



Fenômenos de Transporte **ADIMENSIONALIZAÇÃO**

Expressão das equações de **Fenômenos de Transporte** na forma adimensionalizada

- **Números ADIMENSIONAIS**
(Re, Pr, Sc, Pe, Gr, Sh, Nu etc.)
 - Correlações semi-empíricas generalizadas
 - Analogia dos FT's
- **“SCALING”**
Identificação das ordens de grandeza
 - Simplificação das equações (equações aproximadas)
 - Resultados semi-quantitativos
- **CFD** _Fluidodinâmica Computacional
 - Simplificação das equações (equações aproximadas)
 - Elaboração de critérios e modelos



ADIMENSIONALIZAÇÃO

PARÂMETROS CARACTERÍSTICOS: t_0, ρ_0, v_0, L

ADIMENSIONALIZAÇÃO DAS VARIÁVEIS: $\hat{\rho} = \frac{\rho}{\rho_0}$; $\hat{v} = \frac{\vec{v}}{v_0}$; $\hat{r} = \frac{\vec{r}}{L}$; $\hat{t} = \frac{t}{t_0}$

$$\rho = \rho_0 \hat{\rho} \quad ; \quad \vec{v} = v_0 \hat{v} \quad ; \quad \vec{r} = L \hat{r} \quad ; \quad t = t_0 \hat{t}$$

ADIMENSIONALIZAÇÃO DOS OPERADORES:

$$\text{grãd} () = L \text{grãd} () \quad ; \quad \text{div} () = L \text{div} () \quad ; \quad \text{lãp} () = \text{div} \text{grãd} () = L^2 \text{lãp} ()$$

$$\frac{\partial}{\partial t} = \frac{1}{t_0} \frac{\partial}{\partial \hat{t}}$$

$$\frac{\partial f}{\partial \mathbf{x}} = \frac{\partial (\hat{f} f_0)}{\partial (\hat{\mathbf{x}} x_0)} = \frac{f_0}{x_0} \frac{\partial \hat{f}}{\partial \hat{\mathbf{x}}}$$

$$\frac{\partial^2 f}{\partial \mathbf{x}^2} = \frac{\partial}{\partial \mathbf{x}} \left(\frac{\partial f}{\partial \mathbf{x}} \right) = \frac{\partial}{\partial (\hat{\mathbf{x}} x_0)} \left(\frac{\partial (\hat{f} f_0)}{\partial (\hat{\mathbf{x}} x_0)} \right) = \frac{f_0}{x_0^2} \frac{\partial}{\partial \hat{\mathbf{x}}} \left(\frac{\partial \hat{f}}{\partial \hat{\mathbf{x}}} \right) = \frac{f_0}{x_0^2} \frac{\partial^2 \hat{f}}{\partial \hat{\mathbf{x}}^2}$$

Equação da Continuidade

$$\frac{\partial \rho}{\partial t} = - \operatorname{div} \rho \vec{v}$$

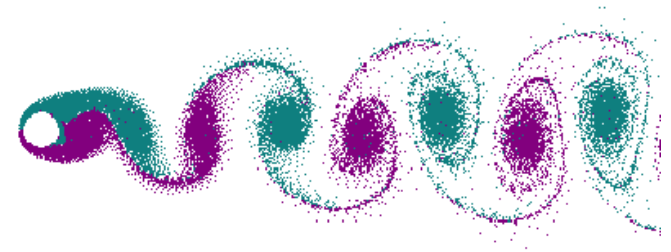
$$\frac{\rho_0}{t_0} \frac{\partial \hat{\rho}}{\partial \hat{t}} = - \frac{\rho_0 v_0}{L} \operatorname{div} \hat{\rho} \hat{v} \quad \Rightarrow \quad \frac{L}{t_0 v_0} \frac{\partial \hat{\rho}}{\partial \hat{t}} = - \operatorname{div} \hat{\rho} \hat{v}$$

$$\frac{1}{\operatorname{Sr}} \frac{\partial \hat{\rho}}{\partial \hat{t}} = - \operatorname{div} \hat{\rho} \hat{v}$$

STROUHAL

$$\operatorname{Sr} = \frac{t_0 v_0}{L}$$

$$\operatorname{Sr} = \frac{\Omega D}{v_0}$$



**t_0 : tempo para o escoamento “atingir o regime permanente”
ou associado à frequência em processo periódico**

Ω : frequência em processo periódico

Equação de Conservação Generalizada

Balanço microscópico de ϕ :

$$\rho \frac{D\phi}{Dt} = \frac{\partial \rho \phi}{\partial t} + \text{div}(\rho \phi \vec{v}) = -\text{div} \vec{j}_\phi + \dot{\sigma}_{V\phi}$$

$$\frac{\partial \rho \phi}{\partial t} + \text{div}(\rho \vec{v} \phi + \vec{j}_\phi) = \dot{\sigma}_{V\phi}$$

Equação constitutiva de difusão:

$$\vec{j}_\phi = -\rho \Gamma_\phi \text{grad } \phi$$

ϕ	Γ_ϕ	v/Γ_ϕ
V	v	1
w_A	D_{AB}	Sc
$c_p T$	α	Pr

$$\frac{\partial \rho \phi}{\partial t} + \text{div} \rho (\vec{v} \phi - \Gamma_\phi \text{grad } \phi) = \dot{\sigma}_{V\phi}$$

Equação de Conservação Generalizada

$$\frac{\partial \rho \varphi}{\partial t} + \text{div} \rho \left(\vec{v} \varphi - \Gamma_{\varphi} \text{grad} \varphi \right) = \dot{\sigma}_{\nabla_{\varphi}}$$

$$\rho = \rho_0 \hat{\rho} \quad ; \quad \vec{v} = v_0 \hat{v} \quad ; \quad \vec{r} = L \hat{r} \quad ; \quad t = t_0 \hat{t} \quad ; \quad \varphi = \hat{\varphi} \Delta \varphi + \varphi_0$$

$$\frac{1}{t_0} \frac{\partial \rho_0 \hat{\rho} (\hat{\varphi} \Delta \varphi + \varphi_0)}{\partial \hat{t}} + \frac{1}{L} \hat{\text{div}} \hat{\rho} \left(\rho_0 v_0 \hat{v} (\hat{\varphi} \Delta \varphi + \varphi_0) - \frac{\rho_0}{L} \Gamma_{\varphi} \text{grâd} (\hat{\varphi} \Delta \varphi + \varphi_0) \right) = \dot{\sigma}_{\nabla_{\varphi}}$$

Reagrupando-se os termos:

$$\varphi_0 \frac{\rho_0 v_0}{L} \underbrace{\left[\frac{L}{t_0 v_0} \frac{\partial \hat{\rho}}{\partial \hat{t}} + \hat{\text{div}} (\hat{\rho} \hat{v}) \right]}_{=0, \text{continuidade}} + \frac{\rho_0 \Delta \varphi}{t_0} \frac{\partial (\hat{\rho} \hat{\varphi})}{\partial \hat{t}} + \frac{\rho_0 v_0 \Delta \varphi}{L} \left[\hat{\text{div}} (\hat{\rho} \hat{v} \hat{\varphi}) - \hat{\text{div}} \hat{\rho} \left(\frac{\Gamma_{\varphi}}{v_0 L} \text{grâd} \hat{\varphi} \right) \right] = \dot{\sigma}_{\nabla_{\varphi}}$$

Equação de Conservação Generalizada

$$\frac{\partial \rho \phi}{\partial t} + \text{div } \rho \left(\vec{v} \phi - \Gamma_{\phi} \text{grad } \phi \right) = \dot{\sigma}_{\nabla_{\phi}}$$

$$\frac{L}{v_0 t_0} \frac{\partial (\hat{\rho} \hat{\phi})}{\partial \hat{t}} + \text{div } \hat{\rho} \left(\hat{v} \hat{\phi} - \frac{\Gamma_{\phi}}{v_0 L} \text{grad } \hat{\phi} \right) = \frac{\dot{\sigma}_{\nabla_{\phi}} L}{\rho_0 v_0 \Delta \phi} \Rightarrow$$

$$\frac{1}{\text{Sr}} \frac{\partial \hat{\rho} \hat{\phi}}{\partial \hat{t}} + \text{div } \hat{\rho} \left(\hat{v} \hat{\phi} - \frac{1}{\text{Pe}} \text{grad } \hat{\phi} \right) = \frac{\dot{\sigma}_{\nabla_{\phi}} L}{\rho_0 \Delta \phi v_0}$$

PECLET

$$\text{Pe} = \frac{v_0 L}{\Gamma_{\phi}} = \frac{v}{\Gamma_{\phi}} \frac{v_0 L}{v} = \text{Re} \frac{v}{\Gamma_{\phi}}$$

$$\text{Pe} = \text{Re} \frac{v}{\Gamma_{\phi}}$$

Equação de Conservação Generalizada

ADIMENSIONAIS

PECLET

$$Pe = Re \frac{v}{\Gamma_{\phi}}$$

CONVECÇÃO / DIFUSÃO

**PECLET
MÁSSICO**

$$Pe = Re Sc$$

**PECLET
TÉRMICO**

$$Pe = Re Pr$$

PRANDTL

$$Pr = \frac{v}{\alpha}$$

$$\alpha = \frac{k}{\rho C_p}$$

SCHMIDT

$$Sc = \frac{v}{D_{AB}}$$

ϕ	Γ_{ϕ}	v/Γ_{ϕ}
V	v	1
w_A	D_{AB}	Sc
$c_p T$	α	Pr

Equação de Energia

$$\frac{1}{\text{Sr}} \frac{\partial(\hat{\rho}\hat{\phi})}{\partial\hat{t}} + \text{div}\hat{\rho} \left(\hat{\mathbf{v}}\hat{\phi} - \frac{1}{\text{Pe}} \text{gr\^ad}\hat{\phi} \right) = \frac{\dot{\sigma}_{\nabla\phi} L}{\rho_0 v_0 \Delta\phi} \Rightarrow$$

$$\varphi = \text{CpT}, \quad \text{Cp cte} \quad \hat{T} = \frac{T - T_0}{T_s - T_0} = \frac{T - T_0}{\Delta T}$$

$$\frac{1}{\text{Sr}} \frac{\partial\hat{\rho}\hat{T}}{\partial\hat{t}} + \text{div}\hat{\rho} \left(\hat{\mathbf{v}}\hat{T} - \frac{1}{\text{Pe}} \text{gr\^ad}\hat{T} \right) = \frac{\dot{\sigma}_{\nabla\phi} L}{\rho_0 c_p \Delta T v_0}$$

Para dissipação viscosa:

$$\dot{\sigma}_{\nabla T} = \mu \Phi_{\nabla}$$

$$\Rightarrow \frac{\mu \Phi_{\nabla} L}{\rho_0 c_p \Delta T v_0} = \frac{1}{\text{Pe}} \frac{\mu \Phi_{\nabla} L^2}{k \Delta T} = \frac{\text{Br}}{\text{Pe}}$$

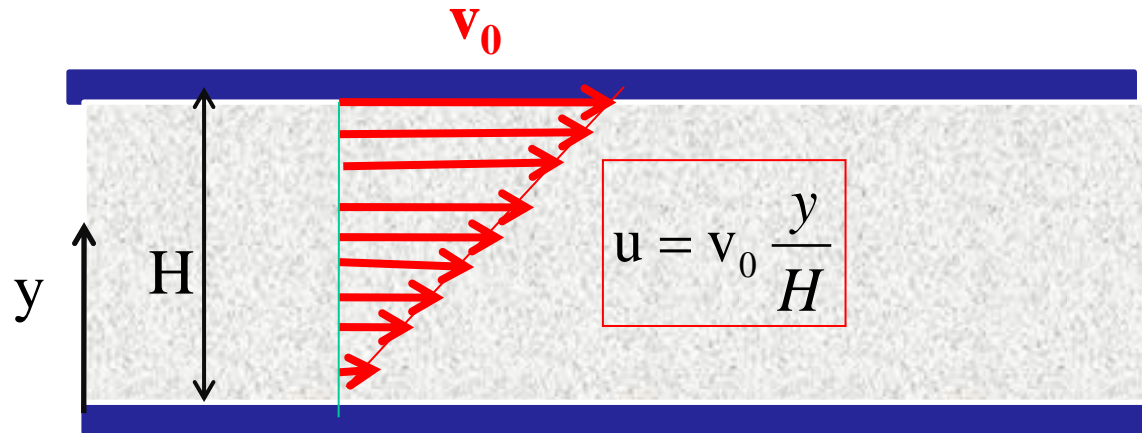
BRINKMAN

$$\text{Br} = \frac{\mu \Phi_{\nabla} L^2}{k \Delta T}$$

Equação de Energia - **BRINKMAN**

$$\frac{1}{\text{Sr}} \frac{\partial \hat{\rho} T}{\partial \hat{t}} + \text{div} \hat{\rho} \left(\hat{\mathbf{v}} \hat{T} - \frac{1}{\text{Pe}} \text{grãd} \hat{T} \right) = \frac{\text{Br}}{\text{Pe}}$$

Caso particular: perfil linear de velocidade



$$\mu \Phi_{\nabla} = \mu \left(\frac{\partial v}{\partial y} \right)^2 = \mu \left(\frac{v_0}{L} \right)^2$$

$$L = H$$

$$\text{Br} = \frac{\mu \Phi_{\nabla} L^2}{k \Delta T} = \frac{\mu v_0^2}{k \Delta T}$$

Não depende de L !!

Navier-Stokes

Pressão Modificada- Piezométrica

Navier-Stokes:

$$\rho \frac{\partial \vec{v}}{\partial t} + \rho \vec{v} \cdot \text{grad} \vec{v} = \rho \vec{g} - \text{grad} p + \mu \text{lap} \vec{v}$$

**Força de campo,
gradiente do
potencial U**

$$\begin{aligned}\vec{g} &= \vec{f} = - \text{grad} U \\ \rho \vec{g} &= - \rho \text{grad} U \\ \rho \vec{g} &= - \text{grad} \rho U \quad (\text{grad} \rho = 0)\end{aligned}$$

z orientado “para cima”

$$\begin{aligned}U &= g z + cte \\ \text{grad} U &= - \vec{g}\end{aligned}$$

$$\rho \vec{g} - \text{grad} p = - \text{grad} \rho U - \text{grad} p = - \text{grad} (\rho U + p)$$

Pressão modificada:

$$P = \rho U + p = \rho g z + p$$

$$\text{grad} P = -\rho \vec{g} + \text{grad} p$$

Navier-Stokes - Adimensionalização

$$\vec{g}rad P = -\rho \vec{g} + \vec{g}rad p$$

Substituindo-se na
Navier-Stokes:

$$\rho \frac{\partial \vec{v}}{\partial t} + \rho \vec{v} \cdot \vec{g}rad \vec{v} = \rho \vec{g} - \underbrace{\vec{g}rad p}_{-\vec{g}rad P} + \mu lap \vec{v}$$

Adimensionalizando-se:

$$\hat{P} = \frac{P}{P_0}$$

$$P_0 = \rho g z_0 + cte + p_0$$

$$\frac{1}{Sr} \frac{\partial \hat{v}}{\partial \hat{t}} + \hat{v} \cdot \hat{g}rad \hat{v} = -\frac{1}{Ru} \vec{g}rad \hat{P} + \frac{1}{Re} lap \hat{v}$$

RUARK

EULER

$$Ru = \frac{\rho v_0^2}{P_0}$$

Navier-Stokes - Adimensionalização

$$Ru = \frac{\rho v_0^2}{P_0}$$

$$Re = \frac{v_0 L}{\nu}$$

Regime permanente

$$\hat{\mathbf{v}} \cdot \hat{\text{grad}} \hat{\mathbf{v}} = -\frac{1}{Ru} \hat{\text{grad}} \hat{P} + \frac{1}{Re} \hat{\text{lap}} \hat{\mathbf{v}}$$

Euler – invíscido

$$Re \rightarrow \infty$$

Escoamento externo (camada limite)

$$\hat{\mathbf{v}} \cdot \hat{\text{grad}} \hat{\mathbf{v}} = -\frac{1}{Ru} \hat{\text{grad}} \hat{P}$$

“Creeping flow”

$$Re \rightarrow 0$$

Leito poroso (filtração, solo)

$$-\frac{1}{Ru} \hat{\text{grad}} \hat{P} + \frac{1}{Re} \hat{\text{lap}} \hat{\mathbf{v}} = 0$$

Incompressível

$$\hat{\text{lap}} \hat{P} = 0$$

Equação da Continuidade para espécie A:

$$\frac{L}{v_0 t_0} \frac{\partial(\hat{\rho}\hat{\phi})}{\partial \hat{t}} + \text{div} \hat{\rho} \left(\hat{\mathbf{v}}\hat{\phi} - \frac{1}{\text{Pe}} \text{grãd } \hat{\phi} \right) = \frac{\dot{\sigma}_{\nabla\phi} L}{\rho_0 v_0 \Delta\phi} \Rightarrow$$

$$\varphi = \omega_A \quad \text{fração mássica} \quad \hat{\phi} = \hat{\omega}_A = \frac{\omega_A - \omega_{A0}}{\omega_{AS} - \omega_{A0}}$$

Reação química

Equação Cinética:

$$\dot{\sigma}_{\nabla T} = r_A \left(\frac{\text{kg de A}}{\text{m}^3 \text{s}} \right)$$

$$\frac{1}{\text{Sr}} \frac{\partial \hat{\rho} \hat{\omega}_A}{\partial \hat{t}} + \text{div} \hat{\rho} \left(\hat{\mathbf{v}} \hat{\omega}_A - \frac{1}{\text{Pe}} \text{grãd } \hat{\omega}_A \right) = \frac{r_A L}{\rho_0 \Delta\omega_A v_0}$$

Equação da Continuidade para espécie A – Escalas de tempos:

$$\frac{L}{t_0 v_0} \frac{\partial \hat{\rho} \hat{\omega}_A}{\partial \hat{t}} + \text{div} \hat{v} \hat{\rho} \left(\hat{v} \hat{\omega}_A - \frac{D_{AB}}{v_0 L} \text{grad} \hat{\omega}_A \right) = \frac{r_A L}{\rho_0 \Delta \omega_A v_0}$$

$$\frac{L}{t_0 v_0} \frac{\partial \hat{\rho} \hat{\omega}_A}{\partial \hat{t}} + \text{div} \hat{v} \hat{\rho} \hat{v} \hat{\omega}_A = \frac{D_{AB}}{v_0 L} \text{láp} \hat{\omega}_A + \frac{r_A L}{\rho_0 \Delta \omega_A v_0}$$

$$\frac{1}{t_0} \frac{\partial \hat{\rho} \hat{\omega}_A}{\partial \hat{t}} + \frac{v_0}{L} \text{div} \hat{v} \hat{\rho} \hat{v} \hat{\omega}_A = \frac{D_{AB}}{L^2} \text{láp} \hat{\omega}_A + \frac{r_A}{\rho_0 \Delta \omega_A}$$

$$\frac{1}{t_0} \frac{\partial \hat{\rho} \hat{\omega}_A}{\partial \hat{t}} + \frac{1}{t_C} \text{div} \hat{v} \hat{\rho} \hat{v} \hat{\omega}_A = \frac{1}{t_D} \text{láp} \hat{\omega}_A + \frac{1}{t_R}$$

Conveccção

$$t_C = \frac{L}{v_0}$$

Difusão

$$t_D = \frac{L^2}{D_{AB}}$$

Reação

$$t_R = \frac{\rho_0 \Delta \omega_A}{r_A}$$

Equação da Continuidade para espécie A:

$$\frac{1}{\text{Sr}} \frac{\partial \hat{\rho} \hat{\omega}_A}{\partial \hat{t}} + \text{div} \hat{v} \hat{\rho} \left(\hat{v} \hat{\omega}_A - \frac{1}{\text{Pe}} \text{grad} \hat{\omega}_A \right) = \frac{r_A L}{\rho_0 \Delta \omega_A v_0}$$

$$\frac{1}{\text{Pe}} = \frac{L}{v_0} \frac{D_{AB}}{L^2} = \frac{t_C}{t_D}$$

$$\frac{r_A L}{\rho_0 \Delta \omega_A v_0} = \frac{t_C}{t_R} = \text{Da}_1$$

DAMKÖHLER 1

$$\frac{1}{\text{Sr}} \frac{\partial \hat{\rho} \hat{\omega}_A}{\partial \hat{t}} + \text{div} \hat{v} \hat{\rho} \left(\hat{v} \hat{\omega}_A - \frac{1}{\text{Pe}} \text{grad} \hat{\omega}_A \right) = \text{Da}_1$$

Equação da Continuidade para espécie A:

$$\frac{1}{\text{Sr}} \frac{\partial \hat{\rho} \hat{\omega}_A}{\partial \hat{t}} + \text{div} \hat{\rho} \left(\hat{\mathbf{v}} \hat{\omega}_A - \frac{1}{\text{Pe}} \text{gr} \hat{\omega}_A \right) = \frac{r_A L}{\rho_0 \Delta \omega_A v_0}$$

x Pe:

$$\frac{\text{Pe}}{\text{Sr}} \frac{\partial \hat{\rho} \hat{\omega}_A}{\partial \hat{t}} + \text{div} \hat{\rho} \left(\text{Pe} \hat{\mathbf{v}} \hat{\omega}_A - \text{gr} \hat{\omega}_A \right) = \frac{r_A L^2}{\rho_0 \Delta \omega_A D_{AB}}$$

Tempo de Reação:

$$t_R = \frac{\rho_0 \Delta \omega_A}{r_A}$$

Tempo de Difusão:

$$t_D = \frac{L^2}{D_{AB}}$$

$$\frac{r_A L^2}{\rho_0 \Delta \omega_A D_{AB}} = \frac{t_D}{t_R} = \text{Da}_2$$

DAMKÖHLER 2

$$\frac{\text{Pe}}{\text{Sr}} \frac{\partial \hat{\rho} \hat{\omega}_A}{\partial \hat{t}} + \text{div} \hat{\rho} \left(\text{Pe} \hat{\mathbf{v}} \hat{\omega}_A - \text{gr} \hat{\omega}_A \right) = \text{Da}_2$$

Reação/difusão em poros de catalisador sólido –

$$\text{Módulo de Thiele} = \text{Th} = (\text{Da}_2)^{0,5}$$

Coeficientes Convectivos

ADIMENSIONALIZAÇÃO

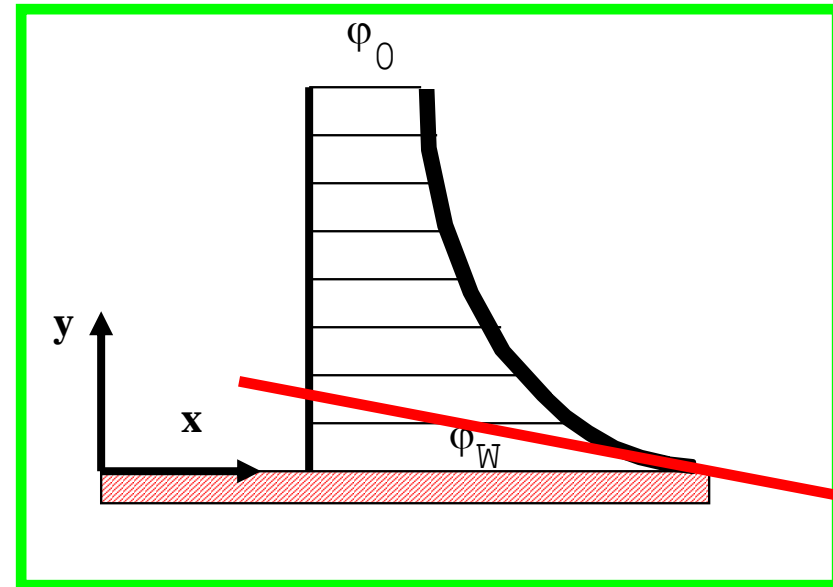
$$\frac{1}{\text{Sr}} \frac{\partial \hat{\rho} \hat{\phi}}{\partial \hat{t}} + \text{div} \hat{\rho} \left(\hat{\mathbf{v}} \hat{\phi} - \frac{1}{\text{Pe}} \text{grad} \hat{\phi} \right) = \frac{\dot{\sigma}_{\nabla \phi} L}{\rho_0 \Delta \phi v_0}$$

ESCOAMENTO + DIFUSÃO

INTERFACE / PAREDE

COEFICIENTE DE CONVECÇÃO

$$\vec{j}_{\phi, \text{parede}} = CO_{\phi} (\varphi_S - \varphi_0)$$

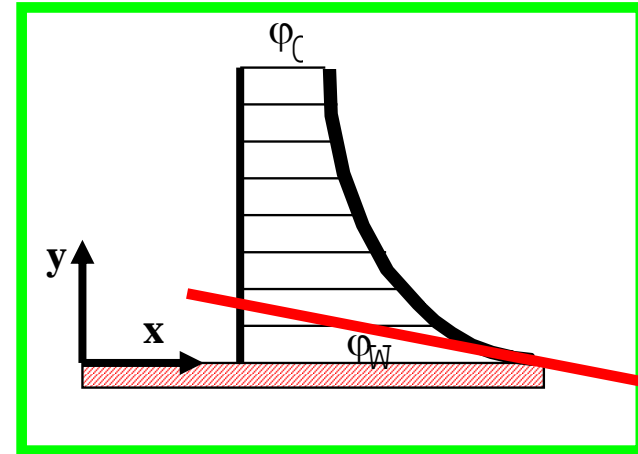


grad φ

Coeficientes Convectivos

ADIMENSIONAIS

$$\frac{1}{Sr} \frac{\partial \hat{\rho} \hat{\phi}}{\partial \hat{t}} + \text{div} \hat{\rho} \left(\underbrace{\hat{v} \hat{\phi} - \frac{1}{Pe} \text{grad} \hat{\phi}}_{\text{NA PAREDE } \hat{v}=0} \right) = \frac{\dot{\sigma}_{\nabla \phi} L}{\rho_0 \Delta \phi v_0}$$



NUSSELT

$$Nu = \left(\text{grad} \hat{T} \right)_{\hat{r}=0} = \frac{hL}{k}$$

CALOR

grad ϕ

SHERWOOD

$$Sh = \left(\text{grad} \hat{w}_i \right)_{\hat{r}=0} = \frac{kL}{D_{AB}}$$

MASSA

FATOR DE ATRITO

$$f = \frac{1}{Re} \left(\text{grad} \hat{v} \right)_{\hat{r}=0}$$

QUANTIDADE DE MOVIMENTO

ADIMENSIONAIS –ANALOGIA de REYNOLDS

NÚMERO DE STANTON

St = NÚMERO DE STANTON

QUANTIDADE DE MOVIMENTO

$$St = \frac{f}{2}$$

FATOR DE FANNING

CALOR

$$St = \frac{Nu}{Pe} = \frac{Nu}{Re Pr} = \frac{h}{\rho c_p V}$$

MASSA

$$St = \frac{Sh}{Pe} = \frac{Sh}{Re Sc} = \frac{k}{V}$$

ADIMENSIONAIS –ANALOGIA DE COLBURN

FATOR j

QUANTIDADE DE
MOVIMENTO

$$\frac{f}{2} = j_H = j_M$$

FATOR DE
FANNING

CALOR

$$j_H = \frac{Nu}{Re Pr^{1/3}}$$

MASSA

$$j_M = \frac{Sh}{Re Sc^{1/3}}$$