



ESCOLA POLITÉCNICA DA UNIVERSIDADE DE SÃO PAULO

- PQI 3203 Fenômenos de Transporte I

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ESCOLA POLITÉCNICA DA UNIVERSIDADE DE SÃO PAULO

Aula 15.5 – Equações para leitos

PQI 3203 Fenômenos de Transporte

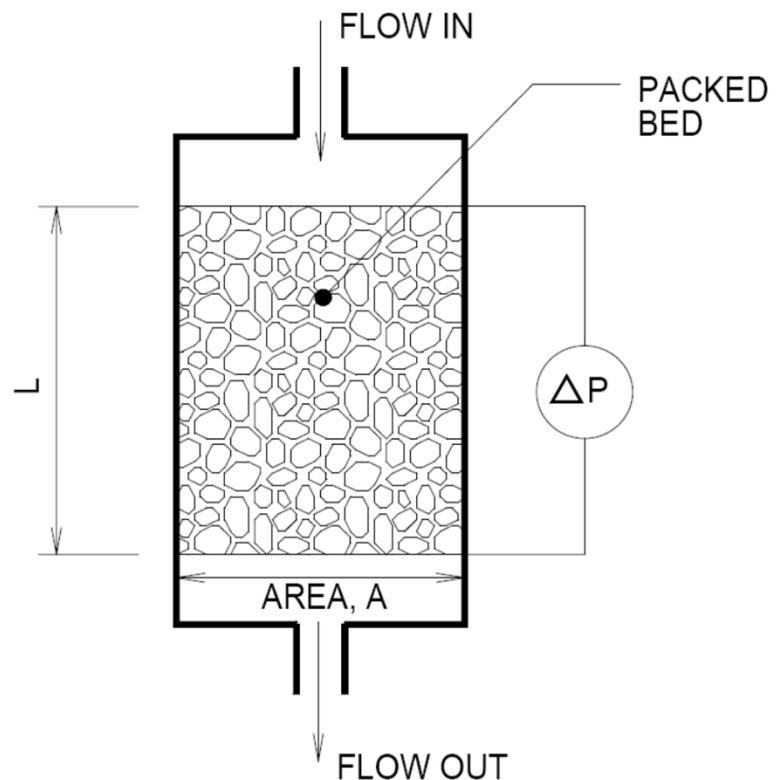


Equações para perda de carga

1. D'Arcy
2. Ergun
3. Outras



D'Arcy – Permeabilidade (1830)



$$\frac{Q}{A} = \frac{k}{\mu} \left(\frac{P_0 - P_L}{L} \right)$$

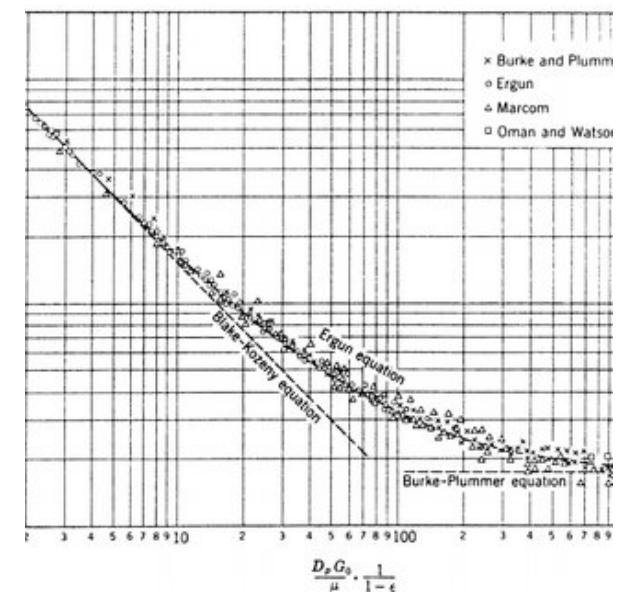


Ergun

$$\frac{-\Delta P}{L} = \frac{150 \mu q (1 - \varepsilon)^2}{(\psi D_P)^2 \varepsilon^3} + \frac{1.75 \rho q^2 (1 - \varepsilon)}{\psi D_P \varepsilon^3}$$

$q = Q / \text{área do tubo}$, q é a velocidade dita superficial

$$\text{Fluxo} = G = \rho \cdot q$$



Ergun

$$\frac{-\Delta P}{L} = \frac{150 \mu q (1-\varepsilon)^2}{(\psi D_p)^2 \varepsilon^3} + \frac{1.75 \rho q^2 (1-\varepsilon)}{\psi D_p \varepsilon^3}$$

- Ou
- $\frac{-\Delta P}{\rho q^2} \frac{\psi D_p}{L} \frac{\varepsilon^3}{(1-\varepsilon)} = \frac{150(1-\varepsilon)}{\rho q \psi D_p / \mu} + 1.75$



Ergun

- $$\frac{-\Delta P}{\rho q^2} \frac{\psi D_P}{L} \frac{\varepsilon^3}{(1-\varepsilon)} = \frac{150(1-\varepsilon)}{\rho q \psi D_P / \mu} + 1.75$$
- Onde: fator de fricção e Reynolds para a partícula
- $f_p = \frac{-\Delta P}{\rho q^2} \frac{\psi D_P}{L} \frac{\varepsilon^3}{(1-\varepsilon)}$ $Re_{leito} = \frac{\rho q \psi D_P}{\mu (1-\varepsilon)}$ $f_p = \frac{150}{Re_{leito}} + 1.75$



Ergun

- Ergun

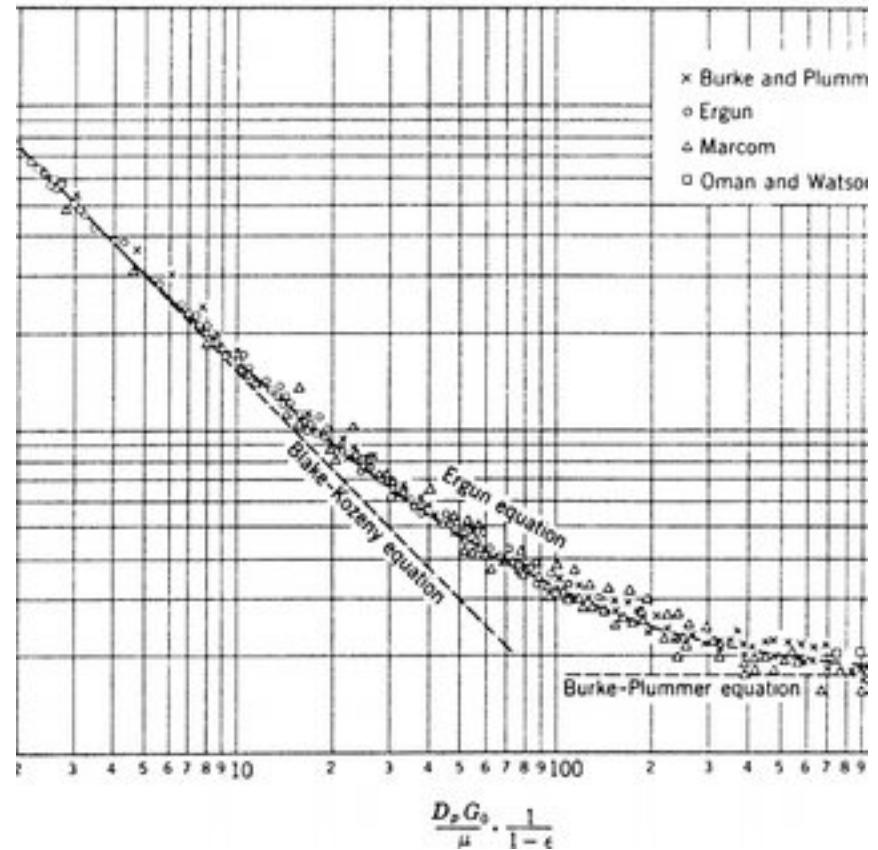
$$\frac{-\Delta P}{L} = \frac{150 \mu q (1-\varepsilon)^2}{(\psi D_p)^2 \varepsilon^3} + \frac{1.75 \rho q^2 (1-\varepsilon)}{\psi D_p \varepsilon^3}$$

- Ou

$$\frac{-\Delta P}{\rho q^2} \frac{\psi D_p}{L} \frac{\varepsilon^3}{(1-\varepsilon)} = \frac{150(1-\varepsilon)}{\rho q \psi D_p / \mu} + 1.75$$

- Onde

$$f_p = \frac{-\Delta P}{\rho q^2} \frac{\psi D_p}{L} \frac{\varepsilon^3}{(1-\varepsilon)} \quad Re_{leito} = \frac{\rho q \psi D_p}{\mu (1-\varepsilon)}$$



$$f_p = \frac{150}{Re_{leito}} + 1.75$$



Outras relações para perda de carga

- Tallmadge (1970) $0,1 < \text{Re} < 10^5$

$$f = \frac{150}{N_{Re}} + \frac{4,2}{N_{Re}^{1/6}}$$

Nemec e Levec (2005)

$$\frac{\Delta P}{L} = \frac{150}{\phi^{\frac{3}{2}}} \frac{(1 - \varepsilon)^2}{\varepsilon^3} \frac{\mu \cdot u}{(d_p \phi)^2} + \frac{1,75}{\phi^{\frac{4}{3}}} \frac{(1 - \varepsilon) \rho_f \cdot u^2}{\varepsilon^3 d_p \cdot \phi}$$

- Gibiliaro e Waldram (1985)

$$\frac{\Delta P}{L} = 17,3 \cdot \frac{\mu \cdot u}{d_p^2} \cdot \frac{(1 - \varepsilon)}{\varepsilon^{4,8}} + 0,366 \cdot \frac{\rho_f \cdot u^2}{d_p} \cdot \frac{(1 - \varepsilon)}{\varepsilon^{4,8}}$$



Conclusões

- Perda de carga em leito fixo
- Regimes laminar e turbulento
- Fluidodinâmica através de leito sólido



Bibliografia

- JM Coulson, JF Richardson, JR Backhurst, JH Harker, Chemical Engineering: Vol. 2. Particle Technology and Separation Processes, 6th ed., Butterworth-Heinemann, 2019.
- Foust, Wenzel, Clump et al., Princípios das Operações Unitárias, LTC; 2^a edição, 1982.
- Tallmadge, J.A.. Packed bed pressure drop – an extension to higher Reynolds numbers. A.I.C.H.E. Journal 16, 1092-1093, 1970.
- Gibilaro, L. G. et al. Generalized friction factor and drag coefficient correlations for fluid particle interactions. Chemical Engineering Science, v. 40, no. 10. p. 1817-1823, 1985.
- Nemec, D.; Levec, J. Flow through packed bed reactors: single-phase flow. Chemical Engineering Science, v. 60, p. 6947-6957, 2005.