



$$x_A = 0,3 \quad (R1)$$



TC

NVI	(3) + 4(T ₁ , T ₂ , T ₃ , T ₄) + 1(Q _{TC})
NVEI	(1) + 3(T ₁ , T ₂ , T ₃) + 1(Q _{TC} =0)
NBI	1(BE)
NRI	0
NGL	2

reactor

(3) + 1(n) + 2(T ₂ , T ₃) + 1(Q _R)
(1) + 2(T ₂ , T ₃)
(2) + 1(BE)
(1)
0

global

NVI	(3) + 1(n) + 2(T ₁ , T ₄) + 1(Q _{glb})
NVEI	(1) + 1(T ₁)
NBI	(2) + 1(BE)
NRI	(0)
NGL	2

processo (5x5)

(3) + 1(n) + 4(T ₁ , T ₂ , T ₃ , T ₄) + 2(Q _{TC} , Q _R)
(1) + 3(T ₁ , T ₂ , T ₃) + 1(Q _{TC} =0)
(2) + 2(BE)
(1)
0

1) reactor: BM e BE macopladas

$$\begin{aligned} A: F_{A,2} - F_{A,3} - n_0 &= 0 \\ 1 - F_{A,3} - n_0 &= 0 \quad (1) \end{aligned} \quad \begin{aligned} D: F_{D,2} - F_{D,3} + 2n &= 0 \\ - F_{D,3} + 2n &= 0 \quad (2) \end{aligned}$$

$$R1: (F_{A,2} - F_{A,3}) / F_{A,2} = 0,3 \rightarrow (1 - F_{A,3}) / 1 = 0,3 \quad (3)$$

$$De(3): F_{A,3} = 0,7 \text{ kmol/h} ; De(1): n_0 = 0,3 \text{ kmol/h}$$

$$De(2): F_{D,3} = 0,6 \text{ kmol/h}$$

$$\begin{aligned} BE: \sum_{A=1}^5 \left[\sum_{j=1}^J F_{A,j} \cdot (\tilde{H}_{A,j} - \tilde{H}_{A,ref}) - \sum_{K=1}^K F_{A,K} \cdot (\tilde{H}_{A,K} - \tilde{H}_{A,ref}) \right] + \\ - \sum_{q=1}^Q n_q \cdot \Delta \tilde{H}_{R,q}(T_{ref}) + \dot{Q}_R - \dot{W}_0 &= 0 ; \text{ se j o } T_{ref} = T_3 = 200^\circ\text{C} \end{aligned}$$

$$F_{A,2} \cdot (\tilde{H}_{A,2} - \tilde{H}_{A,3}) - n_0 \cdot \Delta \tilde{H}_{R}(T_3) + \dot{Q}_R = 0$$

$$F_{A,2} \cdot \int_{T_3}^{T_2} \tilde{C}_P, AdT - n_0 \cdot \Delta \tilde{H}_{R}(T_3) + \dot{Q}_R = 0 \quad (4)$$

$$\Delta \tilde{H}_R(T_{ref}) = \Delta \tilde{H}_R^o(T^o) + \int_{T^o}^T \Delta \tilde{C}_P dT$$

$$\Delta \tilde{H}_R^o(T^o) = \Delta \tilde{H}_R^o(25^\circ C) = z \cdot \Delta \tilde{H}_{P,D} - \Delta \tilde{H}_{P,A}$$

$$= z \cdot (-3 \cdot 10^5) - (-2 \cdot 10^5) = -4 \cdot 10^5 \text{ kJ/Kmol}$$

$$\Delta \tilde{C}_P = z \cdot \tilde{C}_{P,D} - \tilde{C}_{P,A} = 2.50 - 15 = 85 \text{ kJ/(Kmol}^\circ\text{C)}$$

$$\therefore \Delta \tilde{H}_R(200^\circ C) = -4 \cdot 10^5 \frac{\text{kJ}}{\text{Kmol}} + 85 \frac{\text{kJ}}{\text{Kmol}^\circ\text{C}} \cdot (200-25)^\circ\text{C} = -385125 \frac{\text{kJ}}{\text{Kmol}}$$

$$\text{De (4)} : 1.15 \cdot (100-200) - 0,3 \cdot (-385125) + \dot{Q}_R = 0$$

$$\dot{Q}_R = -114037,5 \text{ kJ/h}$$

água de resfriamento: $\dot{Q} = -\dot{Q}_R = \dot{m}_{H_2O} \cdot \tilde{C}_{P,H_2O} \cdot \Delta T$

$$\dot{m}_{H_2O} = \frac{\dot{Q}}{\tilde{C}_{P,H_2O} \cdot \Delta T} = \frac{114037,5 \text{ kJ/h}}{4,18 \frac{\text{kJ}}{\text{kg}^\circ\text{C}} \cdot (50-5)^\circ\text{C}} = 606,3 \text{ kg/h}$$

$$2) \underline{T_C} \quad \text{BE: } \sum_{S=1}^3 \left[\sum_{j=1}^4 F_{A,j} \cdot \tilde{H}_{A,j} - \sum_{K=1}^4 F_{D,K} \cdot \tilde{H}_{D,K} \right] + \cancel{\dot{Q}_{TC}} - \cancel{W_S} = 0$$

$$F_{A,1} \cdot \tilde{H}_{A,1} - F_{A,2} \cdot \tilde{H}_{A,2} + F_{A,3} \cdot \tilde{H}_{A,3} - F_{A,4} \cdot \tilde{H}_{A,4} + F_{D,3} \cdot \tilde{H}_{D,3} - F_{D,4} \cdot \tilde{H}_{D,4} = 0$$

$$\text{mas: } F_{A,1} = F_{A,2}; F_{A,3} = F_{A,4}; F_{D,3} = F_{D,4} \quad \therefore$$

$$F_{A,1} \cdot (\tilde{H}_{A,1} - \tilde{H}_{A,2}) + F_{A,3} \cdot (\tilde{H}_{A,3} - \tilde{H}_{A,4}) + F_{D,3} \cdot (\tilde{H}_{D,3} - \tilde{H}_{D,4}) = 0$$

$$F_{A,1} \cdot (\tilde{H}_A(T_1) - \tilde{H}_A(T_2)) + F_{A,3} \cdot (\tilde{H}_A(T_3) - \tilde{H}_A(T_4)) + F_{D,3} \cdot (\tilde{H}_D(T_3) - \tilde{H}_D(T_4)) = 0$$

$$F_{A,1} \cdot \int_{T_2}^{T_1} \tilde{C}_{P,A} dT + F_{A,3} \cdot \int_{T_4}^{T_3} \tilde{C}_{P,A} dT + F_{D,3} \cdot \int_{T_4}^{T_3} \tilde{C}_{P,D} dT = 0$$

$$F_{A,1} \cdot \tilde{C}_{P,A} (T_1 - T_2) + F_{A,3} \cdot \tilde{C}_{P,A} (T_3 - T_4) + F_{D,3} \cdot \tilde{C}_{P,D} (T_3 - T_4) = 0$$

$$F_{A,1} \cdot \tilde{C}_{P,A} (T_1 - T_2) + (F_{A,3} \cdot \tilde{C}_{P,A} + F_{D,3} \cdot \tilde{C}_{P,D}) \cdot (T_3 - T_4) = 0$$

$$1.15 \cdot (25-100) + (0,7 \cdot 15 + 0,6 \cdot 50) \cdot (200 - T_4) = 0$$

$$-112,5 + 40,5 (200 - T_4) \longrightarrow T_4 = 172,2^\circ C$$