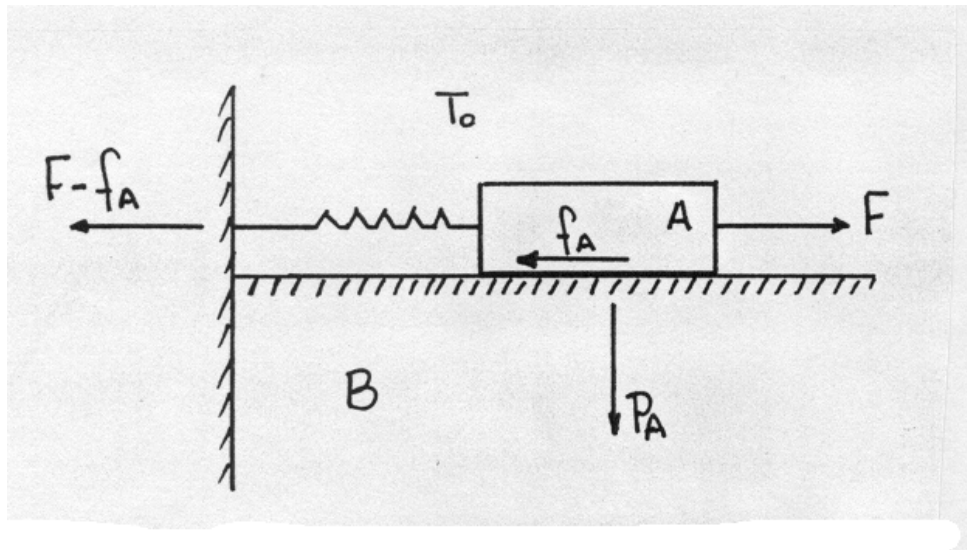


ENTROPY GENERATION ELEMENTARY PROCESSES

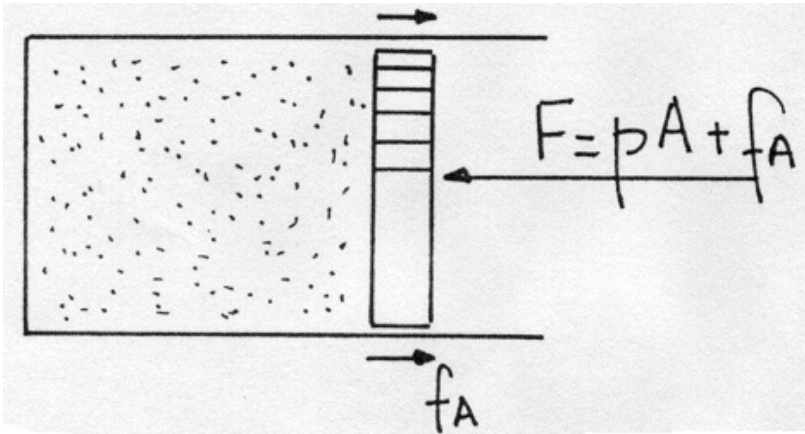
1. MECHANICAL FRICTION



$$f_A = \mu'_{AB} P_A \quad (1)$$

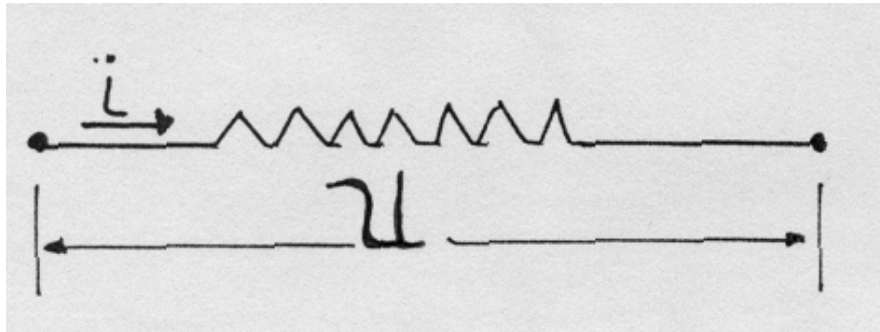
$$W_{friction} = f_A \cdot \Delta l \quad (\text{converted to heat}) \quad (2)$$

$$S_{gen} = \frac{W_{friction}}{T_0} = \frac{f_A \cdot \Delta \ell}{T_0} \quad (3)$$



$$S_{gen} = \sum \frac{\partial q_i}{T_i} \quad (4)$$

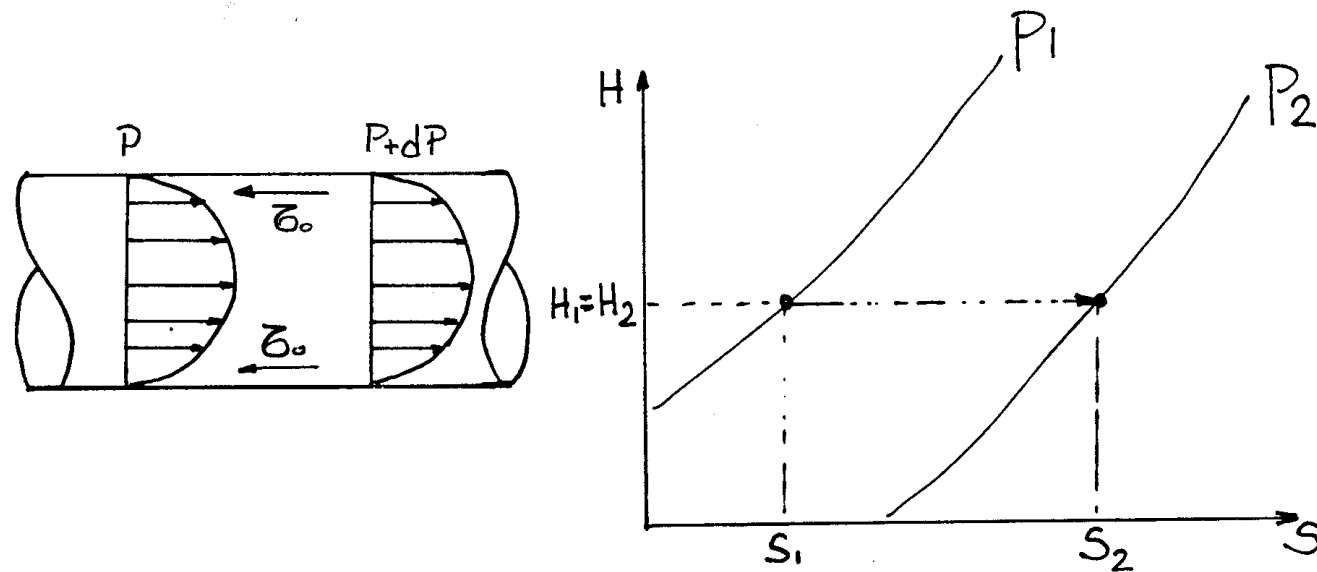
2. ELECTRICAL HEATING (Joule Effect)



$$S_{gen} = \frac{W_e}{T} = \frac{Ui}{T} \quad (5)$$

3. HEAD LOSS

Internal Flow



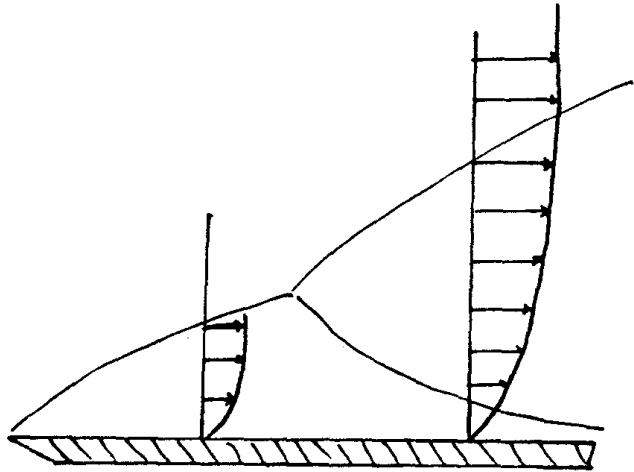
$$H_2 = H_1 \quad \text{and} \quad S_{gen} = (S_2 - S_1)\dot{m} \quad (6)$$

Considering

$$Tds = dh - vdp \quad (7)$$

For an isenthalpic process: $h = \text{cte} \rightarrow \frac{ds}{dp} = -\frac{v}{T}$ or $\left(\frac{\partial s}{\partial p}\right)_h = -\frac{v}{T}$ or $\partial p < 0$ and $\partial s > 0$

External Flow



$$dU = T_{\infty} dS - p_{\infty} dV$$

\Rightarrow

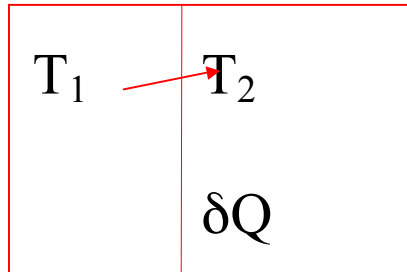
$$S_{gen} = \frac{F_A \cdot U_{\infty}}{T_{\infty}}$$

$$F_A \cdot U_{\infty} = \frac{dU}{dt} \quad (8)$$

$$S_{gen} = \frac{dS}{dt} \quad (9)$$

(10)

4. HEAT TRANSFER



$$dS_{sist} = S_{gen}$$

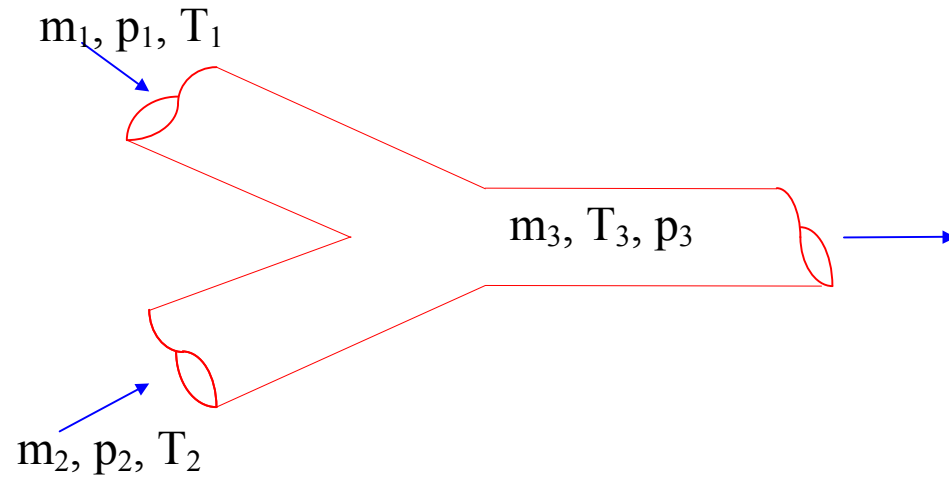
$$S_{gen} = (\Delta S)_1 + (\Delta S)_2 = \frac{-\partial Q}{T_1} + \frac{\partial Q}{T_2} \quad (11)$$

$$S_{gen} = \partial Q \frac{(T_1 - T_2)}{T_1 T_2}$$

$$T_{final} = \frac{C_1 T_1 + C_2 T_2}{C_1 + C_2} \quad (12)$$

with $C = m c$ (13)

5. MIXTURE



$$(\Delta S)_{CV} = S_{gen}$$

a) Same fluid

$$T_3 = \frac{m_1 T_1 + m_2 T_2}{(m_1 + m_2)} \quad ds = \frac{C_p dT}{T} - \frac{1}{\rho} \frac{dP}{T} \quad (14)$$

$$S_{gen} = m_3 s_3 - m_2 s_2 - m_1 s_1 \quad (15)$$

$$S_{gen} = m_1 (s_3 - s_1) + m_2 (s_3 - s_2) \quad (16)$$

$$S_{gen} = m_1 C_p \ln \frac{T_3}{T_1} + m_2 C_p \ln \frac{T_3}{T_2} - m_1 \left(\frac{1}{\rho T_1} (P_3 - P_1) \right) - m_2 \left(\frac{1}{\rho T_2} (P_3 - P_2) \right) \quad (17)$$

$$C_p = C \text{ (incompressible fluid)} \quad (18)$$

b) Mixture of perfect gases

$$\text{Equation of state: } p = \rho R T \quad (19)$$

$$\frac{1}{\rho} \frac{dp}{T} = R \frac{dp}{p} \quad (20)$$

$$S_{gen} = m_1 C_p \ln \frac{T_3}{T_1} + m_2 C_p \ln \frac{T_3}{T_2} - m_1 R_1 \ln \frac{(p_3)_1}{p_1} - m_2 R_2 \ln \frac{(p_3)_2}{P_p} \quad (21)$$

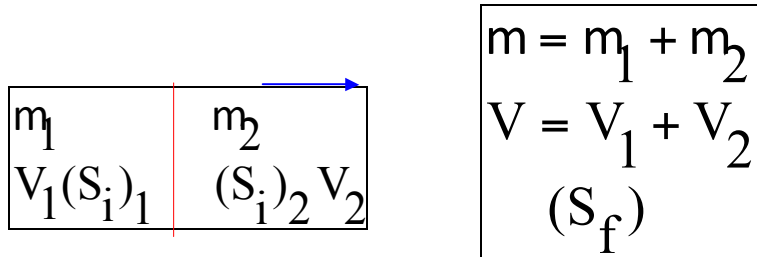
$(p_3)_1$ = Partial pressure of gas 1

$(p_3)_2$ = Partial pressure of gas 2

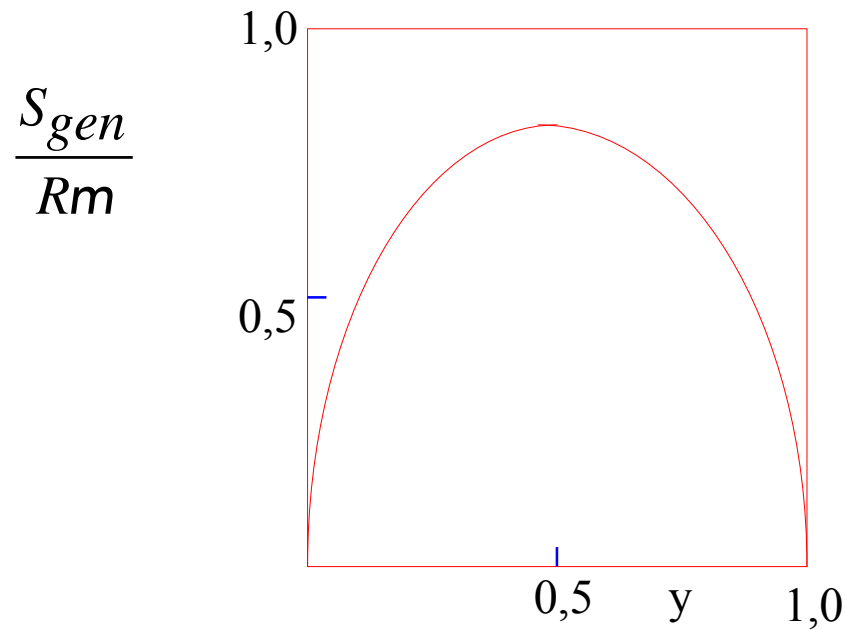
If: $p_1 = p_2 = p_3$

$$\left. \begin{array}{l} p_1 = p_2 = p_3 = p \\ \frac{(p_3)_1}{p} = \frac{m_1}{m} = y_1 \\ \frac{(p_3)_2}{p} = \frac{m_2}{m} = y_2 \end{array} \right\} S_{gen} = -Rm_1 \ln y_1 - Rm_2 \ln y_2 \quad (22)$$

$$\frac{S_{gen}}{Rm} = -\left[y_1 \ln y_1 + y_2 \ln y_2 \right] \quad (23)$$



For perfect gases, ΔS_{gen} is independent of the gas (O₂, N₂, H₂, etc.)



If there is only one gas then:

$$y_1 = y_2 = 1$$

and

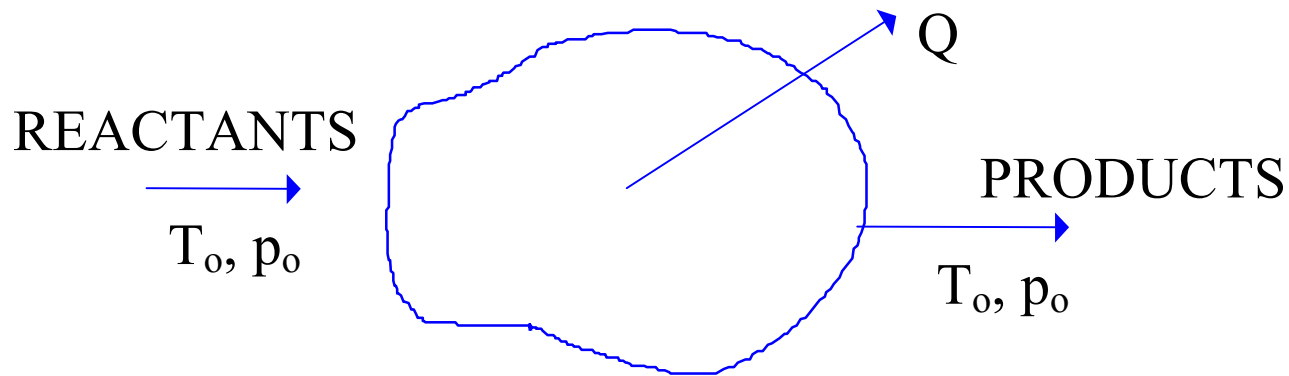
$$\therefore (S_{gen})_{mist} = 0$$

For a mixture with n gases at p , T ctes:

$$\frac{S_{gen}}{Rm} = \sum_{i=1}^n y_i \ln \frac{1}{y}; \quad (24)$$

$$\text{with } \sum y_i = 1 \quad (25)$$

6. CHEMICAL REACTION (COMBUSTION)



\bar{h} = molar partial enthalpy

\bar{s} = molar partial entropy

$$H_p - H_r = \frac{\dot{Q}}{\dot{n}_{fuel}}$$

(26)

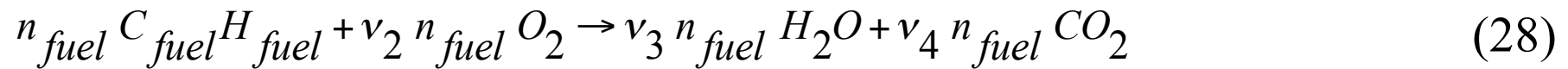
$$\sum_{i=1}^n \nu_{pi} \bar{h}_{pi} - \sum_{i=1}^m \nu_{ri} \bar{h}_{ri} = \dot{Q} / \dot{n}_{fuel} \quad (27)$$

with $\nu_{r1} = 1$

$$\dot{n}_{ri} = \nu_{ri} \dot{n}$$

$$\dot{n}_{pi} = \nu_{pi} \dot{n}$$

\dot{n} = reaction velocity



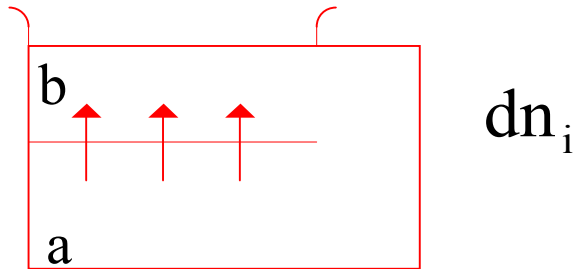
$$\frac{1}{\dot{n}_{fuel}} S_{gen} = -\frac{\dot{Q}}{\dot{n}_{fuel} T_o} - \sum v_{ri} \bar{s}_{ri} + \sum v_{pi} \bar{s}_{pi} \quad (29)$$

$$S_{gen} = (\sum v_{ri} \mu_{ri} - \sum v_{pi} \bar{\mu}_{pi}) \frac{\dot{n}_{fuel}}{T_o} \quad (30)$$

$$S_{gen} = \frac{A}{T_o} \dot{n}_{fuel} \quad (31)$$

$$A = \left(\sum v_{ri} \mu_{ri} - \sum v_{pi} \mu_{pi} \right) = \text{chemical affinity} \quad (32)$$

7. DIFFUSION



Chemical potential reduction:

$$S_{gen} = \frac{dn_i}{T} (\mu_i(a) - \mu_i(b)) \quad (33)$$