

# Processamento Térmico Descontínuo e Contínuo de Alimentos: Conceitos e Cálculos Preditivos

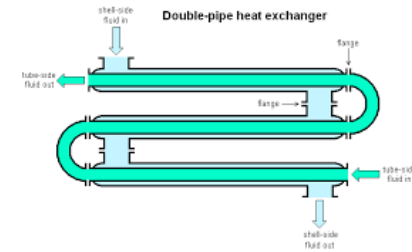
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PROFA. DRA. CYNTHIA DITCHFIELD

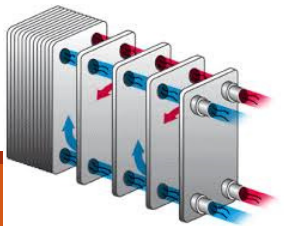




# Processo Térmico de Alimentos

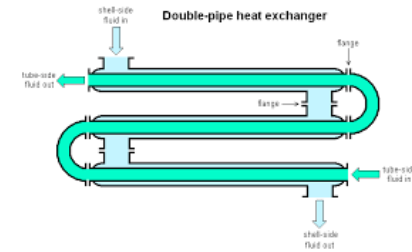


- Conceitos
- Curvas de penetração de calor
- Cinética de destruição microbiana
- Processo térmico contínuo
- Processo térmico descontínuo

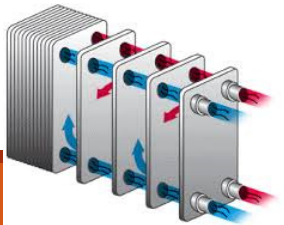




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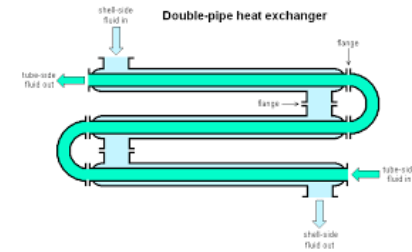


- Processo térmico: uso do calor para estender a vida de prateleira do produto
- Determinar a combinação de tempo-temperatura que resulte:
  - ✓ Produto seguro (Saúde pública)
  - ✓ Longa vida de prateleira (Comercial)
  - ✓ Alta qualidade nutricional e sensorial (Consumidor)





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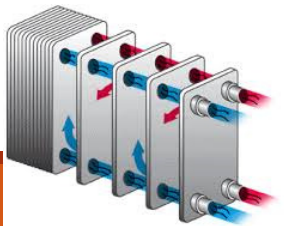


## ➤ Critérios:

- ✓ Destruição de microrganismos
- ✓ Inativação de enzimas

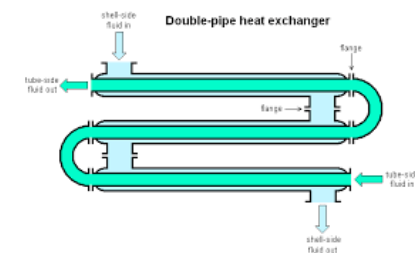
## ➤ Restrições:

- ✓ Preservação de nutrientes
- ✓ Controle da textura





# Processo Térmico de Alimentos

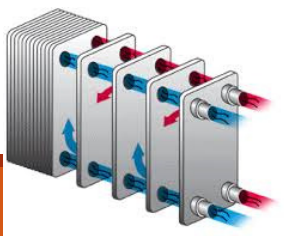


## ➤ Tipos de Processo Térmico:

## ✓ Branqueamento

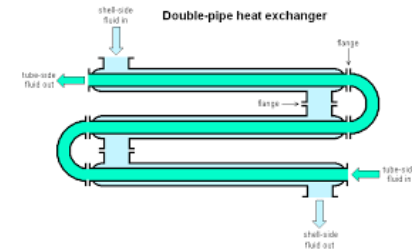
- Remoção de gases dos tecidos
- Pré-tratamento de frutas e vegetais
- Imersão em água fervente ou vapor fluente

- Inativação de enzimas
- Limpeza e amolecimento do tecido
- Redução inicial de microrganismos





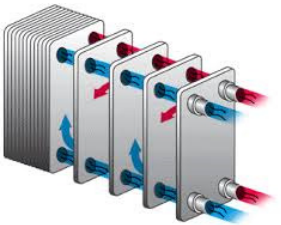
# Processo Térmico de Alimentos



## ➤ Tipos de Processo Térmico: ✓ Pasteurização

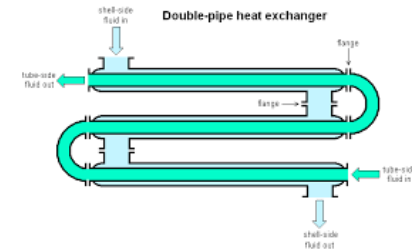
- Eliminação de microrganismos patogênicos (células vegetativas)
- Temperaturas mais brandas de processo
- Inativação de enzimas

- Combinação com outros tratamentos (refrigeração, aditivos químicos, embalagem, fermentação,....)



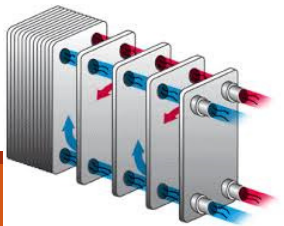


# Processo Térmico de Alimentos



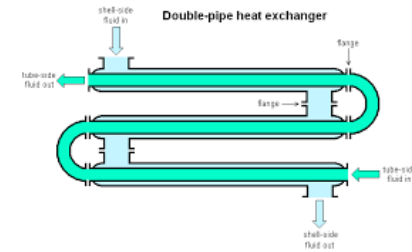
## ➤ Tipos de Processo Térmico: ✓ Esterilização

- Nenhum microrganismo viável no alimento
- Estável em temperatura ambiente
- Esterilidade comercial



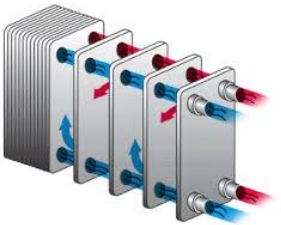


# Processo Térmico de Alimentos



## ➤ Condições de processo

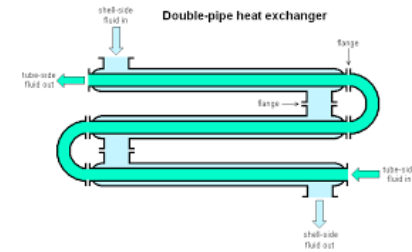
- Características intrínsecas do alimento: pH, força iônica, potencial redox, nível de oxigênio
- Armazenamento pós processo
- Microrganismos ou esporos de interesse





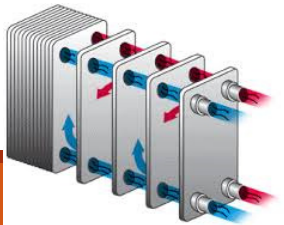


# Processo Térmico de Alimentos



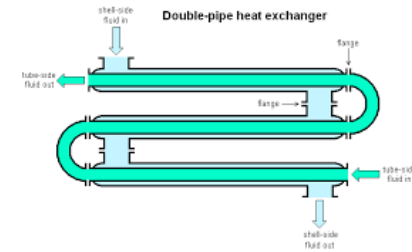
## ➤ Condições de processo

- Contaminação inicial
- Propriedades termofísicas do alimento
- Modo de transferência de calor
- Tamanho e forma da embalagem





# Processo Térmico de Alimentos

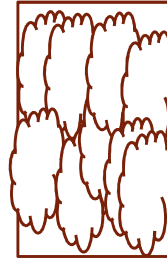
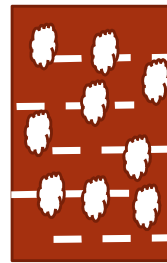
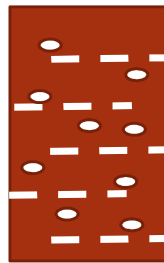
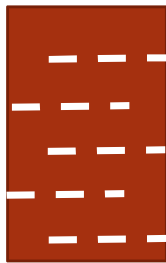


## Modos de Transferência de Calor em Latas

Aquecimento por convecção

Aquecimento por convecção e condução

Aquecimento por condução



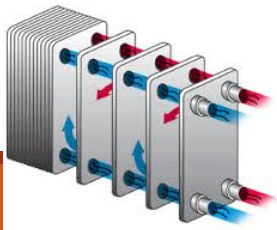
Alimento fluido

Partículas em líquido

Partículas num líquido viscoso

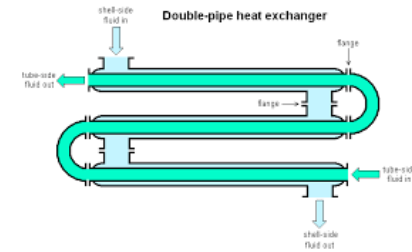
Alimento em camadas densas

Alimento sólido empacotado

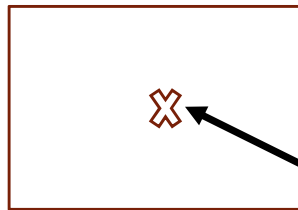




# Processo Térmico de Alimentos

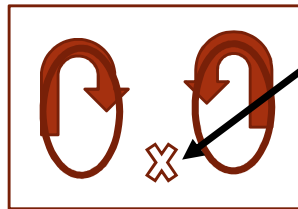


## Localização do Ponto Frio em Latas

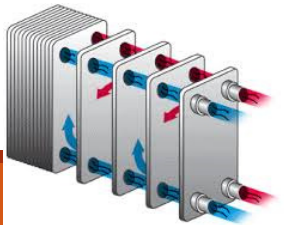


Aquecimento por condução (sólido)

Ponto frio

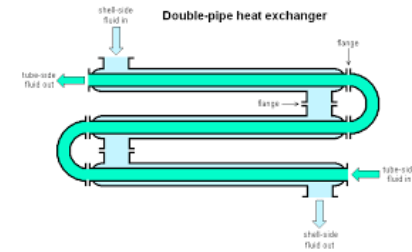


Aquecimento por convecção (líquido)





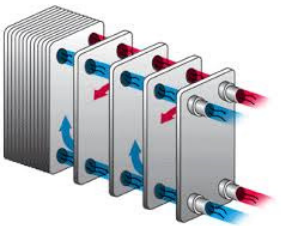
# Processo Térmico de Alimentos



## ➤ Definição do Processo Térmico

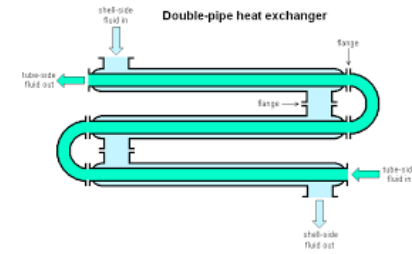
### ✓ Destruição de microrganismos

- Tempo e Temperatura : Letalidade
- Taxas de Inativação – decaimento logarítmico
- Exposição a uma temperatura constante: aumento da inativação com aumento do tempo e da temperatura
- Reação de Primeira ordem

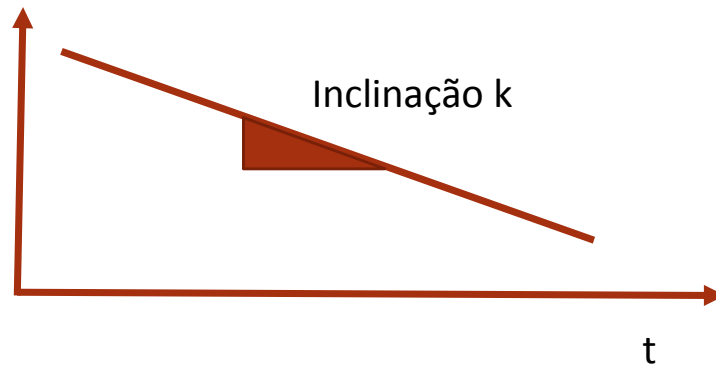




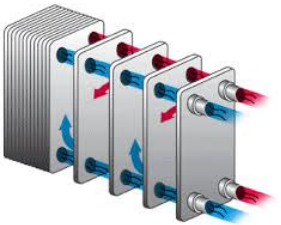
# Processo Térmico de Alimentos



Log N

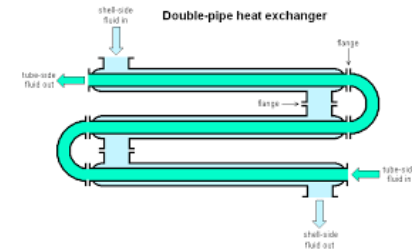


N = número de microrganismos viáveis





# Processo Térmico de Alimentos



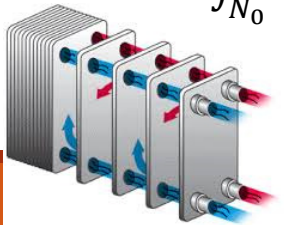
$$\frac{dN}{dt} = -kN \quad (1)$$

Separando as variáveis:

$$\frac{dN}{N} = -k dt \quad (2)$$

Integrando e considerando que para  $t = 0$ ,  $N = N_0$ :

$$\int_{N_0}^N \frac{dN}{N} = - \int_0^t k dt \quad (3)$$



Considerando que  $k$  é constante:

$$\ln \left( \frac{N}{N_0} \right) = -kt \quad (4)$$

Transformando para logaritmo decimal:

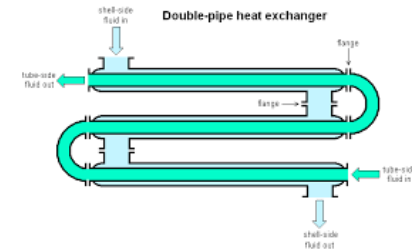
$$2,303 \log \left( \frac{N}{N_0} \right) = -kt; \log \left( \frac{N}{N_0} \right) = - \frac{k}{2,303} t \quad (5)$$

Como  $D = 2,303/k$ :

$$\log \left( \frac{N}{N_0} \right) = - \frac{t}{D} \quad (6)$$

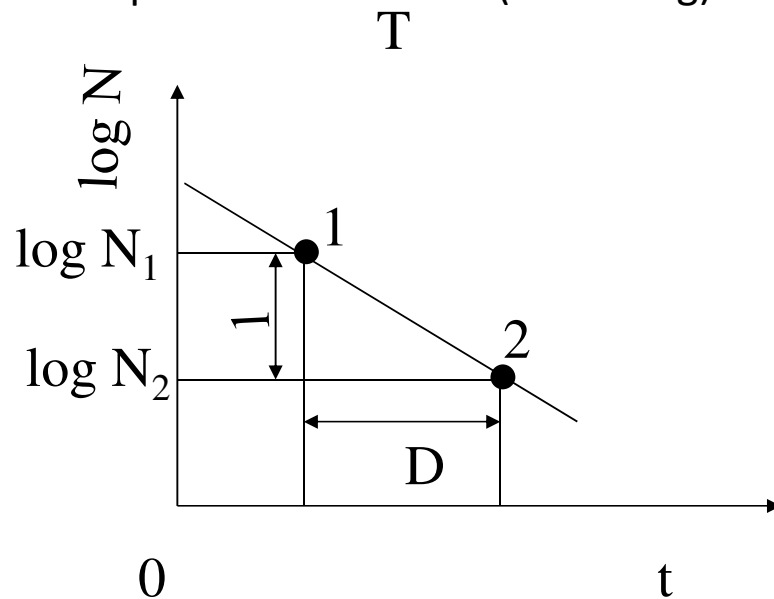


# Processo Térmico de Alimentos



## Tempo de Redução Decimal (D)

- ✓ Tempo necessário a uma dada temperatura para reduzir a população de microrganismos viáveis por um fator de 10 (1 ciclo log)



$$D = 2,303/k$$

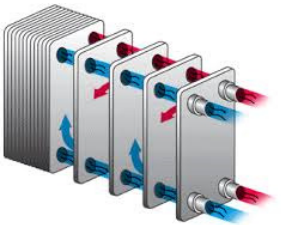
$$\log N_f = \log N_0 - (1/D) t$$

$$N_f = N_0 10^{- (t/D)}$$

$N_f$  = número de microrganismos sobreviventes

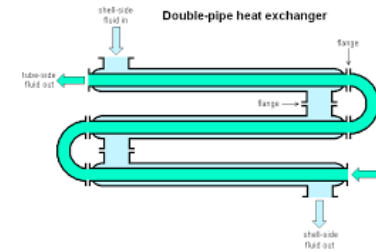
$N_f \geq 1$  haverá deterioração

$N_f < 1$  probabilidade de deterioração



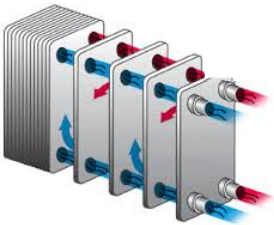
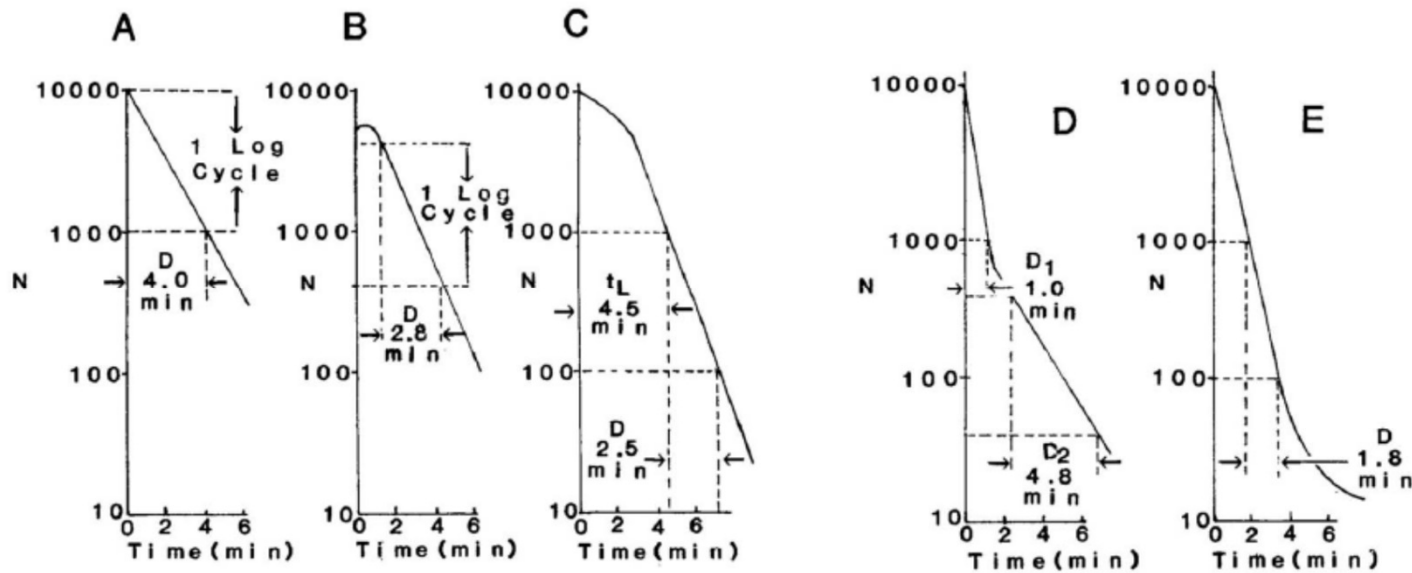


# Processo Térmico de Alimentos



## ➤ Curvas de Inativação Microbiana

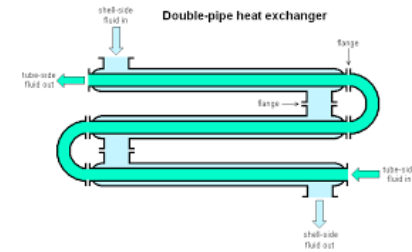
TOLEDO, R. T. Thermal Process Calculations In: TOLEDO, R. T. **Fundamentals of Food Process Engineering**. New York: Springer Science +Business Media, LLC, 2007. Cap. 9, p. 301-378.







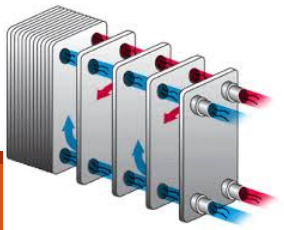
# Processo Térmico de Alimentos



## ➤ Valor de Esterilização ou Letalidade

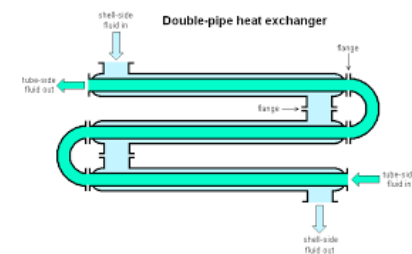
- ✓ Destruição de microrganismos num material aquecido
- S = número de reduções decimais

$$S = \log N - \log N_0 = \log (N/N_0) = t/D$$





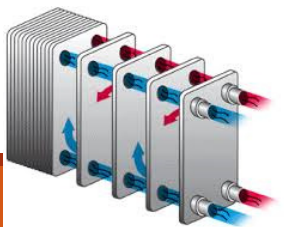
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## ➤ Valor de Esterilização ou Letalidade

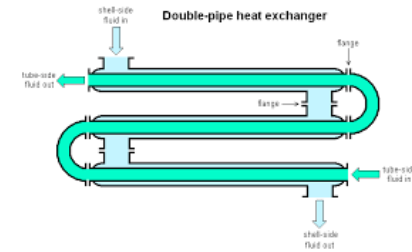
- ✓  $F_T$  (tempo) Tempo total de aquecimento a uma dada temperatura  $T$  para atingir uma determinada letalidade

$$F_T = SD_T \text{ processo isotérmico}$$





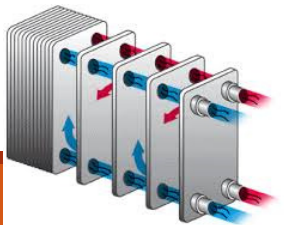
# Processo Térmico de Alimentos



✓ Para microrganismos patogênicos (Ex. *Clostridium botulinum*) o valor ideal para  $S = 12$

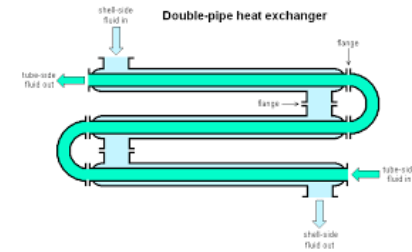
✓  $F$  é expresso numa temperatura de referência

- Esterilização  $T = 121,1\text{ °C} = 250\text{ °F}$   $F_0, D_0$
- Pasteurização  $T = 82,2\text{ °C} = 180\text{ °F}$   $F_{82,2}, D_{82,2}$





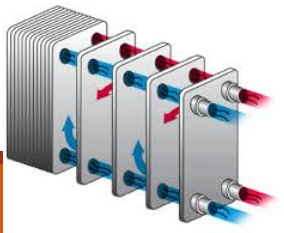
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## ➤ Valor de Esterilização ou Letalidade

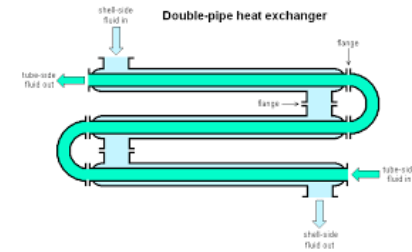
### ✓ Microrganismos patogênicos

- (pH > 4,5 baixa acidez *Clostridium botulinum*) 12 D





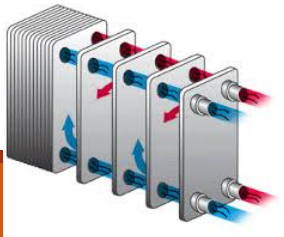
# Processo Térmico de Alimentos



## ➤ Valor de Esterilização ou Letalidade

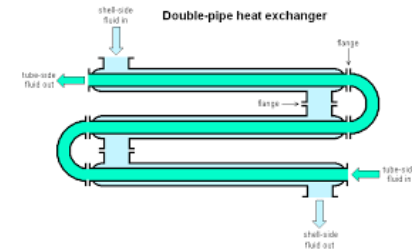
### ✓ Microrganismos deterioradores

- Bactérias esporuladas não patogênicas (*Clostridium sporogenes*, *Bacillus subtilis*) 5 D
- Bactérias termófilas não patogênicas (*Bacillus stearothermophilus*) 3 D





# Processo Térmico de Alimentos



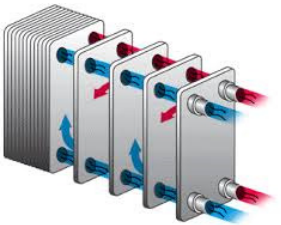
## ➤ Valor de Esterilização ou Letalidade

✓  $D_0$  *C. botulinum* = 0,21 min

$$12 * D = 12 * 0,21 = 2,52 \text{ min}$$

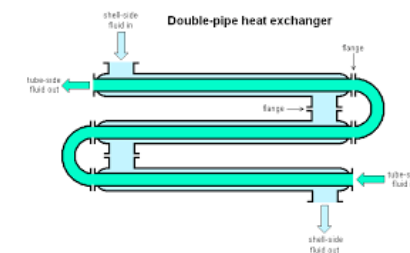
✓  $D_0$  *C. sporogenes* PA 3679 = 1 min

$$5 * D = 5 * 1 = 5 \text{ min}$$





# Processo Térmico de Alimentos

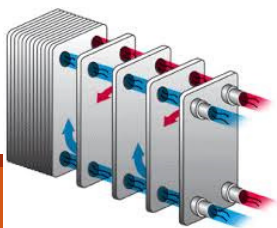


**Table 9.2** Heat Resistance of Spoilage Microorganisms in Low-Acid Canned Foods

Organism	Product	$D_0$ (min)	z	
			(°F)	(°C)
<i>Clostridium botulinum</i> 213-B	Phosphate buffer (pH7)	0.16	18	10
	Green beans	0.22	22	12
	Peas	0.22	14	8
<i>Clostridium botulinum</i> 62A	Phosphate buffer (pH7)	0.31	21	12
	Green beans	0.22	20	11
	Corn	0.3	18	10
	Spinach	0.25	19	11
	Phosphate buffer (pH7)	1.45	21	12
<i>Clostridium</i> spp. PA 3679	Asparagus	1.83	24	13
	Green beans	0.70	17	9
	Corn	1.20	18	10
	Peas	2.55	19	10
	Shrimp	1.68	21	12
	Spinach	2.33	23	13
	Phosphate buffer (pH7)	3.28	17	9
	Asparagus	4.20	20	11
<i>Bacillus stearothermophilus</i> FS 1518	Green beans	3.96	18	10
	Corn	4.32	21	12
	Peas	6.16	20	11
	Pumpkin	3.50	23	13
	Shrimp	3.90	16	9
	Spinach	4.94	21	12

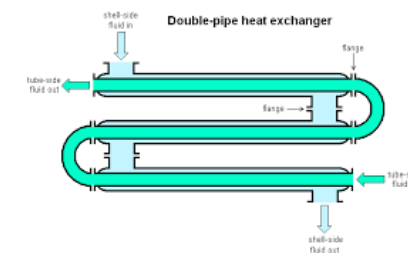
TOLEDO, R. T. Thermal Process Calculations In: TOLEDO, R. T. **Fundamentals of Food Process Engineering**. New York: Springer Science +Business Media, LLC, 2007. Cap. 9, p. 301-378.

Source: Reed, J. M., Bohrer, C. W. and Cameron, E. J., *Food Res.* 16:338-408.  
Reprinted from: Toledo R. T. 1980. *Fundamentals of Food Engineering*. AVI Pub. Co., Westport, CT.





# Processo Térmico de Alimentos



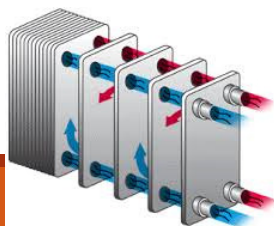
**Table 9.3** Heat Resistance of Spoilage Microorganisms in Acid and in Pasteurized Foods

Organism	Temperature		D (min)	Z	
	°F	°C		°F	°C
<i>Bacillus coagulans</i>	250	121.1	0.07	18	10
<i>Bacillus polymyza</i>	212	100	0.50	16	9
<i>Clostridium pasteurianum</i>	212	100	0.50	16	9
<i>Mycobacterium tuberculosis</i>	180	82.2	0.0003	10	6
<i>Salmonella spp.</i>	180	82.2	0.0032	12	7
<i>Staphylococcus spp.</i>	180	82.2	0.0063	12	7
<i>Lactobacillus spp.</i>	180	82.2	0.0095	12	7
Yeasts and molds	180	82.2	0.0095	12	7
<i>Clostridium botulinum</i> Type E	180	82.2	2.50	16	9

TOLEDO, R. T. Thermal Process Calculations In: TOLEDO, R. T. **Fundamentals of Food Process Engineering**. New York: Springer Science +Business Media, LLC, 2007. Cap. 9, p. 301-378.

Source: (1) Anderson, E. E., Esselen Jr., W. B. and Fellers, C. R. *Food Res.* 14:499-510, 1949. (2) Crissley, F. D., Peeler, J. T., Angelotti, R. and Hall, H. E., *J. Food Sci.* 33:133-137, 1968. (3) Stumbo, C. R. *Thermobacteriology in Food Processing*, Academic Press, New York, 1973. (4) Townsend, C. T. *Food Res.* 4:231-237, 1939. (5) Townsend, C. T., and Collier, C. P. *Proc. Technical Session of the 48th Annual Convention of the National Canners Association (NCA)*. NCA information Newsl. No. 1526, February 28, 1955. (6) Winter, A. R., Stewart, G. F., McFarlane, V. H. and Soloway, M. *Am. J. Pub. Health* 36:451-460, 1946. (7) Zuccharo, J. B., Powers, J. J., Morse, R. E. and Mills W. C. *Food. Res.* 16:3038, 1951

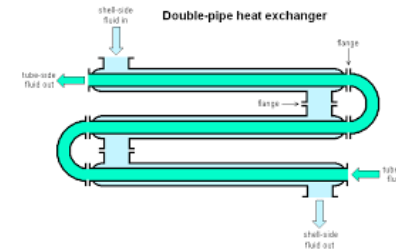
Reprinted from: Toledo, 1980. *Fundamentals of Food Process Engineering*, 1st. ed. AVI Pub. Co. Westport, Conn.



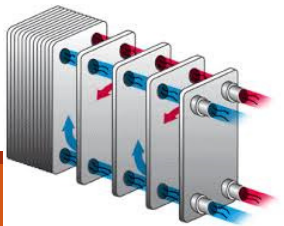
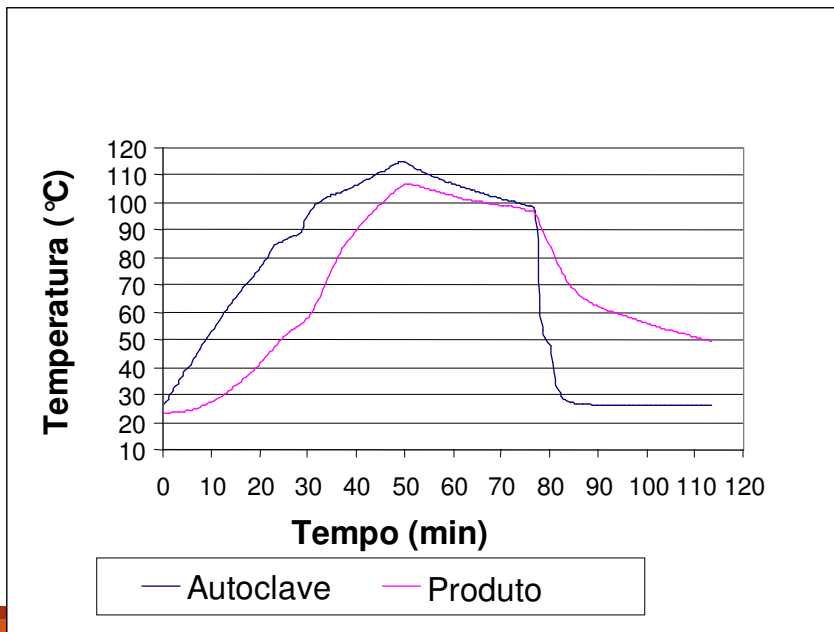




# Processo Térmico de Alimentos

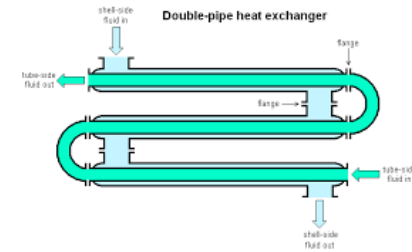


- Processos reais não ocorrem a temperatura constante
- ✓ Descrever a dependência da taxa de inativação com a temperatura

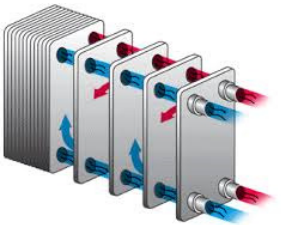




# Processo Térmico de Alimentos

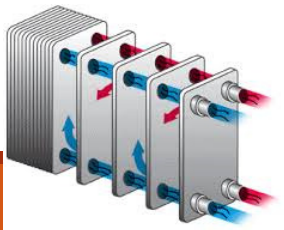
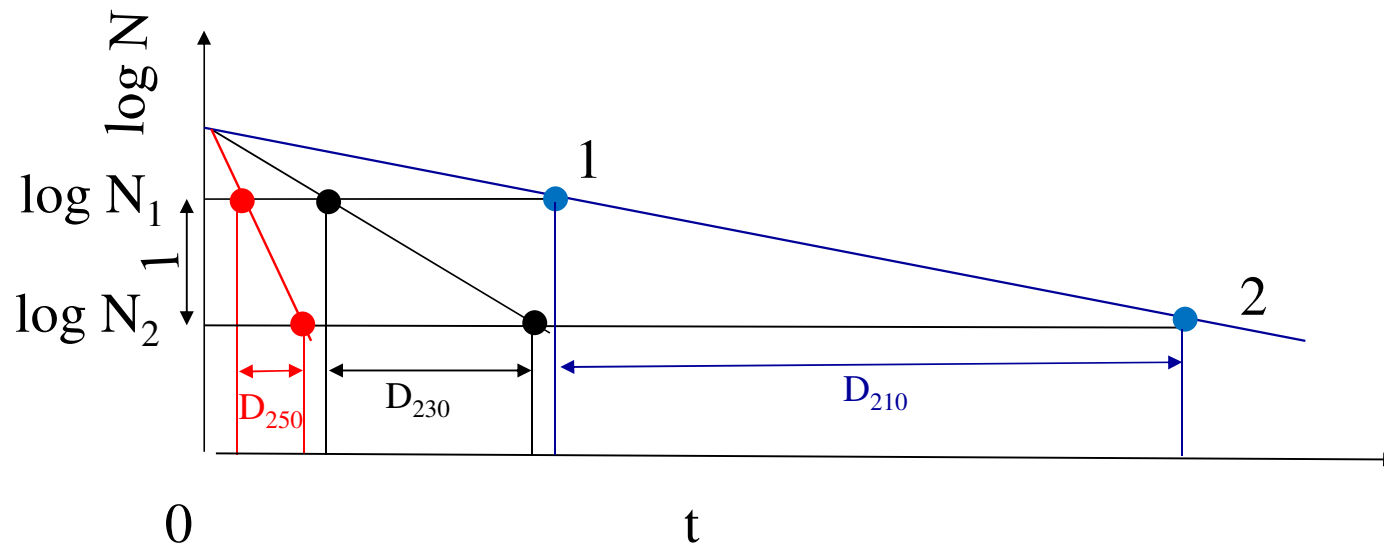
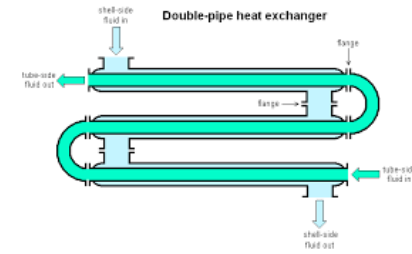


- Curvas de Tempo de Morte Térmica “TDT”
  - ✓ Curvas de inativação microbiana em diferentes temperaturas
  - ✓ Determinação dos valores de  $D$  em cada temperatura



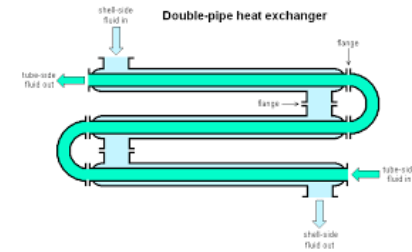


# Processo Térmico de Alimentos



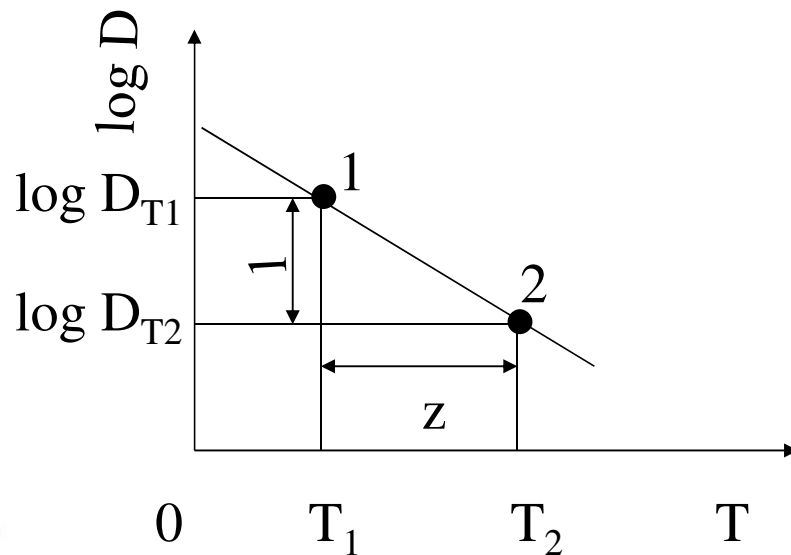


# Processo Térmico de Alimentos



## ➤ Valor z

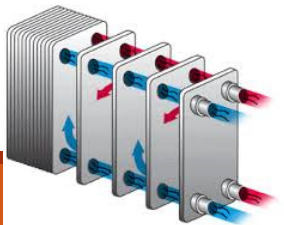
- ✓ Diferença de temperatura necessária para reduzir o valor do tempo de redução decimal (D) por um fator de dez (1 ciclo log)



$$\log D_{T2} = \log D_{T1} - (1/z) (T_2 - T_1)$$

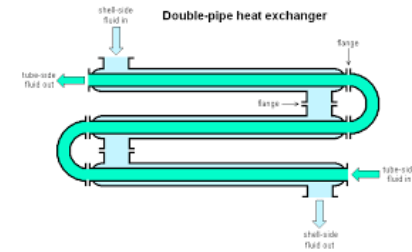
$$D_{T2} = D_{T1} 10^{-(T_2 - T_1)/z}$$

$$D_T = D_0 10^{-(T - T_0)/z}$$

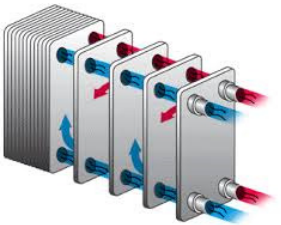




# Processo Térmico Descontínuo

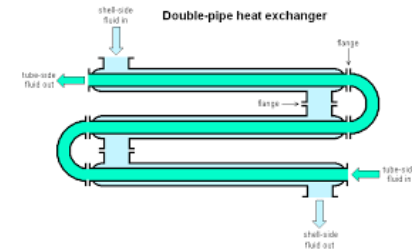


- Alimento contido numa embalagem (lata, vidro, bolsa flexível)
- Processo de aquecimento e resfriamento em autoclave batelada ou contínua





# Processo Térmico Descontínuo

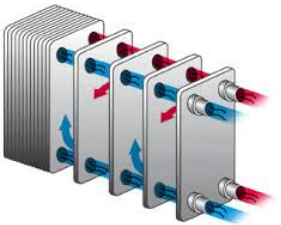


➤ Determinar a letalidade do processo para verificar se foi atingido o grau desejado de esterilização

✓  $F_T = SD_T$

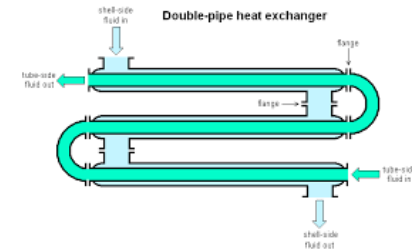
✓ Métodos para determinar a letalidade

- Método geral – integração da curva temperatura/tempo
- Método das fórmulas – previsão da temperatura do produto (Stumbo e Hayakawa)





# Processo Térmico Descontínuo



$$F_T = SD_T \quad (1)$$

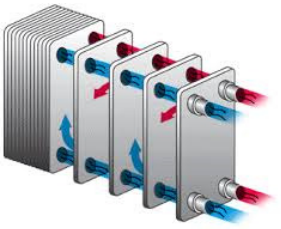
Fator de Letalidade ou Taxa Letal (L):

$$F_0 = SD_0 \quad (2)$$

$$L = 10^{\frac{(T-T_0)}{z}}$$

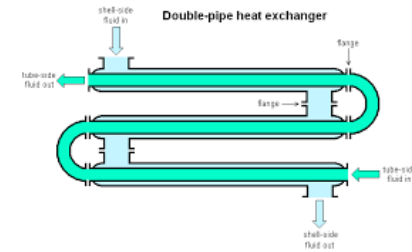
Dividindo (1) por (2):

$$\frac{F_T}{F_0} = \frac{SD_T}{SD_0} = \frac{D_T}{D_0} = 10^{-\frac{(T-T_0)}{z}} \quad (3)$$

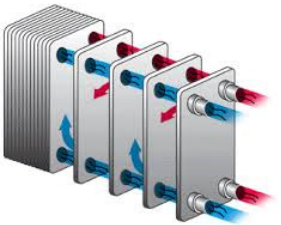




# Processo Térmico Descontínuo



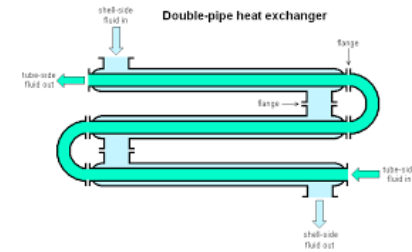
- Determinar o microrganismo a ser utilizado como referência
- Calcular o valor de letalidade desejado ( $F_0$ )
- Teste de penetração de calor obtendo a história da temperatura do produto no ponto frio





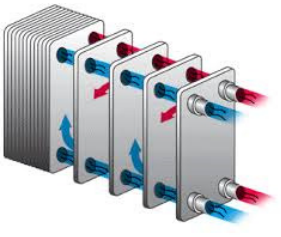


# Processo Térmico Descontínuo



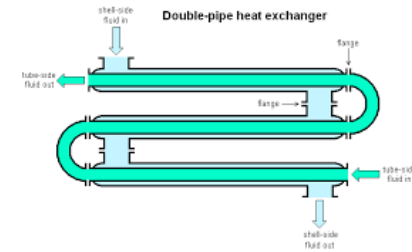
- Obter o valor de  $F_0$  resultante do processo térmico realizado
- Comparar os valores e determinar os parâmetros para que se obtenha a letalidade desejada

$$F_0^Z = \int_0^t L_t dt$$



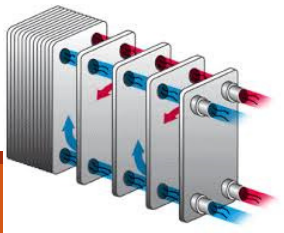


# Processo Térmico Descontínuo



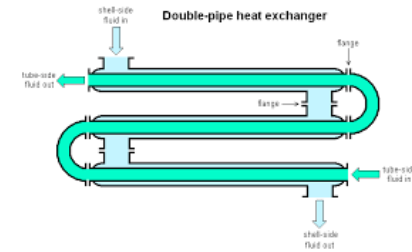
## ➤ Método Geral

- ✓ Regra de Simpson
- ✓ Estabelecer um  $\delta t$  tal que  $t/\delta t$  seja um número par
- ✓  $i = 0, t = 0; i = 1, t = \delta t, i = 2, t = 2 \delta t$
- ✓  $A = \delta t/3 [L_0 + 4L_1 + 2L_2 + 4L_3 + 2L_4 + \dots + 2L_{i-2} + 4L_{i-1} + L_t] = F_0$





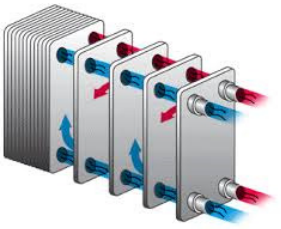
# Processo Térmico Descontínuo



## ➤ Curvas de Penetração de Calor

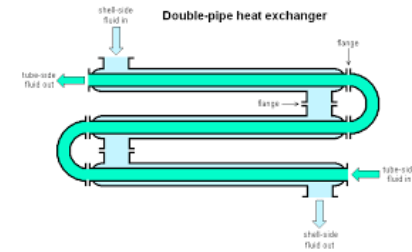
- ✓ Predição da temperatura no ponto frio do produto
- ✓ Cilindro finito

$$\frac{T - T_{\infty}}{T_0 - T_{\infty}} = \exp \left[ \left( \frac{-hA}{\rho C_p V} \right) t \right]$$





# Temperatura no Aquecimento



$$\frac{T - T_{\infty}}{T_0 - T_{\infty}} = \exp \left[ \left( \frac{-hA}{\rho C_p V} \right) t \right]$$

$$\frac{(T_{\infty} - T)}{j_h I_h} = \frac{g}{j_h I_h} = 10^{\frac{-t}{f_h}}$$

$$(T_{\infty} - T) = j_h I_h 10^{\frac{-t}{f_h}}$$

$$T = T_{\infty} - j_h I_h 10^{\frac{-t}{f_h}}$$

$T_{\infty}$  = Temperatura da Autoclave

$T_0$  = Temperatura inicial

$I_h$  = Diferença Inicial de Temperatura =  $T_{\infty} - T_0$

$g$  = Diferença de temperatura entre a autoclave e o ponto frio do produto =  $T_{\infty} - T$

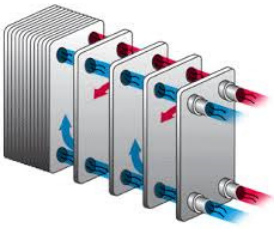
$f_h$  = Tempo necessário para que a diferença de temperatura entre a autoclave e o ponto frio do produto diminua em 1 ciclo logarítmico

$t_{CUT}$  = Tempo de aquecimento da autoclave ("come up time")

$t_{pi}$  = Tempo pseudo inicial =  $0,6 * t_{CUT}$

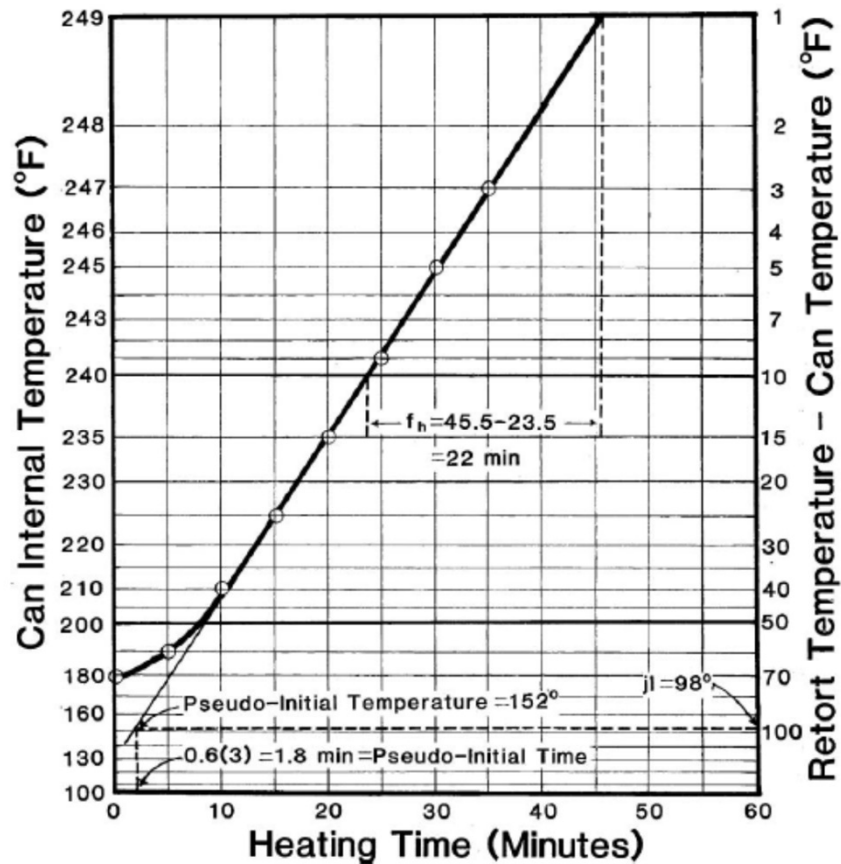
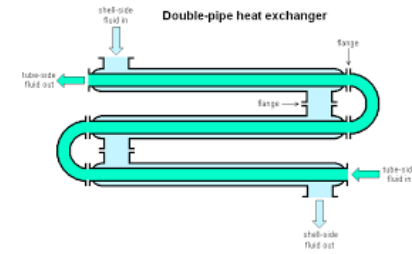
$T_{pi}$  = Temperatura na intersecção do prolongamento da reta com  $t_{pi}$

$$j_h = \text{Fator "lag"} = \frac{T_{\infty} - T_{pi}}{T_{\infty} - T_0}$$





# Temperatura no Aquecimento

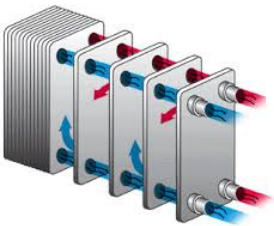


Temperatura da autoclave ( $T_{\infty}$ ) = 250 °F

Tempo de aquecimento ( $t_{CUT}$ ) = 3 min

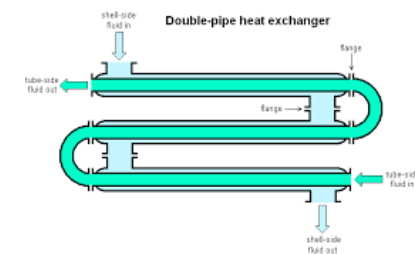
Temperatura do meio resfriador = 60 °F

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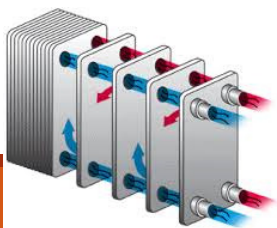
# Processo Térmico Descontínuo



Dados de temperatura ao longo do processamento na autoclave

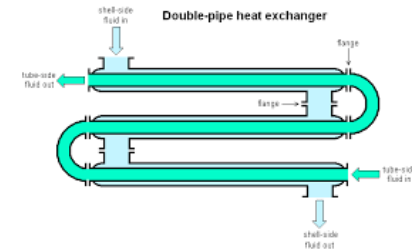
<i>Time (min)</i>	<i>Temp. (°F)</i>	<i>Time (min)</i>	<i>Temp. (°F)</i>
0	180	30	245
5	190	30 (cool)	245
10	210	35	235
15	225	40	175
20	235	45	130
25	241	50	101

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# Temperatura no Resfriamento



$$\frac{(T_g - T_c)}{j_c I_c} = 10^{\frac{-t_c}{f_c}}$$

$$(T_g - T_c) = j_c I_c 10^{\frac{-t_c}{f_c}}$$

$$T_g = T_c + j_c I_c 10^{\frac{-t_c}{f_c}}$$

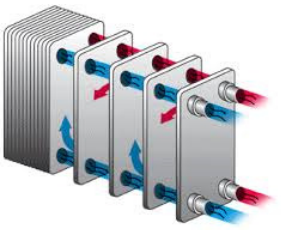
$T_c$  = Temperatura da água de resfriamento

$T_g$  = Temperatura do ponto frio no final do aquecimento

$I_c$  = Diferença de Temperatura no início do resfriamento =  $T_g - T_c$

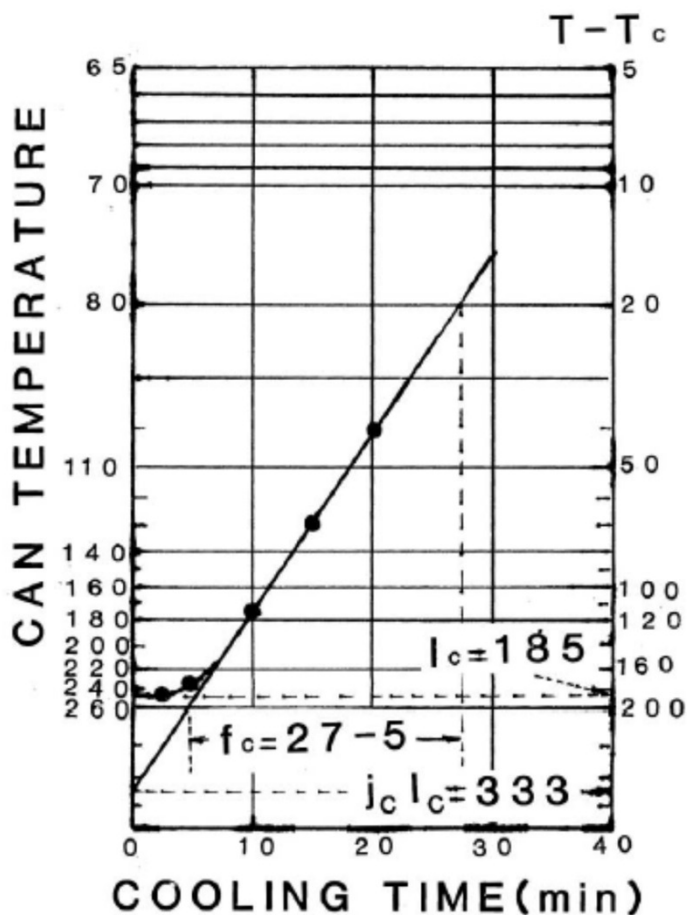
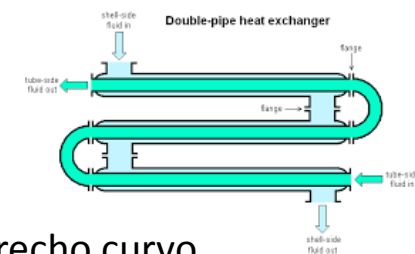
$f_c$  = Tempo necessário para que a diferença de temperatura entre a água de resfriamento e o ponto frio do produto diminua em 1 ciclo logarítmico

$j_c$  = Fator "lag", sendo  $j_c I_c$  = a intersecção entre o prolongamento da reta com o tempo inicial do resfriamento ( $t_c = 0$ )





# Processo Térmico Descontínuo



Hayakawa – função trigonométrica trecho curvo

$$T = T_c + [T_g - T_c]^{\cos(Bt_c)}$$

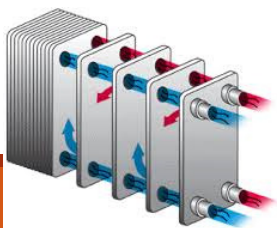
$$B = \frac{1}{t_L} \left[ \arccos \left[ \frac{\log(j_c l_c) - \frac{t_L}{f_c}}{\log l_c} \right] \right]$$

Ângulo em radianos

$t_L$  = tempo para intersecção do trecho curvo com o trecho reto

$$t_L = f_c \log \left( \frac{j_c}{k} \right) \quad \text{Valor típico } k = 0,95$$

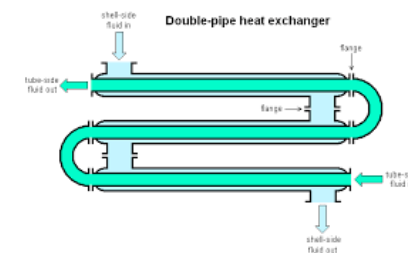
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# Processo Térmico Descontínuo



Time ( $t_c$ )	$E$	$A$	(Temp °F)	
			$70 + 174.3^E$	$70 + (313.74)^A$
0	1	1	244.3	(383.7)
2	0.998	0.811	243.3	(324.5)
4	0.993	0.658	240.4	(276.4)
6	0.984	0.534	235.7	(237.3)
8		0.433		199.4
10		0.351		180.2
12		0.285		159.4
14		0.231		142.5
16		0.187		128.8

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