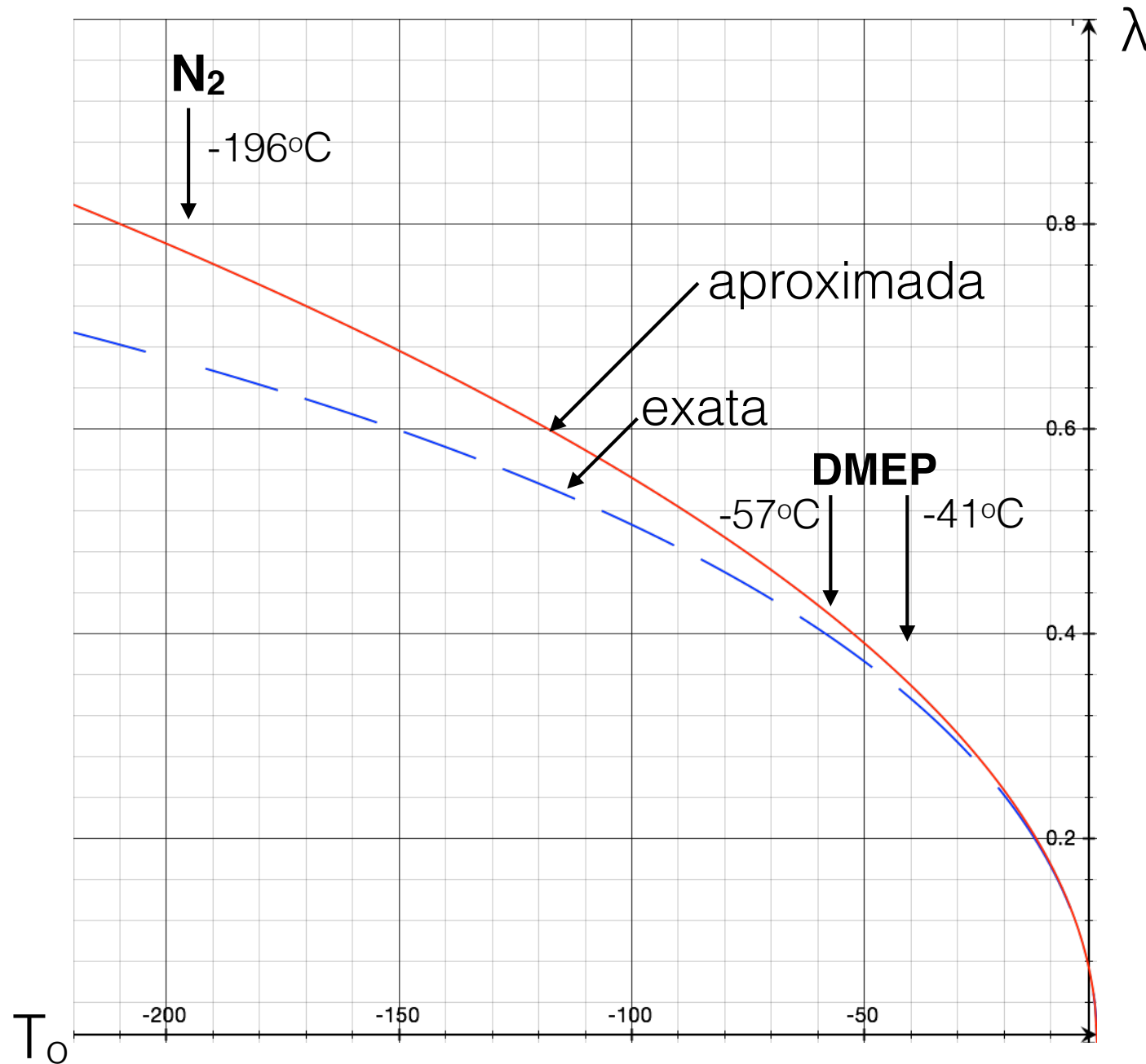
$$\lambda = \sqrt{\frac{c_S (T_f - T_o)}{2h_{SL}}}$$

Combinando com $x_i = \lambda \sqrt{4\alpha_S t}$

$$x_i = \sqrt{\frac{2k_S (T_f - T_o)}{\rho_S h_{SL}}} t$$

Para grandes valores de λ não vale a solução acima. Nesse caso podemos usar o gráfico da página seguinte.

Stefan: valor de λ



DMEP = dimetil-
éter propano