

ESCOAMENTO SOBRE UMA PLACA PLANA: CAMADA LIMITE

Paulo Seleghim Jr.
Universidade de São Paulo



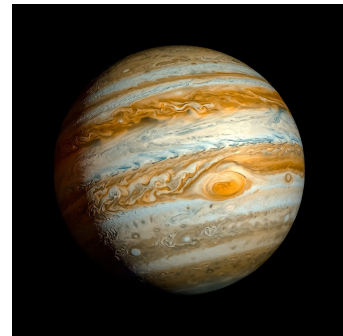
Equações governantes:

Continuidade (massa) $\rightarrow \frac{\partial \rho}{\partial t} + \vec{\nabla} \cdot (\rho \vec{U}) = 0$

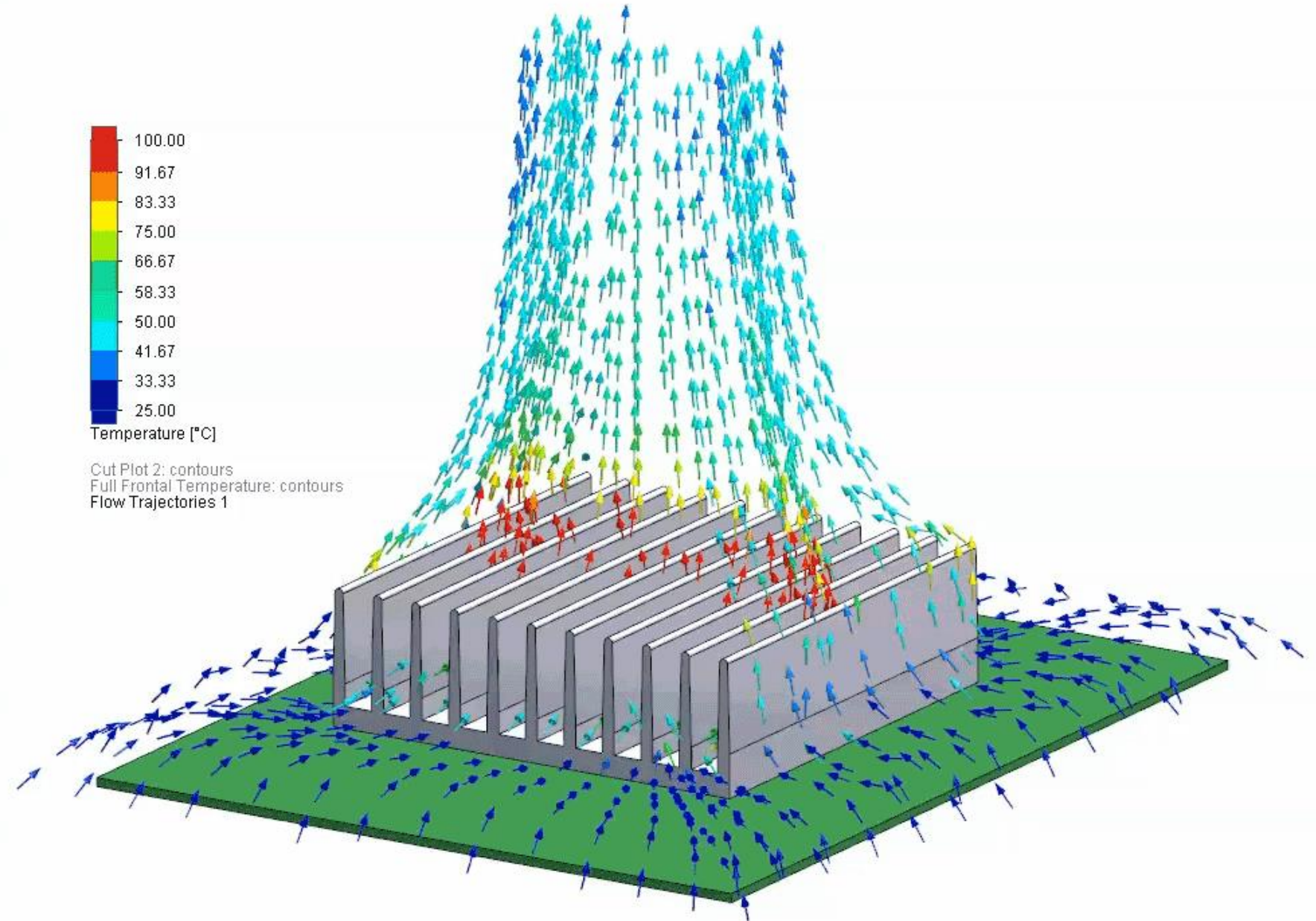
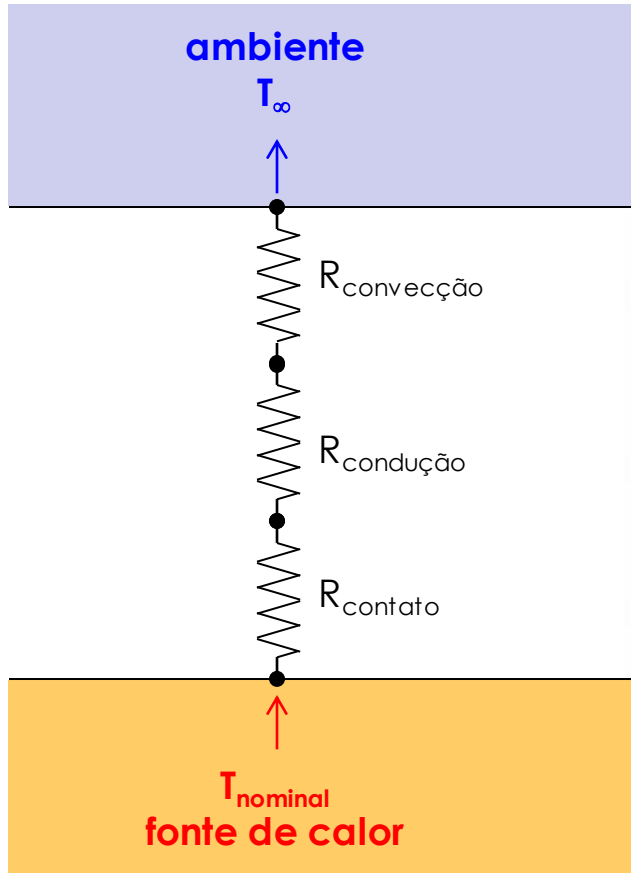
Q. de movimento (Navier-Stokes) $\rightarrow \rho \cdot \left(\frac{\partial \vec{U}}{\partial t} + \vec{U} \cdot \vec{\nabla} \vec{U} \right) = -\vec{\nabla} P + \vec{\nabla} \cdot \tilde{\mathbf{T}} + \sum \vec{F}_{3D}$

Energia (1ª lei) $\rightarrow \rho C_p \left(\frac{\partial T}{\partial t} + \vec{U} \cdot \vec{\nabla} T \right) = \vec{\nabla} \cdot (k \vec{\nabla} T) + \tilde{\mathbf{T}} : \tilde{\mathbf{D}}$

Escalas microscópicas
(Kolmogorov) a escalas
sinóticas...



Resfriamento de componentes eletrônicos...



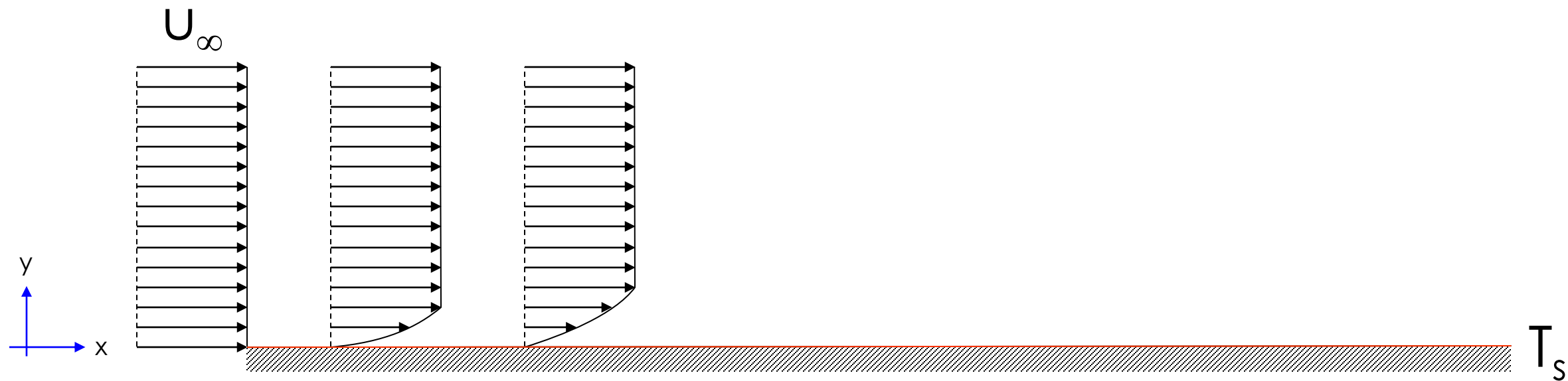
Escoamento incidindo sobre uma placa plana...



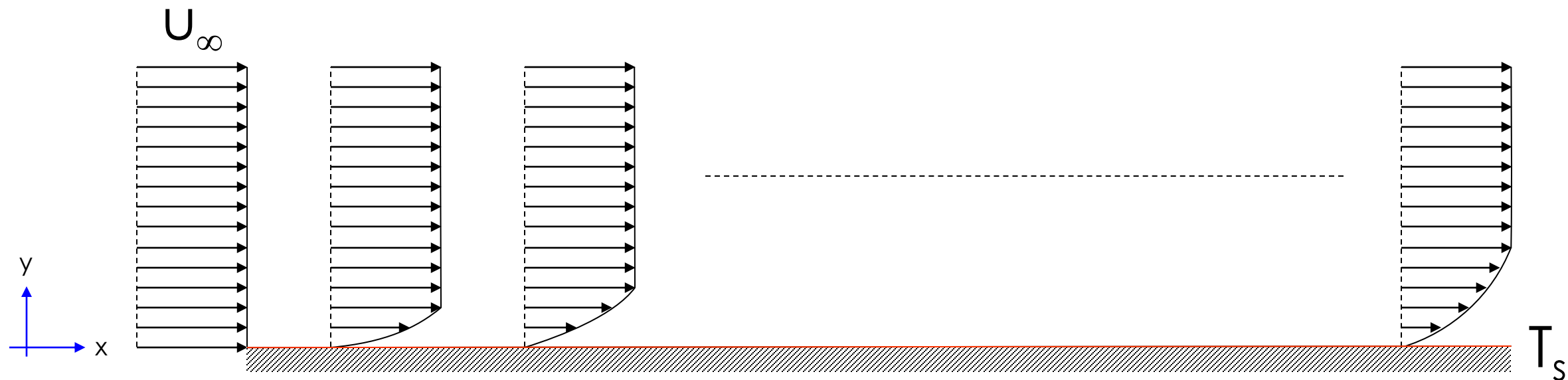
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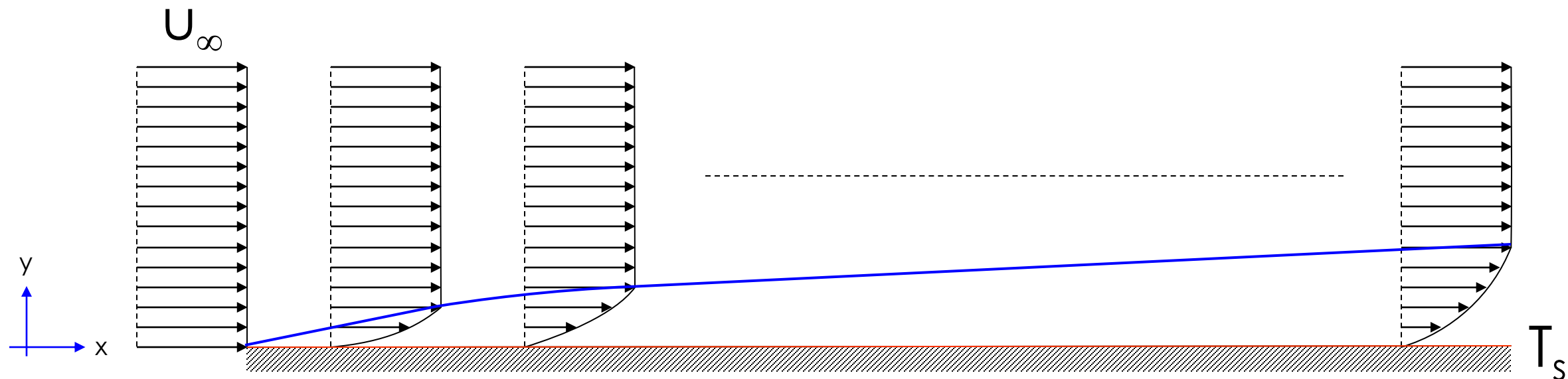
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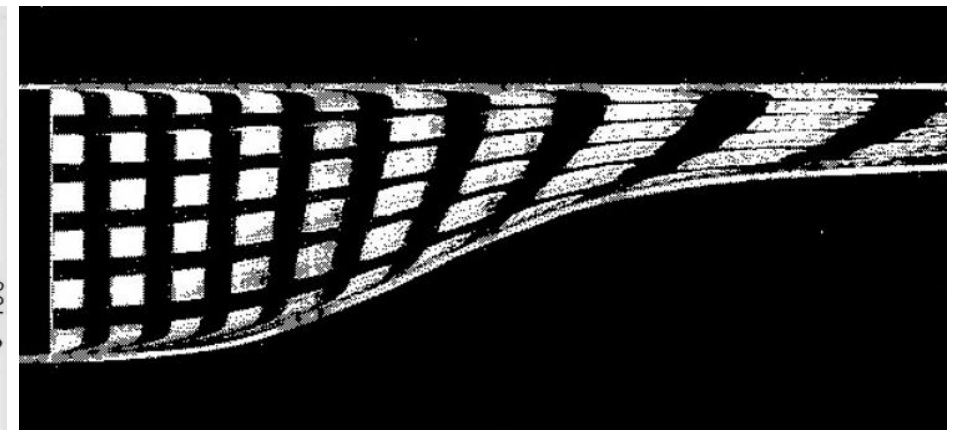
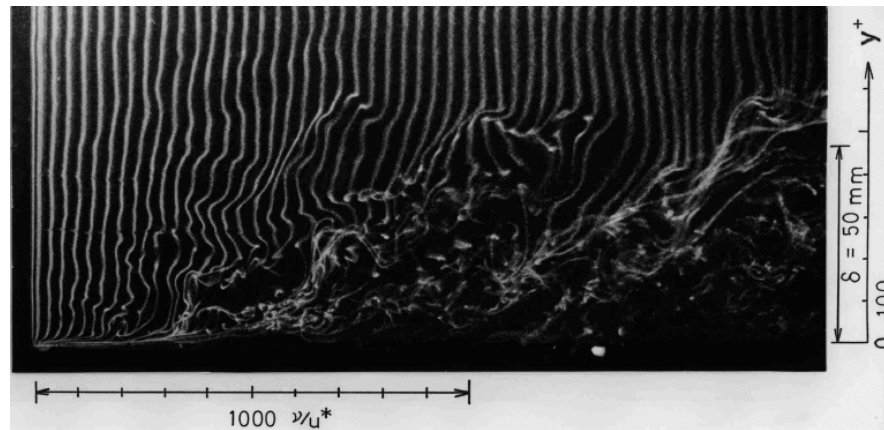
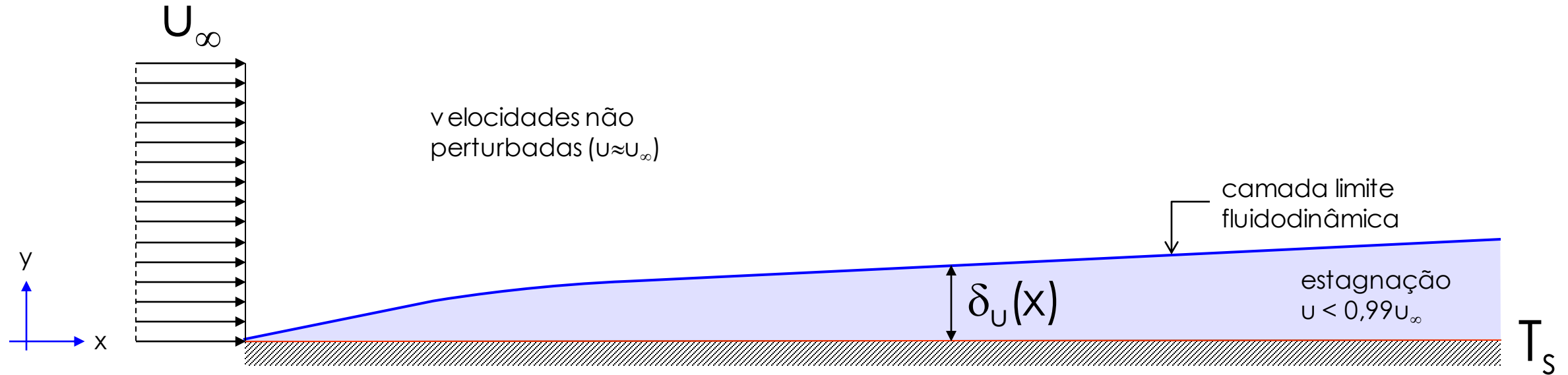
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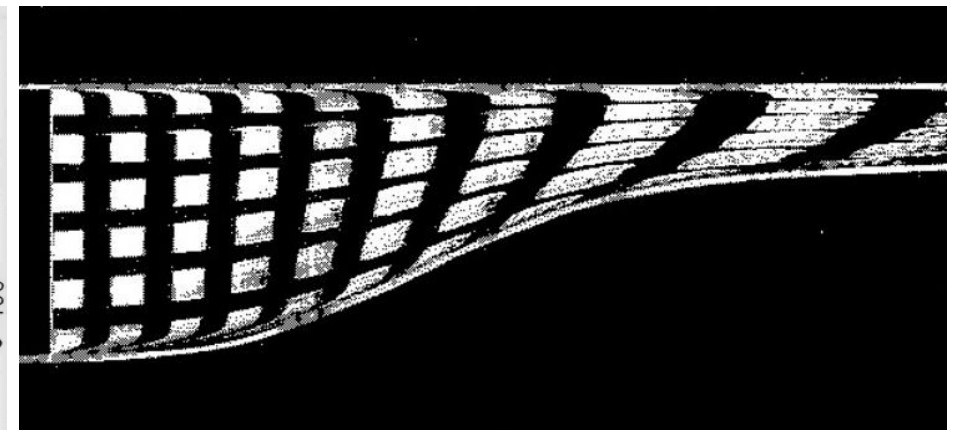
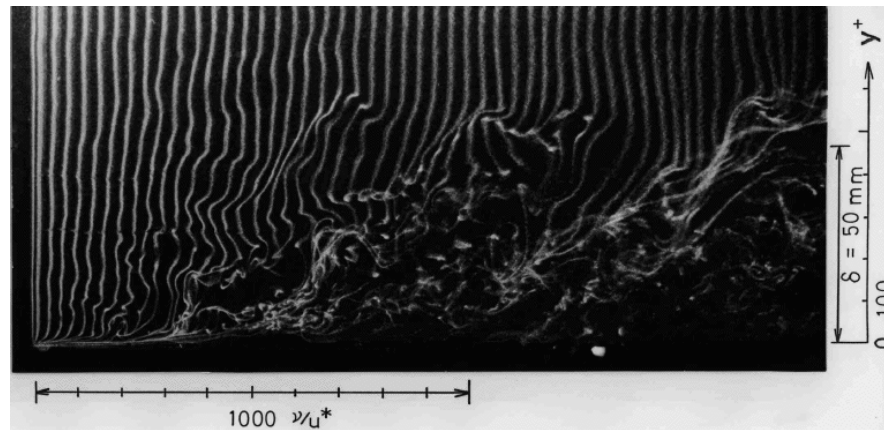
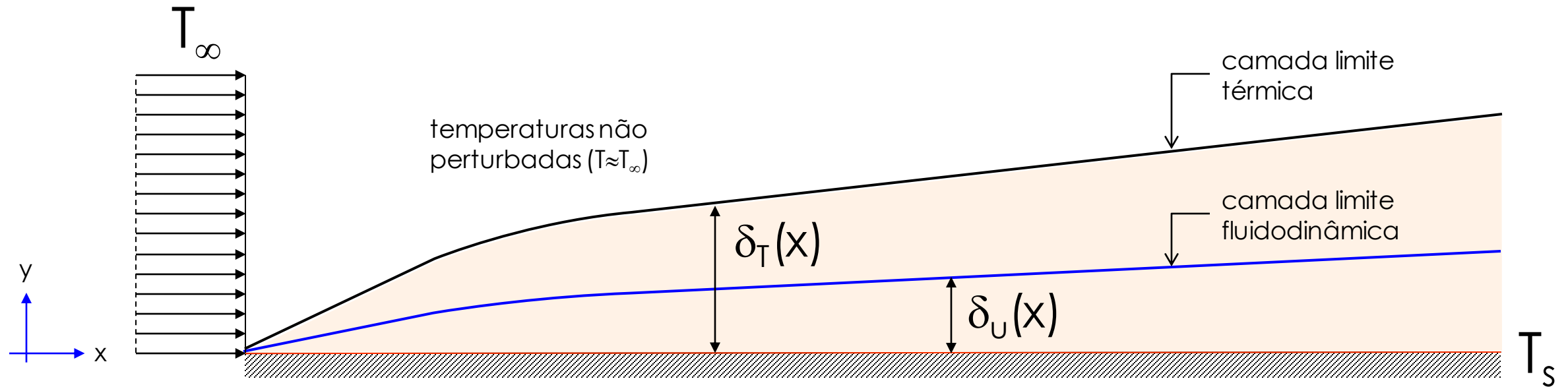


Escoamento incidindo sobre uma placa plana...



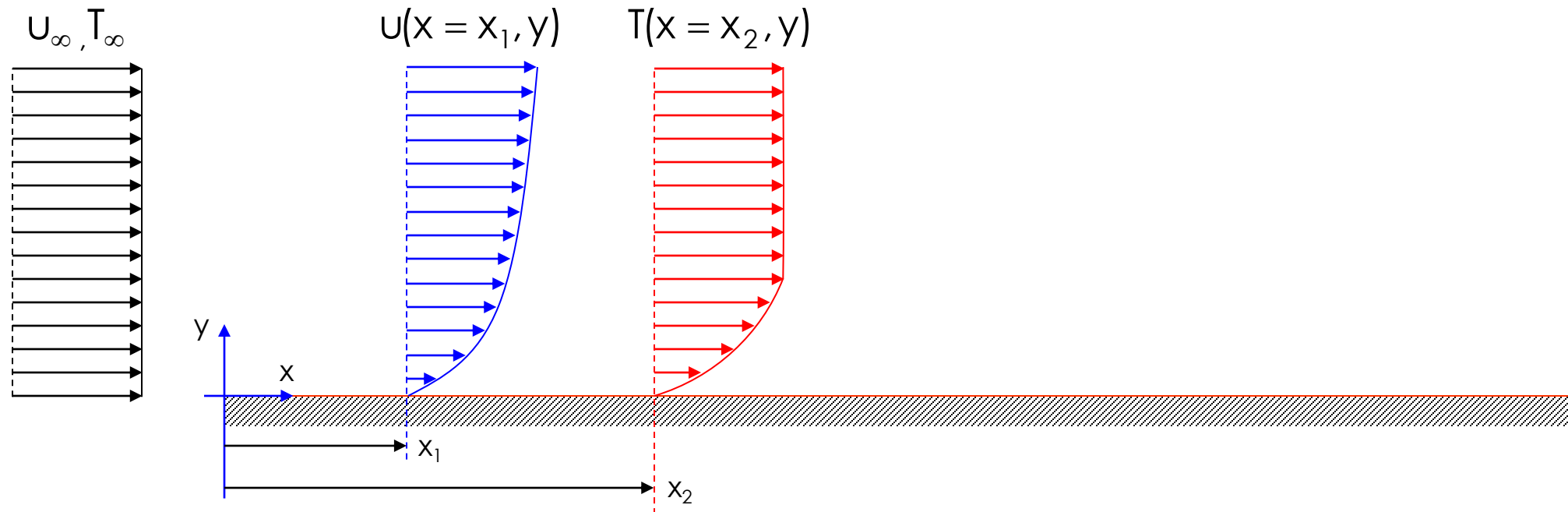
Y. IRITANI, N. KASAGI and M. HIRATA

Escoamento incidindo sobre uma placa plana...

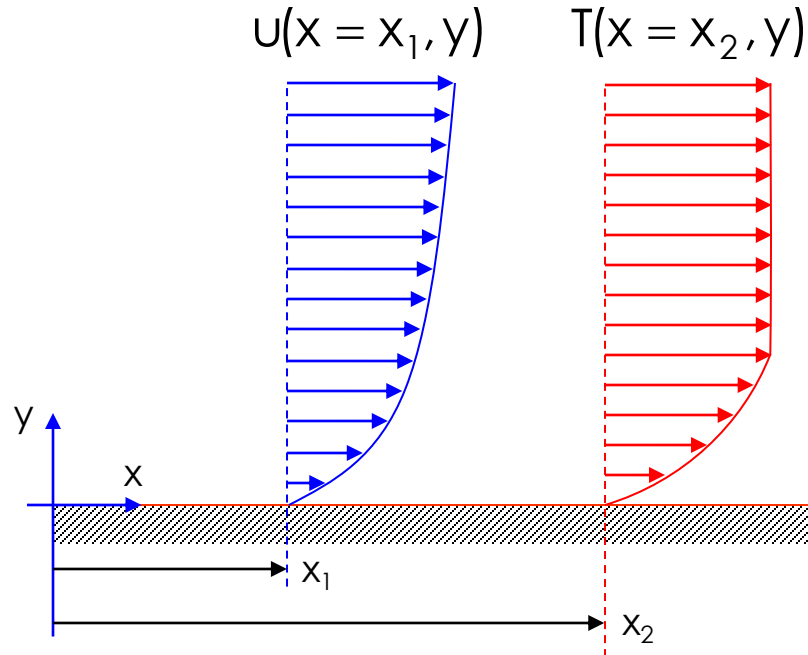
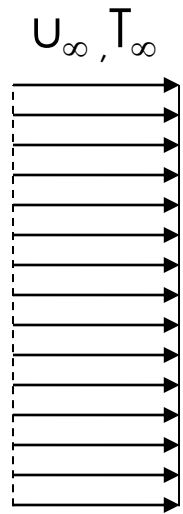


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Cálculo das camadas limites hidrodinâmica e térmica...



Cálculo das camadas limites hidrodinâmica e térmica...



$$U \frac{\partial U}{\partial x} + v \frac{\partial U}{\partial y} = 0$$

← massa

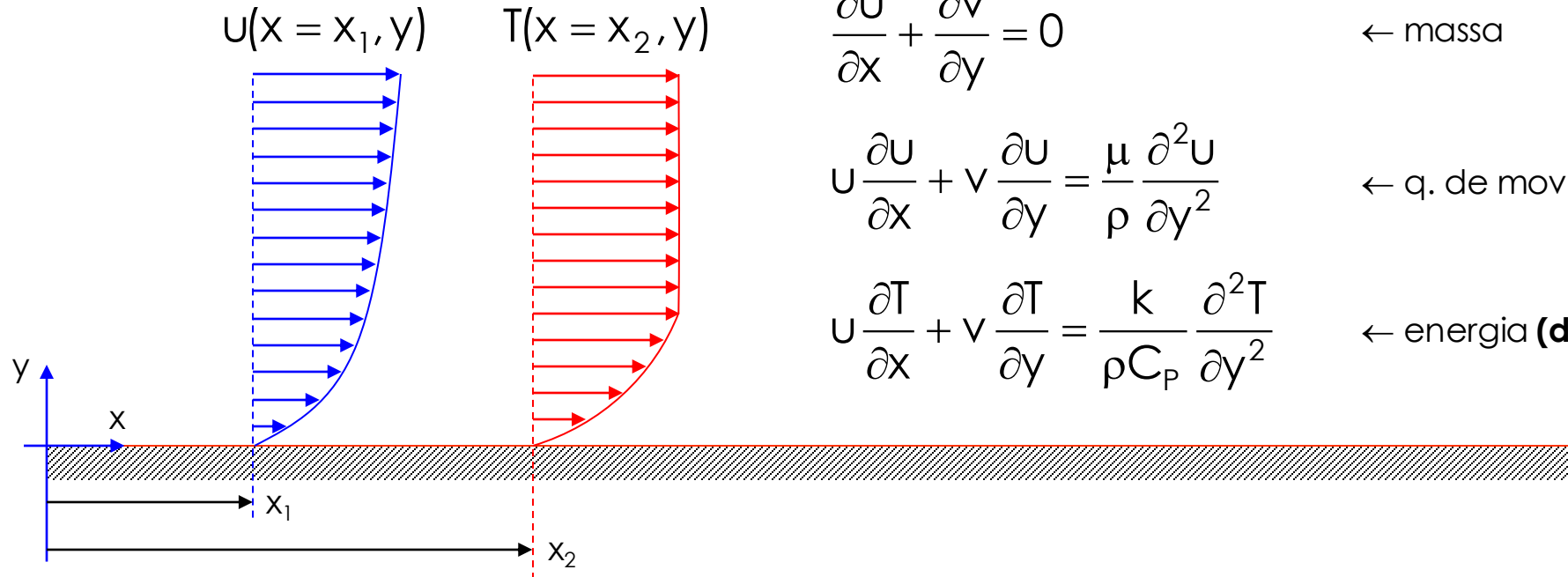
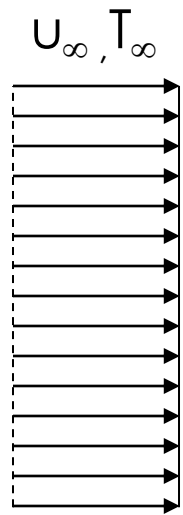
$$U \frac{\partial U}{\partial x} + v \frac{\partial U}{\partial y} = \frac{\mu}{\rho} \frac{\partial^2 U}{\partial y^2}$$

← q. de movimento

$$U \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \frac{k}{\rho C_p} \frac{\partial^2 T}{\partial y^2}$$

← energia

Cálculo das camadas limites hidrodinâmica e térmica...



$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

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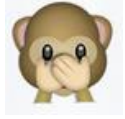
← energia **(desacoplada)**

$$p / x = 0 \rightarrow u(0, y) = u_\infty \text{ e } T(0, y) = T_\infty$$

$$p / y = 0 \rightarrow u(x, 0) = 0, v(x, 0) = 0 \text{ e } T(x, 0) = T_s$$

$$p / y \rightarrow \infty \rightarrow u(x, \infty) = u_\infty \text{ e } T(x, \infty) = T_\infty$$

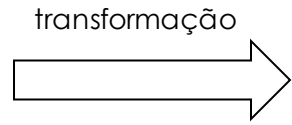
Solução de Blasius (1908)... **velocidades**



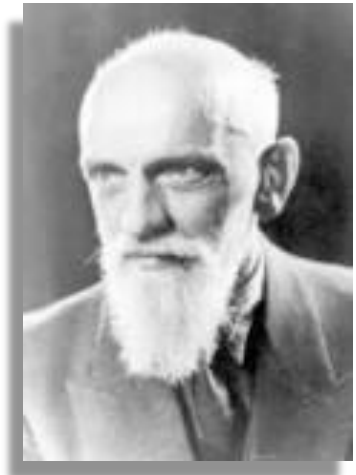
$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$



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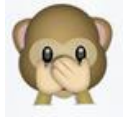


$$a_0 \cdot f(\eta) + a_1 \frac{f(\eta)}{d\eta} + a_2 \frac{f^2(\eta)}{d\eta^2} + a_3 \frac{f^3(\eta)}{d\eta^3} + \dots$$



Paul R.H. Blasius
(1883–1970)

Solução de Blasius (1908)... velocidades

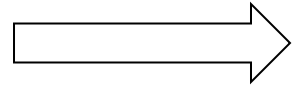


$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

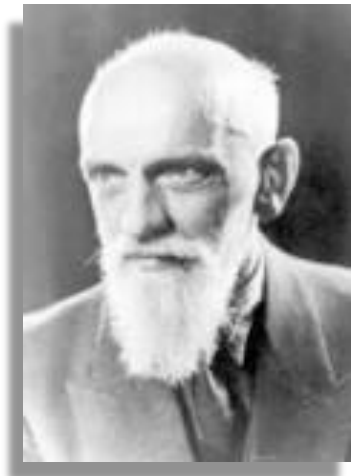


$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \frac{\mu}{\rho} \frac{\partial^2 u}{\partial y^2}$$

transformação



$$a_0 \cdot f(\eta) + a_1 \frac{f(\eta)}{d\eta} + a_2 \frac{f^2(\eta)}{d\eta^2} + a_3 \frac{f^3(\eta)}{d\eta^3} + \dots$$



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variável de similaridade



$$\eta \stackrel{\text{def}}{=} y \cdot \sqrt{\frac{U_\infty}{x \cdot \mu / \rho}}$$

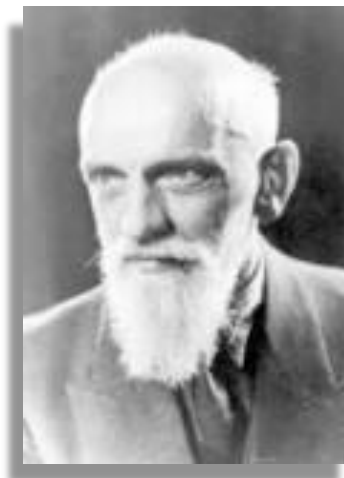
$$f(\eta) \stackrel{\text{def}}{=} \frac{\psi}{U_\infty \cdot \sqrt{\frac{x \cdot \mu / \rho}{U_\infty}}}$$

← ψ = função de corrente

Solução de Blasius (1908)... **velocidades**

$$\psi(x, y) \stackrel{\text{def}}{=} \begin{cases} U = + \frac{\partial \psi}{\partial y} \\ V = - \frac{\partial \psi}{\partial x} \end{cases} \Rightarrow \text{🙈} \equiv 0$$

função de corrente

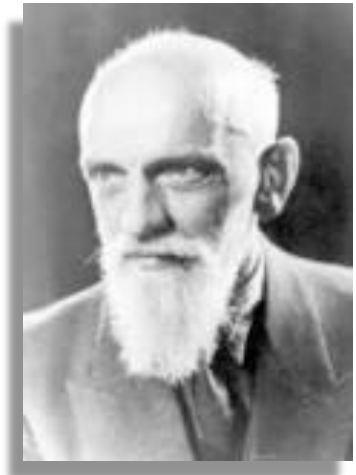


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função de corrente



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(1883–1970)

As componentes da velocidade se escrevem então como:

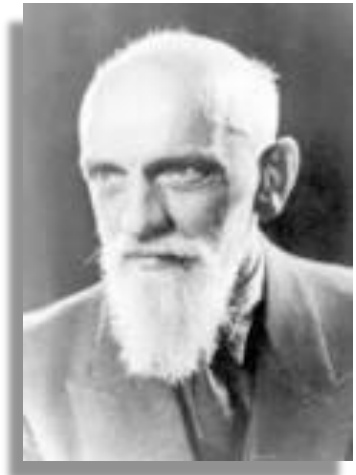
$$\eta = y \cdot \sqrt{\frac{U_\infty}{x \cdot \rho / \mu}}$$

$$\psi = U_\infty \sqrt{x \cdot \frac{\mu / \rho}{U_\infty}} \cdot f(\eta)$$

$$U = + \frac{\partial \psi}{\partial y} = + \left(\frac{\partial \psi}{\partial \eta} \right) \cdot \left(\frac{\partial \eta}{\partial y} \right) = \left(U_\infty \sqrt{\frac{xv}{U_\infty}} \cdot \frac{df}{d\eta} \right) \cdot \left(\sqrt{\frac{U_\infty}{xv}} \right) = U_\infty \frac{df}{d\eta}$$

$$v = \mu / \rho$$

Solução de Blasius (1908)... **velocidades**



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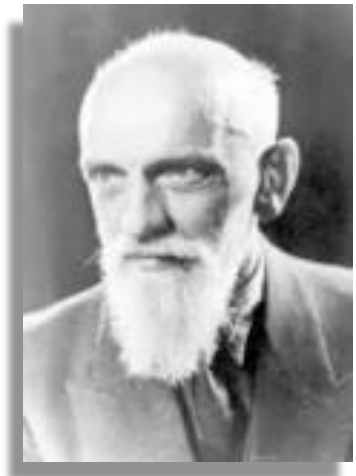
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$$v = - \frac{\partial \psi}{\partial x} = - U_\infty \sqrt{\frac{v}{U_\infty}} \cdot f(\eta) \cdot \left(\frac{x^{-1/2}}{2} \right) - \left(U_\infty \sqrt{x \cdot \frac{v}{U_\infty}} \cdot \frac{\partial f}{\partial x} \right) = \frac{1}{2} \sqrt{\frac{U_\infty v}{x}} \cdot \left(\eta \frac{df}{d\eta} - f \right)$$

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Solução de Blasius (1908)... **velocidades**



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função de corrente

As componentes da velocidade se escrevem então como:

$$\eta = y \cdot \sqrt{\frac{U_\infty}{x \cdot \rho / \mu}}$$

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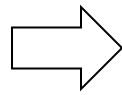
$$\begin{matrix} U = \dots \\ v = \dots \end{matrix} \Rightarrow \text{🙈} \quad U \frac{\partial U}{\partial x} + v \frac{\partial U}{\partial y} = \frac{\mu}{\rho} \frac{\partial^2 U}{\partial y^2}$$

Solução de Blasius (1908)... **velocidades**

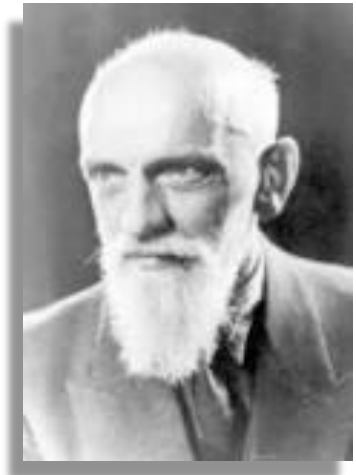
$$\frac{\partial u}{\partial x} = -\frac{u_{\infty}}{2x} \eta \frac{d^2 f}{d\eta^2}$$

$$\frac{\partial u}{\partial y} = u_{\infty} \sqrt{\frac{u_{\infty}}{\nu x}} \frac{d^2 f}{d\eta^2}$$

$$\frac{\partial^2 u}{\partial y^2} = \frac{u_{\infty}^2}{\nu x} \frac{d^3 f}{d\eta^3}$$



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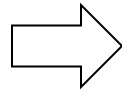
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Solução de Blasius (1908)... **velocidades**

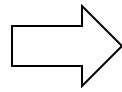
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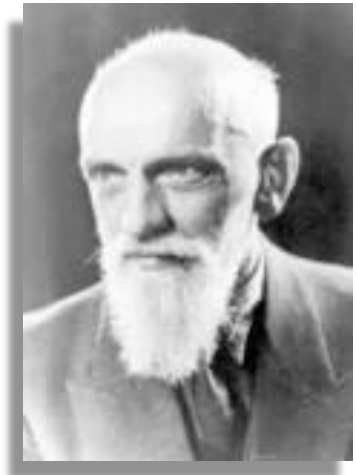
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$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \frac{\mu}{\rho} \frac{\partial^2 u}{\partial y^2}$$



$$2 \frac{d^3 f}{d\eta^3} + f \frac{d^2 f}{d\eta^2} = 0$$



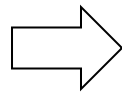
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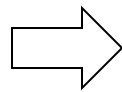
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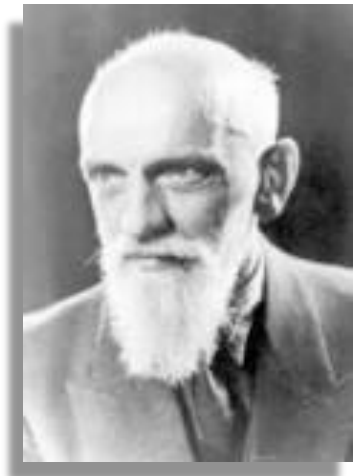
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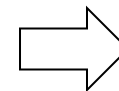


Paul R.H. Blasius
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$$p/x = 0 \rightarrow u(0, y) = u_\infty$$

$$p/y = 0 \rightarrow u(x, 0) = 0, v(x, 0) = 0$$

$$p/y \rightarrow \infty \rightarrow u(x, \infty) = u_\infty$$



$$p/\eta = 0 \rightarrow f(\eta) = 0$$

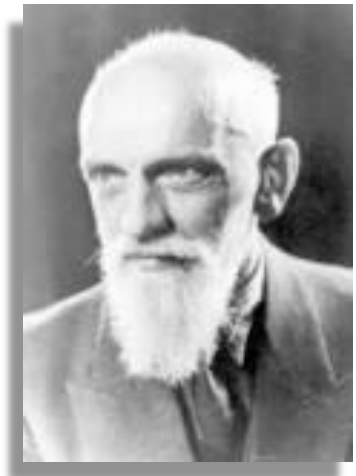
$$p/\eta = 0 \rightarrow df/d\eta = 0$$

$$p/\eta = \infty \rightarrow df/d\eta = 1$$

Solução de Blasius (1908)... **c. limite fluidodinâmica**

$$2 \frac{d^3 f}{d\eta^3} + f \frac{d^2 f}{d\eta^2} = 0$$

η	f	$\frac{df}{d\eta} = \frac{u}{u_\infty}$	$\frac{d^2 f}{d\eta^2}$
0	0	0	0.332
0.5	0.042	0.166	0.331
1.0	0.166	0.330	0.323
1.5	0.370	0.487	0.303
2.0	0.650	0.630	0.267
2.5	0.996	0.751	0.217
3.0	1.397	0.846	0.161
3.5	1.838	0.913	0.108
4.0	2.306	0.956	0.064
4.5	2.790	0.980	0.034
5.0	3.283	0.992	0.016
5.5	3.781	0.997	0.007
6.0	4.280	0.999	0.002
∞	∞	1	0



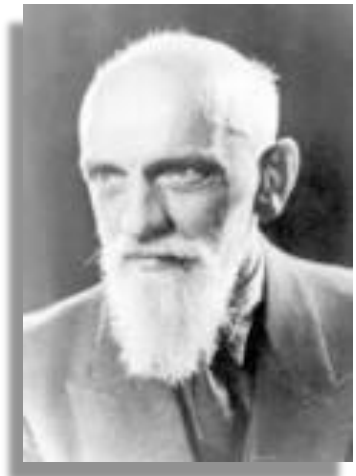
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$$2 \frac{d^3 f}{d\eta^3} + f \frac{d^2 f}{d\eta^2} = 0$$

$$\delta \Rightarrow u/u_\infty = 0.99 \Rightarrow \eta = 5.0$$

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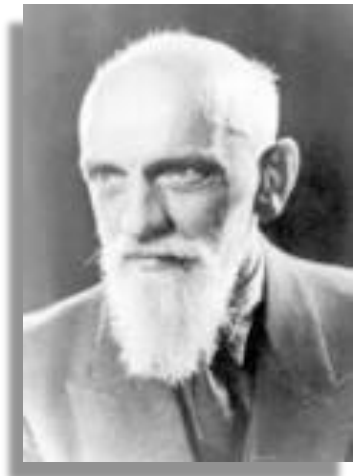
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$$\eta = y \cdot \sqrt{\frac{u_\infty}{xv}} \Rightarrow \delta = 5.0 \cdot \sqrt{\frac{xv}{u_\infty}}$$

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$$\delta \Rightarrow u/u_\infty = 0.99 \Rightarrow \eta = 5.0$$

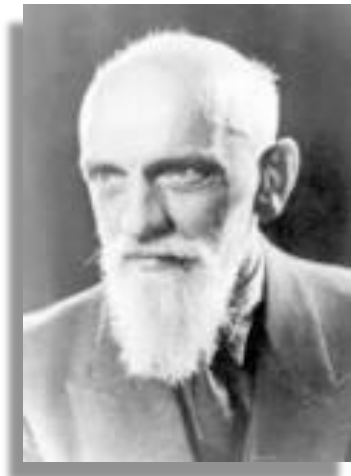
$$\eta = y \cdot \sqrt{\frac{u_\infty}{x\nu}} \Rightarrow \delta = 5.0 \cdot \sqrt{\frac{x\nu}{u_\infty}}$$



$$\delta = \frac{5.0 \cdot x}{\sqrt{Re_x}}$$

$$Re = \frac{\rho u_\infty x}{\mu}$$

η	f	$\frac{df}{d\eta} = \frac{u}{u_\infty}$	$\frac{d^2 f}{d\eta^2}$
0	0	0	0.332
0.5	0.042	0.166	0.331
1.0	0.166	0.330	0.323
1.5	0.370	0.487	0.303
2.0	0.650	0.630	0.267
2.5	0.996	0.751	0.217
3.0	1.397	0.846	0.161
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4.0	2.306	0.956	0.064
4.5	2.790	0.980	0.034
5.0	3.283	0.992	0.016
5.5	3.781	0.997	0.007
6.0	4.280	0.999	0.002
∞	∞	1	0



Paul R.H. Blasius
(1883–1970)

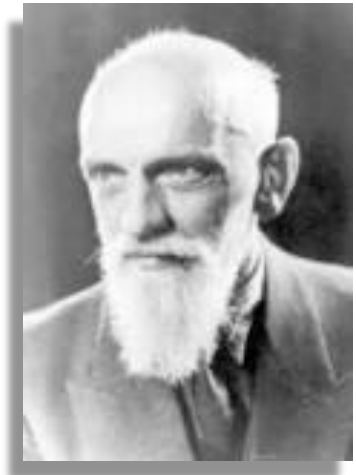
Solução de Blasius (1908)... **tensões de cisalhamento**

$$2 \frac{d^3 f}{d\eta^3} + f \frac{d^2 f}{d\eta^2} = 0$$

$$\tau_x = \mu \left. \frac{\partial u}{\partial y} \right|_{y=0} = \mu U_\infty \sqrt{\frac{U_\infty}{\nu x}} \left. \frac{d^2 f}{d\eta^2} \right|_{\eta=0}$$

$$\tau_x = 0.332 \frac{\rho U_\infty^2}{\sqrt{Re_x}}$$

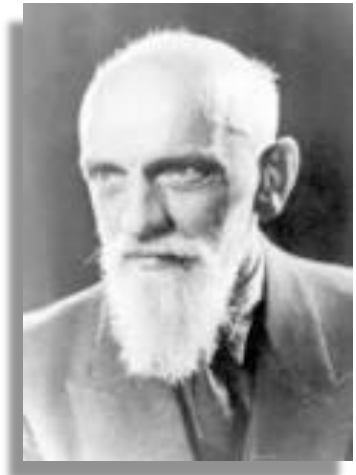
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∞	∞	1	0



Paul R.H. Blasius
(1883–1970)

Solução de Blasius (1908)... **c. limite térmica**

$$U \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \frac{k}{\rho C_p} \frac{\partial^2 T}{\partial y^2}$$



Paul R.H. Blasius
(1883–1970)

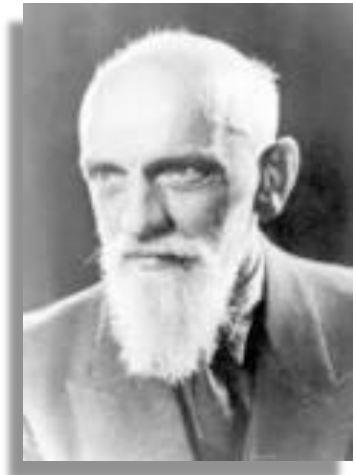
$$\psi = U_\infty \cdot \sqrt{\frac{x \cdot \mu / \rho}{U_\infty}} \cdot f(\eta)$$

Solução de Blasius (1908)... **c. limite térmica**

$$\psi(x, y) \stackrel{\text{def}}{=} \begin{cases} u = +\frac{\partial \psi}{\partial y} \\ v = -\frac{\partial \psi}{\partial x} \end{cases}$$



$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \frac{k}{\rho C_p} \frac{\partial^2 T}{\partial y^2}$$



Paul R.H. Blasius
(1883–1970)

$$\psi = U_\infty \cdot \sqrt{\frac{x \cdot \mu / \rho}{U_\infty}} \cdot f(\eta)$$

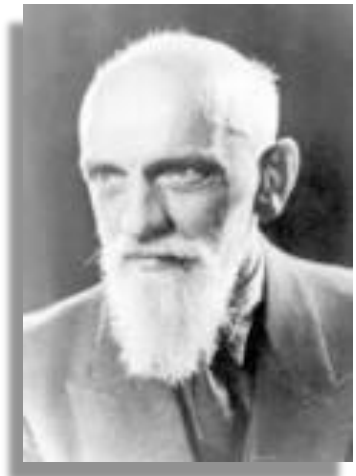
Solução de Blasius (1908)... **c. limite térmica**

$$\psi(x, y) \stackrel{\text{def}}{=} \begin{cases} u = + \frac{\partial \psi}{\partial y} \\ v = - \frac{\partial \psi}{\partial x} \end{cases}$$



$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \frac{k}{\rho C_p} \frac{\partial^2 T}{\partial y^2}$$

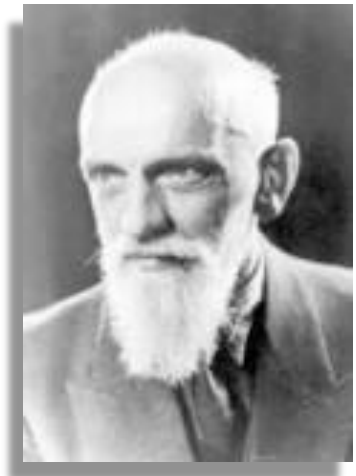
$$\theta(x, y) \stackrel{\text{def}}{=} \frac{T(x, y) - T_s}{T_\infty - T_s} \leftarrow$$



Paul R.H. Blasius
(1883–1970)

$$\psi = U_\infty \cdot \sqrt{\frac{x \cdot \mu / \rho}{U_\infty}} \cdot f(\eta)$$

Solução de Blasius (1908)... **c. limite térmica**



Paul R.H. Blasius
(1883–1970)

$$\psi(x, y) \stackrel{\text{def}}{=} \begin{cases} u = + \frac{\partial \psi}{\partial y} \\ v = - \frac{\partial \psi}{\partial x} \end{cases}$$



$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \frac{k}{\rho C_p} \frac{\partial^2 T}{\partial y^2}$$

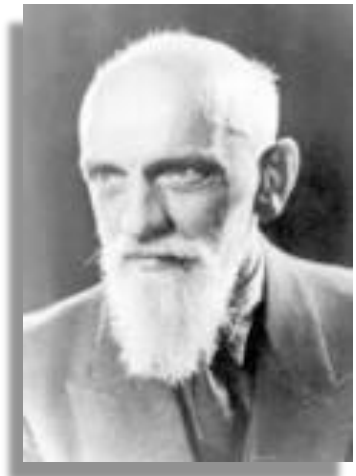
$$\theta(x, y) \stackrel{\text{def}}{=} \frac{T(x, y) - T_s}{T_\infty - T_s}$$



$$\psi = U_\infty \cdot \sqrt{\frac{x \cdot \mu / \rho}{U_\infty}} \cdot f(\eta)$$

$$U_\infty \frac{df}{d\eta} \frac{\partial \theta}{\partial \eta} \frac{\partial \eta}{\partial x} + \frac{1}{2} \sqrt{\frac{U_\infty \nu}{x}} \left(\eta \frac{df}{d\eta} - f \right) \frac{\partial \theta}{\partial \eta} \frac{\partial \eta}{\partial y} = \frac{k}{\rho C_p} \frac{d^2 \theta}{d\eta^2} \left(\frac{\partial \eta}{\partial y} \right)^2$$

Solução de Blasius (1908)... **c. limite térmica**



Paul R.H. Blasius
(1883–1970)

$$u_{\infty} \frac{df}{d\eta} \frac{\partial \theta}{\partial \eta} \frac{\partial \eta}{\partial x} + \frac{1}{2} \sqrt{\frac{u_{\infty} \nu}{x}} \left(\eta \frac{df}{d\eta} - f \right) \frac{\partial \theta}{\partial \eta} \frac{\partial \eta}{\partial y} = \frac{k}{\rho C_p} \frac{d^2 \theta}{d\eta^2} \left(\frac{\partial \eta}{\partial y} \right)^2$$

⋮

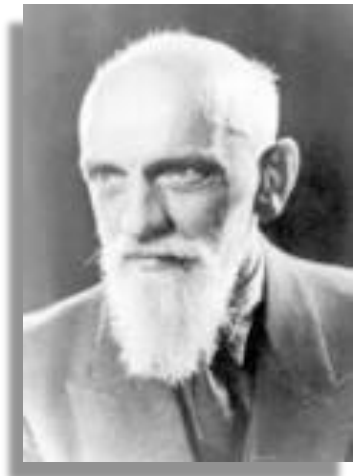
$$Pr = \frac{\mu}{k/C_p} \Rightarrow$$

$$2 \frac{d^2 \theta}{d\eta^2} + Pr \cdot f \frac{d\theta}{d\eta} = 0$$

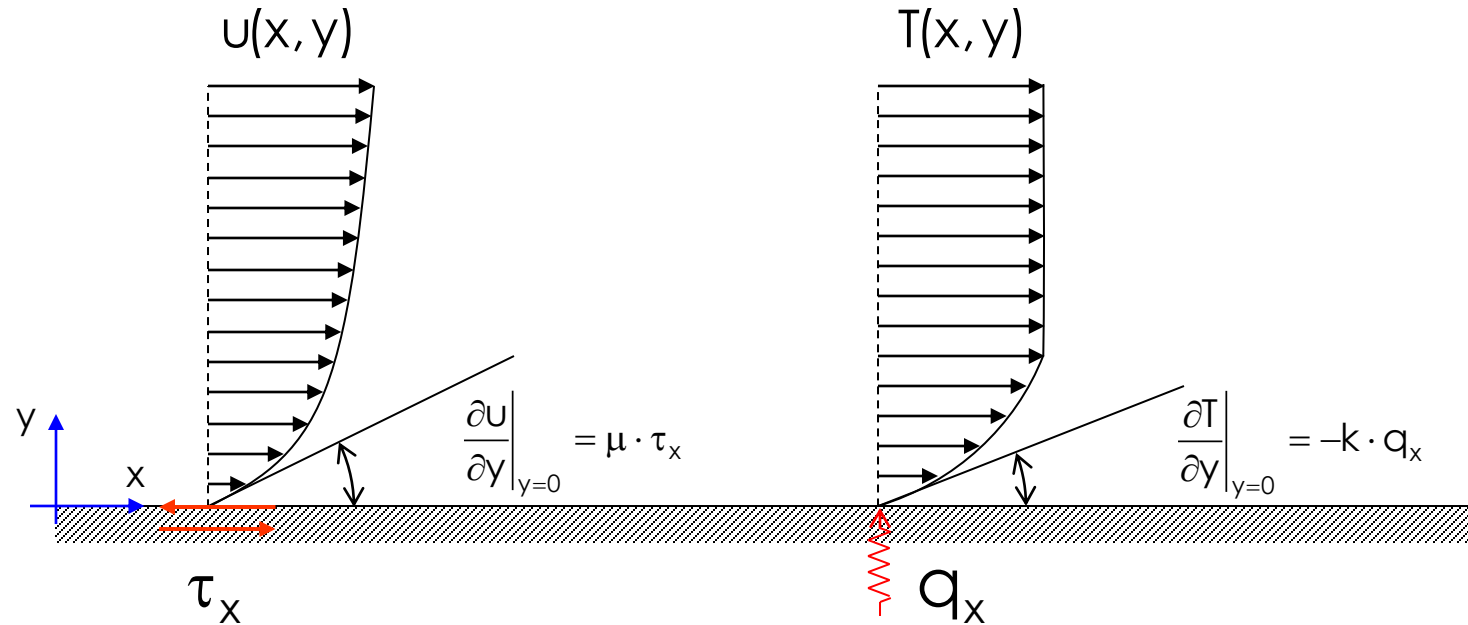
$$\theta(0) = 0 \quad e \quad \theta(\infty) = 1$$

η	f	$\frac{df}{d\eta} = \frac{u}{u_{\infty}}$	$\frac{d^2 f}{d\eta^2}$
0	0	0	0.332
0.5	0.042	0.166	0.331
1.0	0.166	0.330	0.323
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5.0	3.283	0.992	0.016
5.5	3.781	0.997	0.007
6.0	4.280	0.999	0.002
∞	∞	1	0

Solução de Blasius (1908)... c. limite térmica



Paul R.H. Blasius
(1883–1970)



$$\tau_x = 0.332 \frac{\rho U_\infty^2}{\sqrt{Re_x}}$$

$$-\frac{q_x}{k} = 0.332 \cdot Pr^{1/3} (T_\infty - T_s) \sqrt{\frac{U_\infty}{\nu x}}$$

$$\delta_{FD} = \frac{5.0 \cdot x}{\sqrt{Re_x}}$$

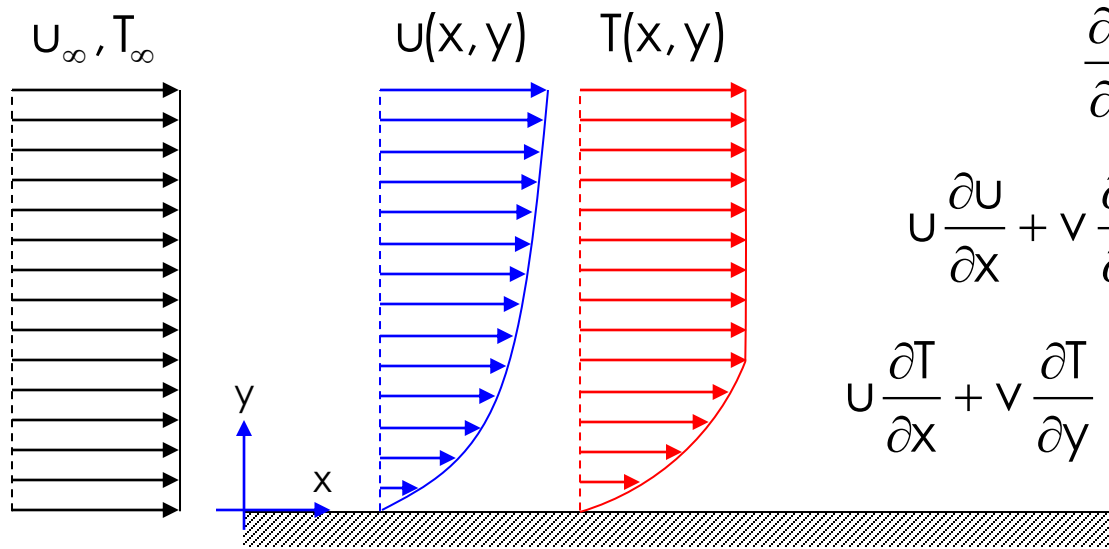
$$\delta_{TM} = \frac{5.0 \cdot x}{Pr^{1/3} \sqrt{Re_x}}$$

η	f	$\frac{df}{d\eta} = \frac{u}{U_\infty}$	$\frac{d^2f}{d\eta^2}$
0	0	0	0.332
0.5	0.042	0.166	0.331
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∞	∞	1	0

ADIMENSIONALIZAÇÃO DAS EQUAÇÕES GOVERNANTES



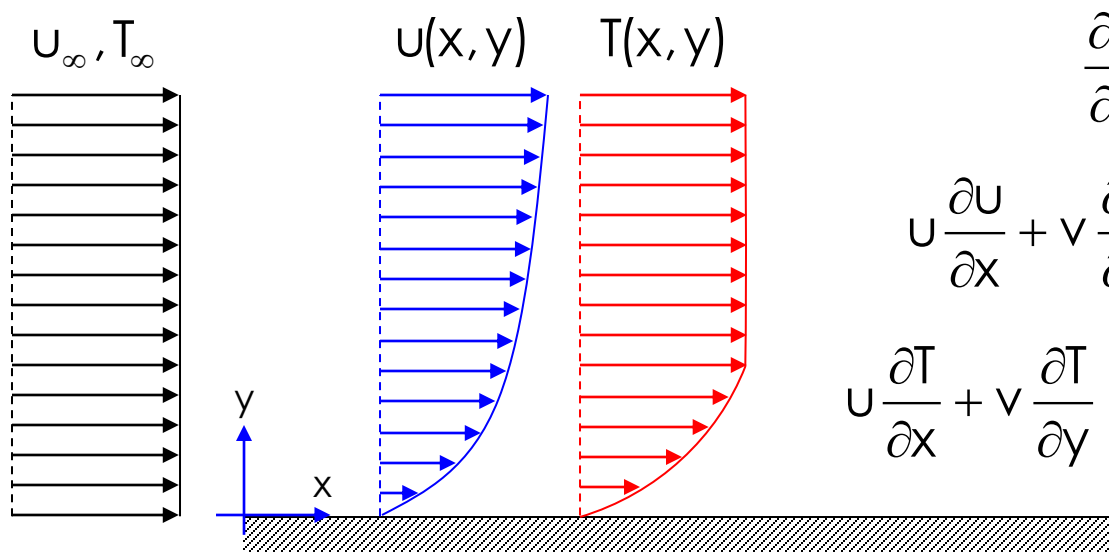
Adimensionalização das equações governantes...



$$\left. \begin{aligned}
 \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} &= 0 \\
 u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} &= \frac{\mu}{\rho} \frac{\partial^2 u}{\partial y^2} \\
 u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} &= \frac{k}{\rho C_p} \frac{\partial^2 T}{\partial y^2}
 \end{aligned} \right\} \begin{aligned}
 x^* &= \frac{x}{L} & y^* &= \frac{y}{L} \\
 U^* &= \frac{U}{U_\infty} & V^* &= \frac{V}{U_\infty} & P^* &= \frac{P}{\rho U_\infty^2} \\
 T^* &= \frac{T - T_2}{T_\infty - T_s}
 \end{aligned}$$

$$\begin{aligned}
 \frac{\partial u}{\partial x} &= \frac{U_\infty}{L} \frac{\partial u^*}{\partial x^*} \\
 \frac{\partial v}{\partial y} &= \frac{U_\infty}{L} \frac{\partial v^*}{\partial y^*}
 \end{aligned}
 \Rightarrow \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \rightarrow \frac{\partial u^*}{\partial x^*} + \frac{\partial v^*}{\partial y^*} = 0$$

Adimensionalização das equações governantes...



$$\left. \begin{aligned}
 \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} &= 0 \\
 u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} &= \frac{\mu}{\rho} \frac{\partial^2 u}{\partial y^2} \\
 u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} &= \frac{k}{\rho C_p} \frac{\partial^2 T}{\partial y^2}
 \end{aligned} \right\} \begin{aligned}
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 U^* &= \frac{u}{U_\infty} & v^* &= \frac{v}{U_\infty} & P^* &= \frac{P}{\rho U_\infty^2} \\
 T^* &= \frac{T - T_2}{T_\infty - T_s}
 \end{aligned}$$

$$\begin{aligned}
 \frac{\partial u}{\partial x} &= \frac{U_\infty}{L} \frac{\partial U^*}{\partial x^*} \\
 \frac{\partial v}{\partial y} &= \frac{U_\infty}{L} \frac{\partial v^*}{\partial y^*}
 \end{aligned}
 \Rightarrow
 u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \frac{\mu}{\rho} \frac{\partial^2 u}{\partial y^2}
 \rightarrow
 U^* \frac{\partial U^*}{\partial x^*} + v^* \frac{\partial U^*}{\partial y^*} = \frac{1}{\text{Re}} \frac{\partial^2 U^*}{\partial y^{*2}}$$

Adimensionalização das equações governantes...

$$\begin{aligned}\frac{\partial u}{\partial x} &= \frac{U_\infty}{L} \frac{\partial u^*}{\partial x^*} \\ \frac{\partial v}{\partial y} &= \frac{U_\infty}{L} \frac{\partial v^*}{\partial y^*} \\ \frac{\partial P}{\partial x} &= \frac{\rho U_\infty^2}{L} \frac{\partial P^*}{\partial x^*} \\ \frac{\partial P}{\partial y} &= \frac{\rho U_\infty^2}{L} \frac{\partial P^*}{\partial y^*}\end{aligned}$$



$$\frac{\partial \rho}{\partial t} + \vec{\nabla} \cdot (\rho \vec{U}) = 0$$

$$\rho \cdot \left(\frac{\partial \vec{U}}{\partial t} + \vec{U} \cdot \vec{\nabla} \vec{U} \right) = -\vec{\nabla} P + \mu \nabla^2 \vec{U} + \sum F_k$$

$$\rho C_p \left(\frac{\partial T}{\partial t} + \vec{U} \cdot \vec{\nabla} T \right) = \vec{\nabla} \cdot (k \vec{\nabla} T)$$

Adimensionalização das equações governantes...

$$\frac{\partial u}{\partial x} = \frac{u_\infty}{L} \frac{\partial u^*}{\partial x^*}$$

$$\frac{\partial v}{\partial y} = \frac{u_\infty}{L} \frac{\partial v^*}{\partial y^*}$$

$$\frac{\partial P}{\partial x} = \frac{\rho u_\infty^2}{L} \frac{\partial P^*}{\partial x^*}$$

$$\frac{\partial P}{\partial y} = \frac{\rho u_\infty^2}{L} \frac{\partial P^*}{\partial y^*}$$



$$\frac{\partial \rho^*}{\partial t^*} + \vec{\nabla} \cdot (\rho^* \vec{U}^*) = 0$$

$$\rho^* \cdot \left(\frac{\partial \vec{U}^*}{\partial t^*} + \vec{U}^* \cdot \vec{\nabla} \vec{U}^* \right) = -\vec{\nabla} P^* + \frac{1}{Re} \nabla^2 \vec{U}^* + \sum \frac{1}{R_k} F_k^*$$

$$\left(\frac{\partial T^*}{\partial t^*} + \vec{U}^* \cdot \vec{\nabla} T^* \right) = \frac{1}{Re \cdot Pr} \vec{\nabla} \cdot \vec{\nabla} T^*$$

$$Re = \frac{\rho u_0 D}{\mu} \rightarrow \frac{\text{inércia}}{\text{d.viscosa}}$$

$$Pr = \frac{\mu}{k / C_p} \rightarrow \frac{\text{d.viscosa}}{\text{d.térmica}}$$

As equações governam o fenômeno via leis de conservação. Os números adimensionais definem o comportamento na escala do problema modelado...

Adimensionalização das equações governantes...



Mesmas equações adimensionais de balanço de massa, q. de movimento e energia porém, com diferentes números adimensionais

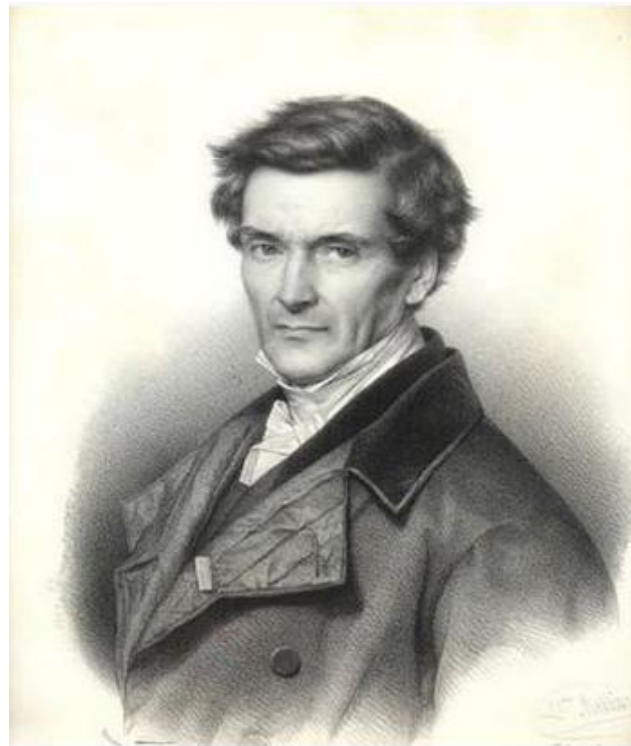
Ω = rotação planetária
 φ = latitude

$$Re = \frac{\rho U_0 D}{\mu} \quad Pr = \frac{C_p \mu}{k} \quad Eu = \frac{P_0}{\rho U_0^2} \quad Fr = \frac{U_0}{\sqrt{gD}} \quad Ec = \frac{U_0^2}{C_p (T_s - T_\infty)} \quad Ro = \frac{U/L}{2\Omega \sin \varphi}$$

Por que os furacões giram no sentido anti-horário no hemisfério norte e no sentido horário no hemisfério sul ???



Por que os furacões giram no sentido anti-horário no hemisfério norte e no sentido horário no hemisfério sul ???



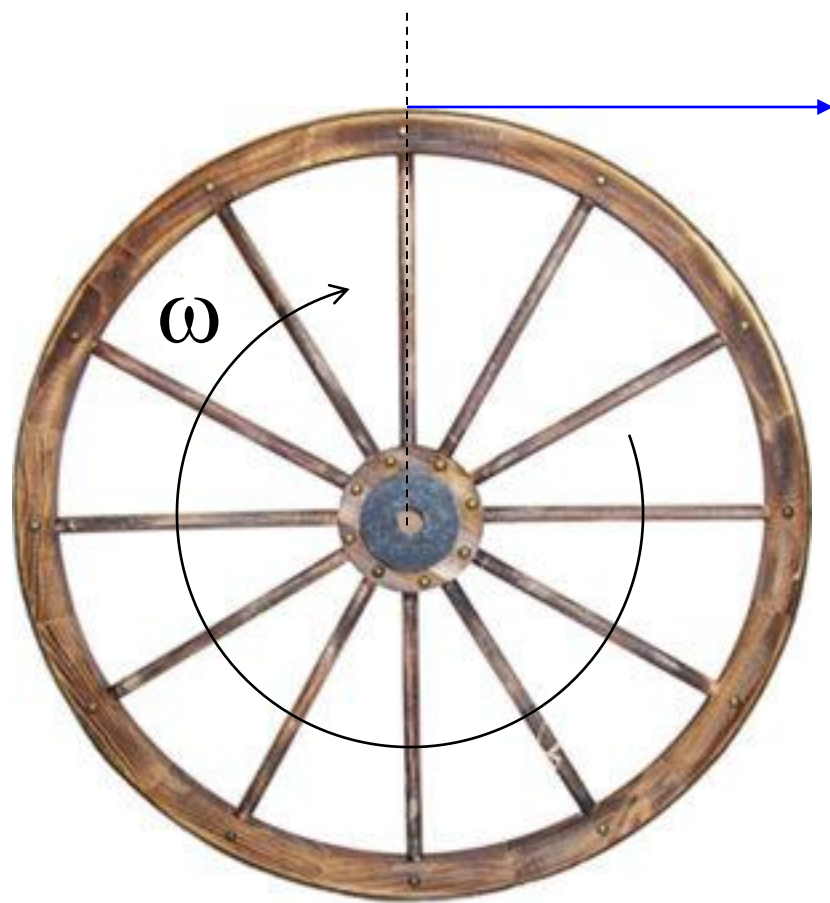
Gaspard-Gustave de Coriolis



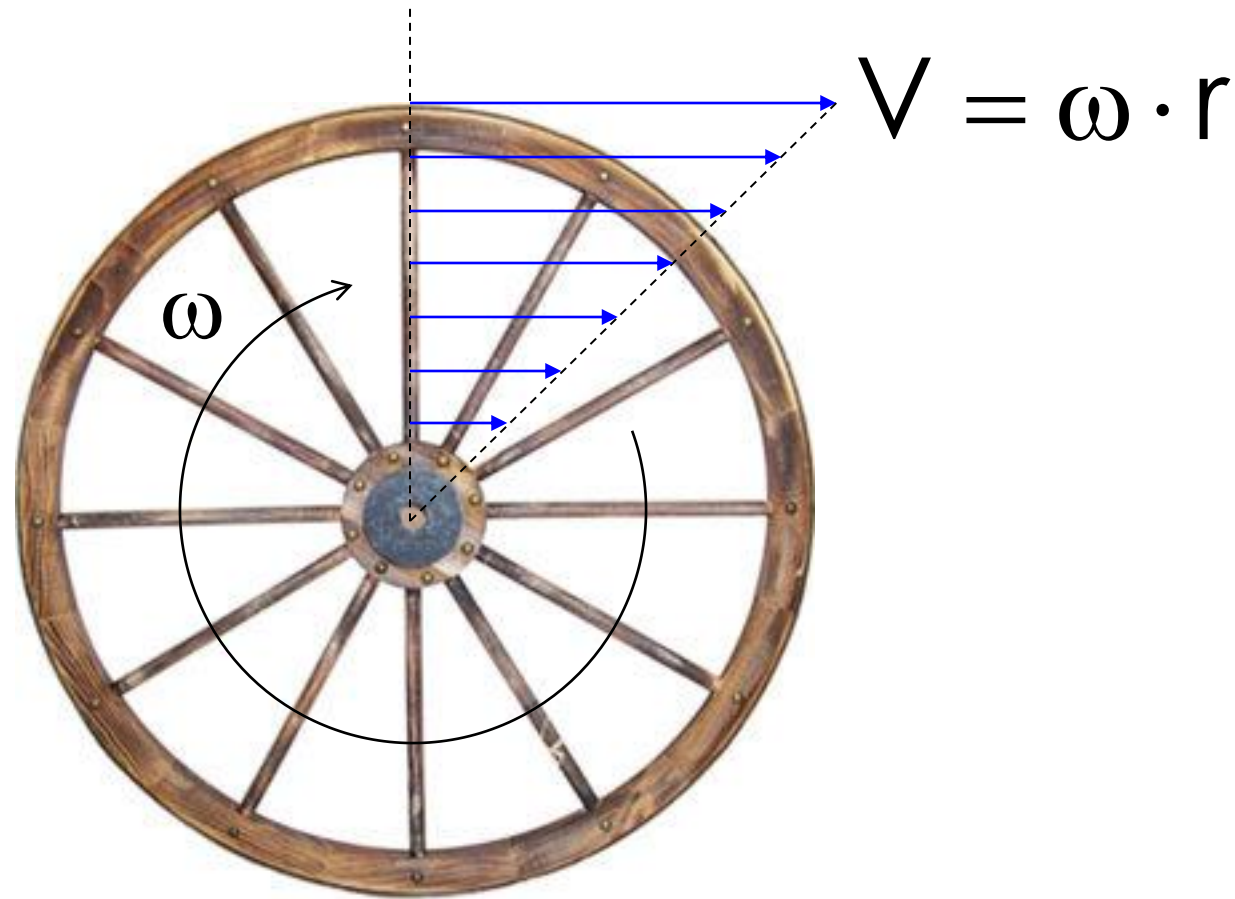
Carl-Gustaf Rossby

Fenômenos atmosféricos de grande escala...

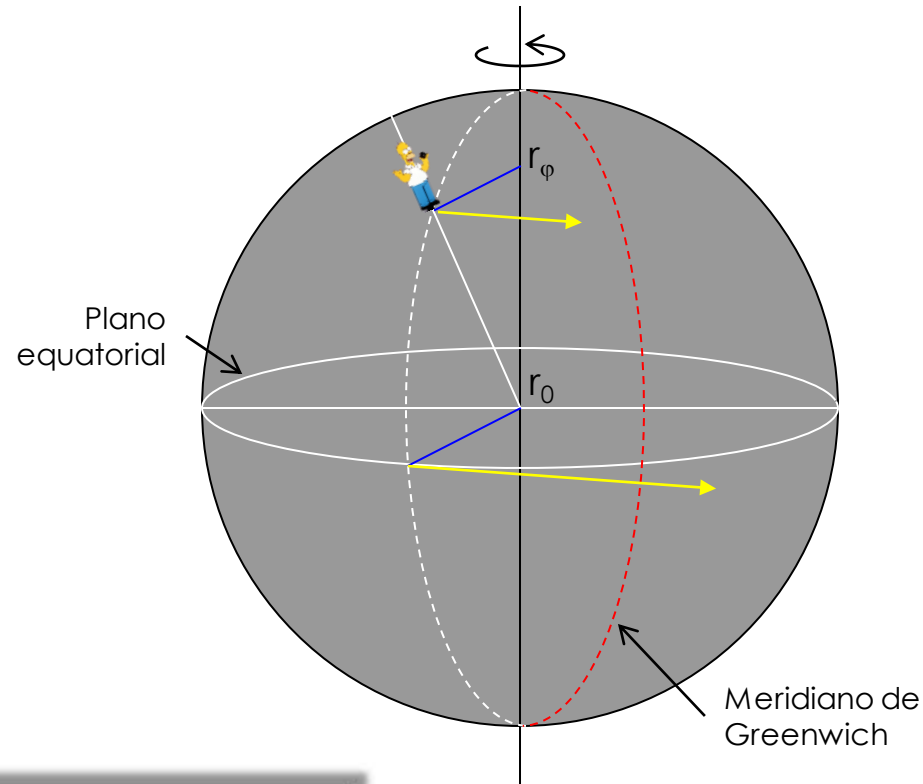
Por que os furacões giram no sentido anti-horário no hemisfério norte e no sentido horário no hemisfério sul ???



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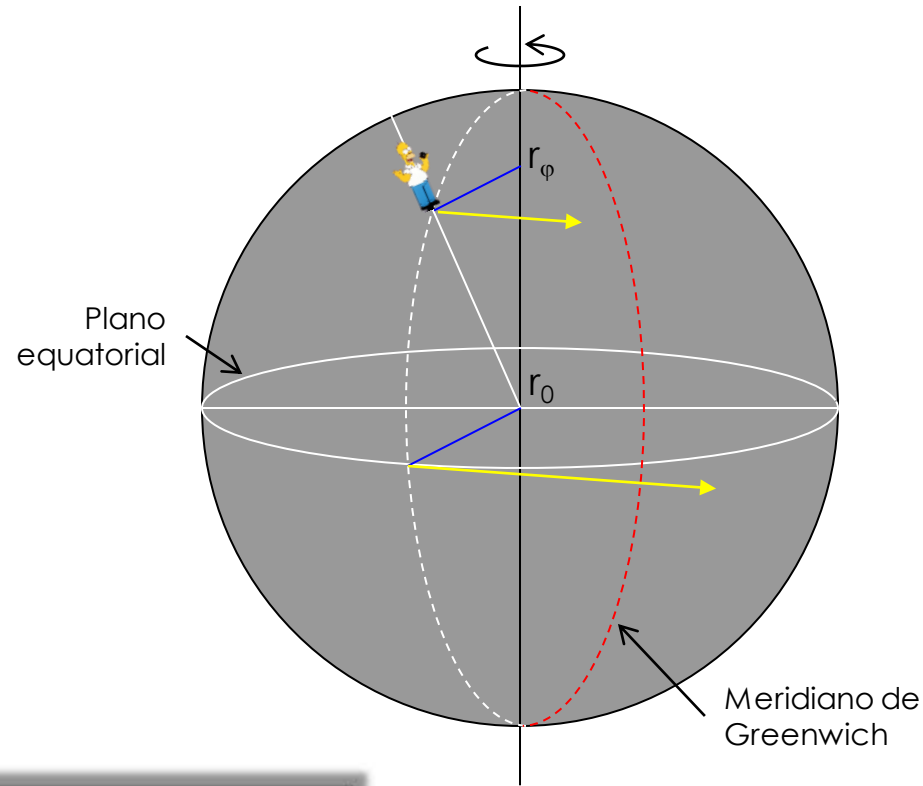


Por que os furacões giram no sentido anti-horário no hemisfério norte e no sentido horário no hemisfério sul ???

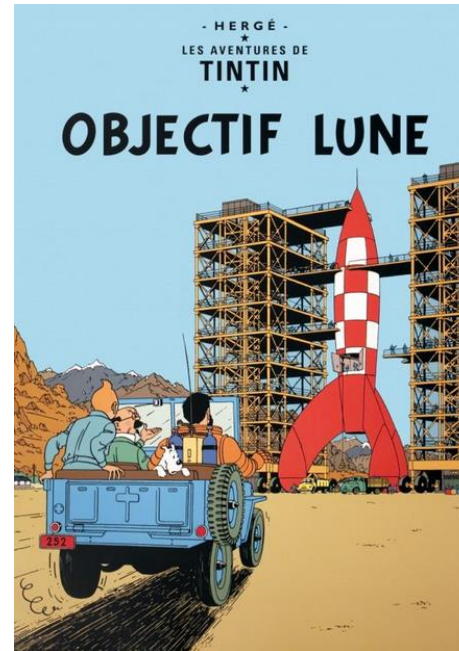


A velocidade tangencial é máxima ao longo do equador e decresce na medida em que a latitude aumenta...

Por que os furacões giram no sentido anti-horário no hemisfério norte e no sentido horário no hemisfério sul ???



A velocidade tangencial é máxima ao longo do equador e decresce na medida em que a latitude aumenta... (“vitesse de libération...”)





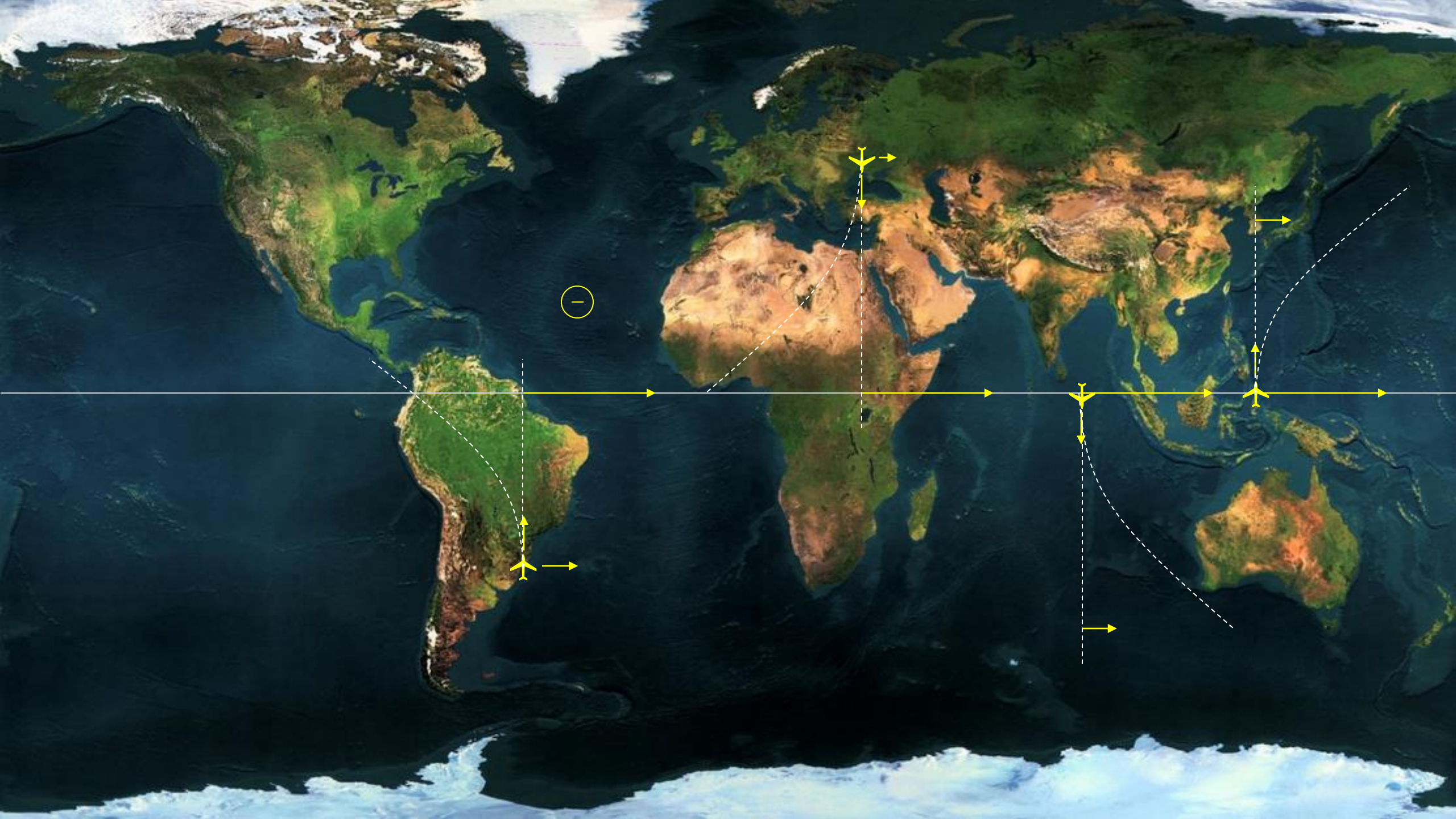


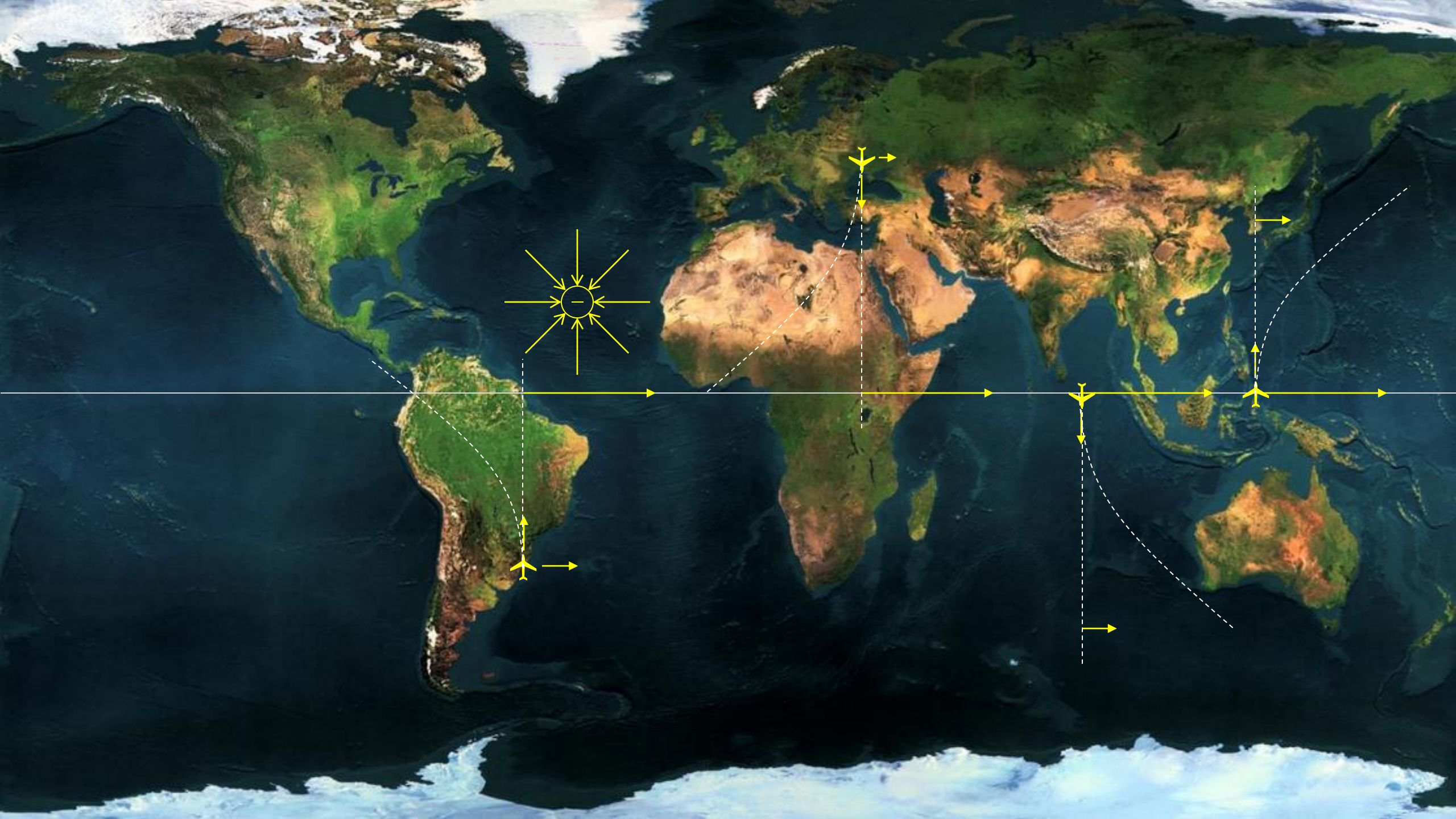


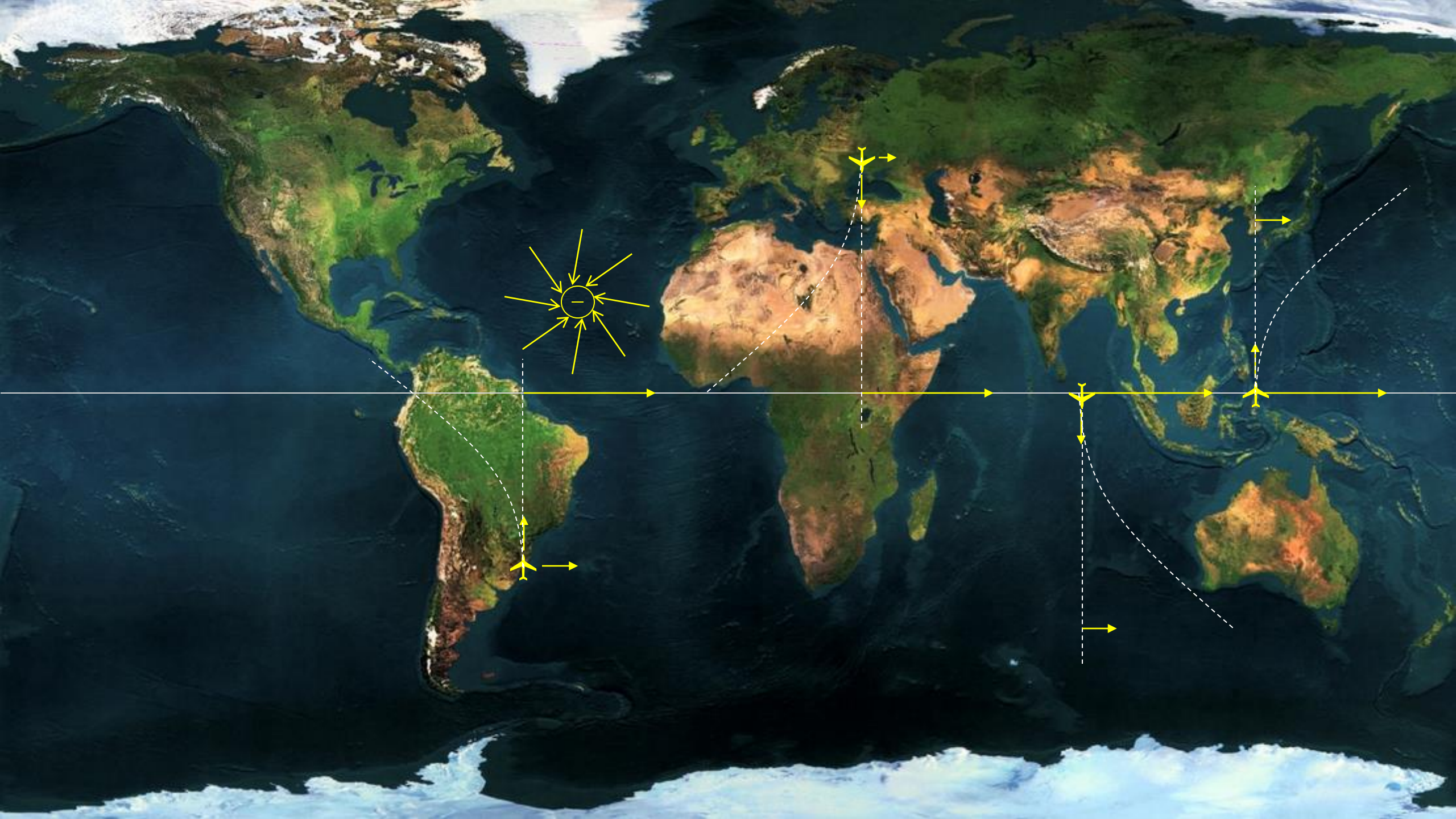


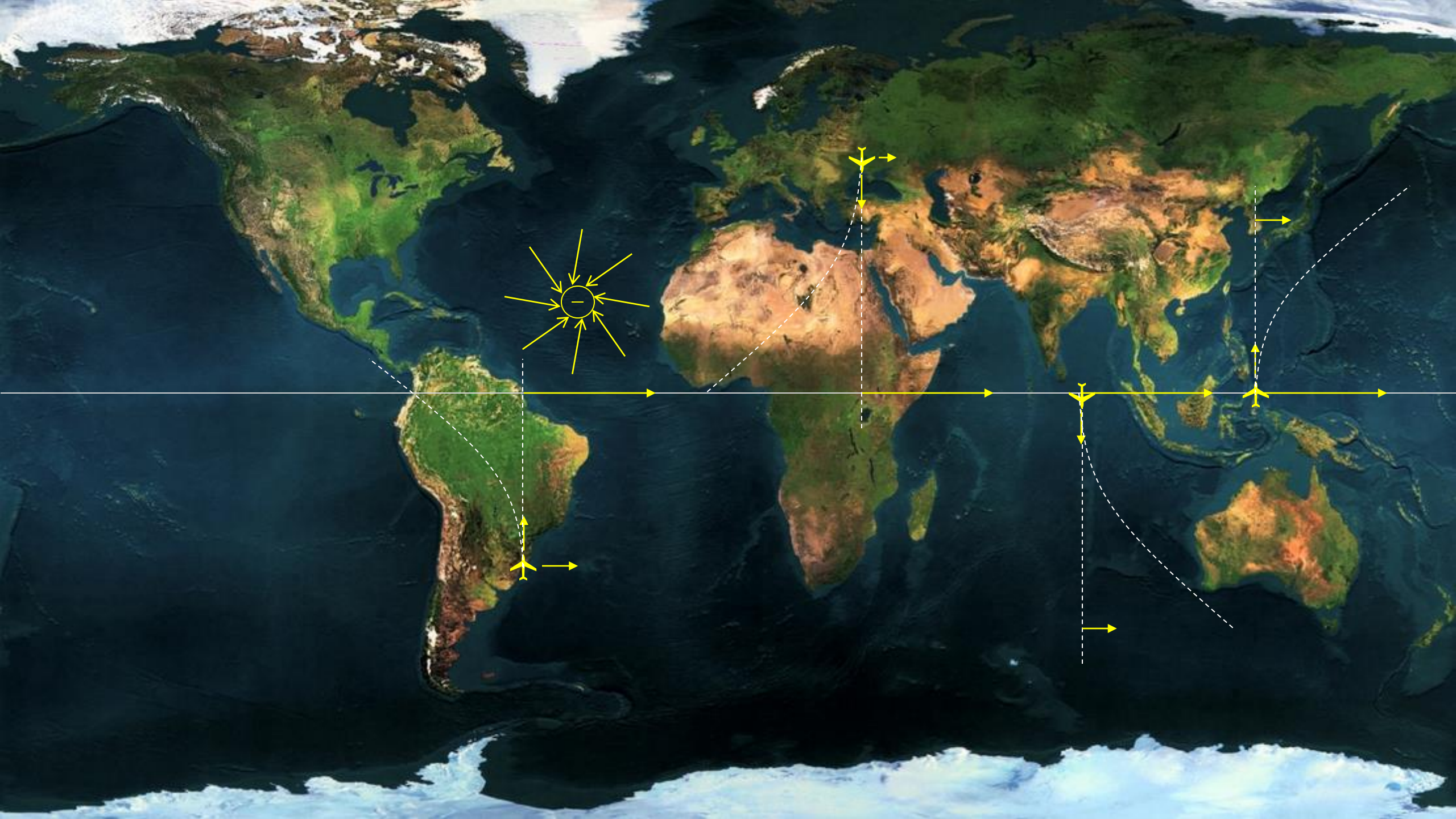


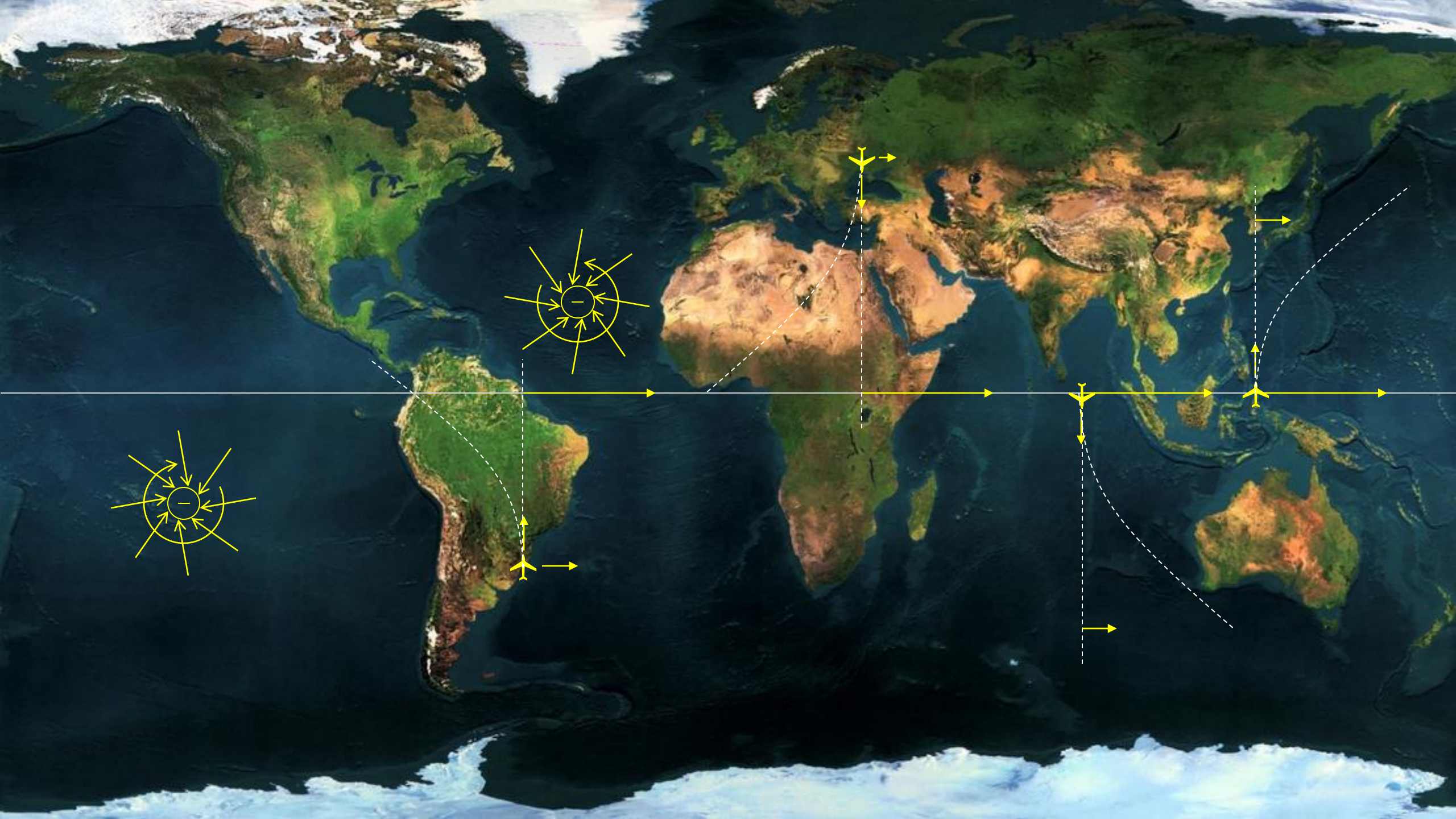


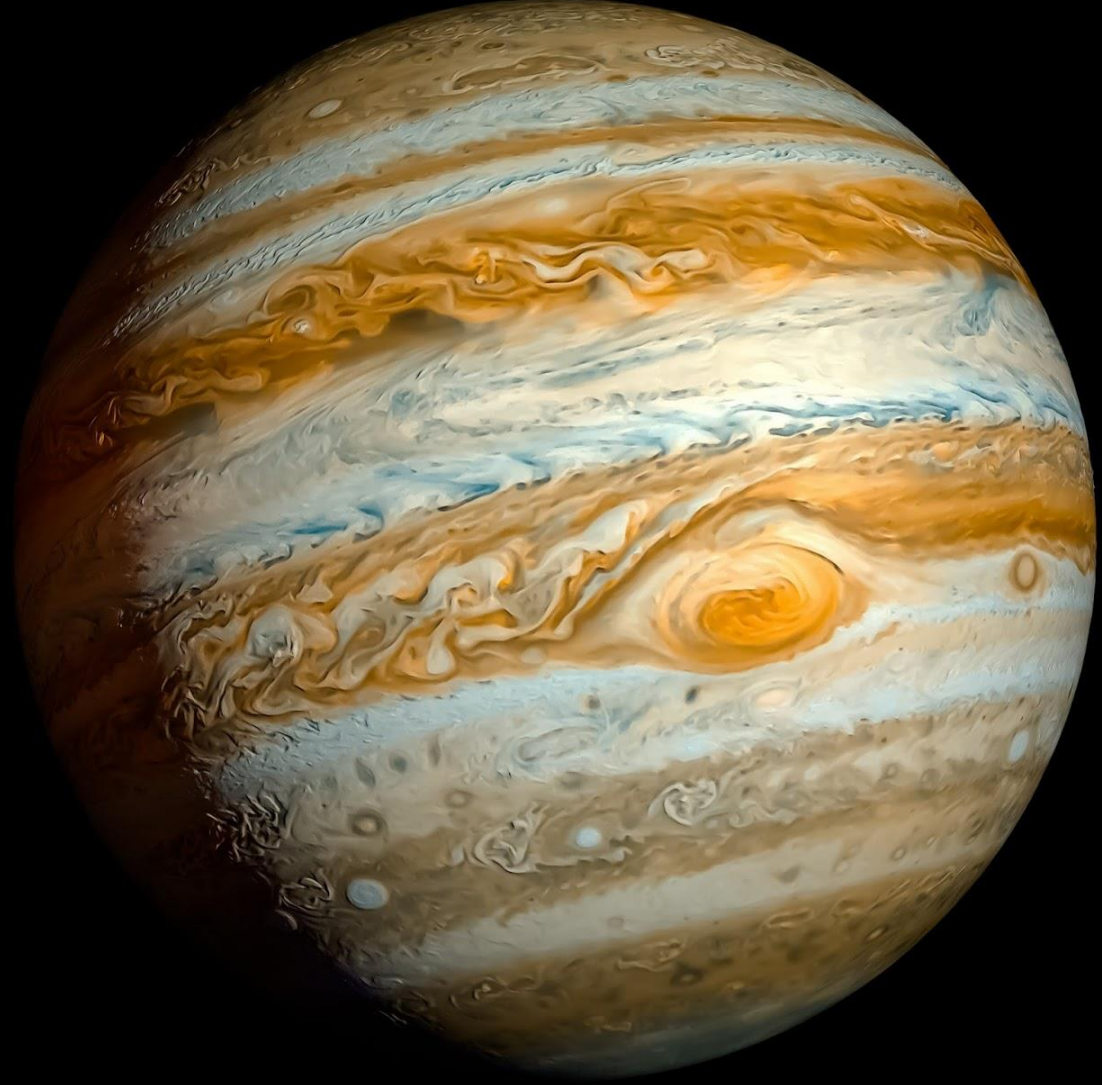












Le pôle sud de Jupiter, photographié
par la sonde Cassini...
<https://saturn.jpl.nasa.gov>





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