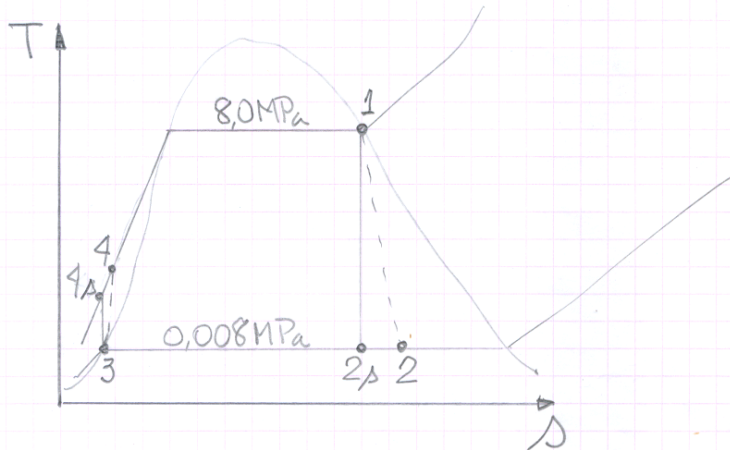


EXERCÍCIOS

CICLO VAPOR

① Propriedades Termodinâmicas

Seção	T(°C)	p(MPa)	h(kJ/kg)
1	295,1	8,0	2.758,0
2	41,5	0,008	1939,3
3	41,5	0,008	173,9
4	42,1	8,0	183,4



(E1)

Ex. 1

Caracterização dos Estados:

* $h_1 = 2758 \text{ kJ.kg}^{-1}$; $s_1 = 5,7432 \text{ kJ.kg}^{-1}\text{K}^{-1}$

$$\eta_t = \frac{h_1 - h_2}{h_1 - h_{2s}} \rightarrow h_2 = h_1 - \eta_t (h_1 - h_{2s})$$

$$h_2 = 2758 - 0,85(2758 - 1794,8)$$

* $h_2 = 1939,3 \text{ kJ.kg}^{-1}$

* $h_3 = 173,9 \text{ kJ.kg}^{-1}$

* $h_4 = h_3 + \dot{W}_B / \dot{m}$ com $\eta_B = \frac{(\dot{W}_B / \dot{m})_s}{(\dot{W}_B / \dot{m})}$

$$(\dot{W}_B)_s = \dot{m} [v_3 (p_4 - p_3)]$$

$$(\dot{W}_B / \dot{m})_s = 8,06 \text{ kJ.kg}^{-1} \rightarrow (\dot{W}_B / \dot{m}) = \frac{8,06}{\eta_B} = \frac{9,48 \text{ kJ}}{\text{kg}}$$

$$\therefore h_4 = 183,36 \text{ kJ.kg}^{-1}$$

a) $\dot{W}_{\text{útil}} = \dot{W}_t - \dot{W}_B = \dot{m} [(h_1 - h_2) - (h_4 - h_3)]$

$$\eta = \frac{(h_1 - h_2) - (h_4 - h_3)}{h_1 - h_4} = 0,314 \text{ (31,4\%)}$$

$$b) \dot{m}_v = \frac{W_{\text{ciclo}}}{(h_1 - h_2) - (h_4 - h_3)} = 4,449 \cdot 10^5 \text{ kg/h}$$

$$c) \dot{\Phi}_{\text{cald}} = \dot{m}_v (h_1 - h_4) = 318,2 \text{ MW}$$

$$d) \dot{\Phi}_{\text{cond}} = \dot{m}_v (h_2 - h_3) = 218,2 \text{ MW}$$

$$e) \dot{m}_{\text{água}} = \frac{\dot{\Phi}_{\text{cond}}}{(h_{\text{ap}} - h_{\text{ae}})} = 9,39 \cdot 10^6 \text{ kg/h}$$

com $h_{\text{as}} = 146,68 \text{ kJ/kg}$
 $h_{\text{ae}} = 62,99 \text{ kJ/kg}$

Ciclo Ideal

$$\eta = 0,371$$

$$\dot{m}_v = 3,77 \cdot 10^5 \text{ kg/h}$$

$$\dot{\Phi}_{\text{cald}} = 269,8 \text{ MW}$$

$$\dot{\Phi}_{\text{cond}} = 169,8 \text{ MW}$$

$$\dot{m}_{\text{água}} = 7,3 \cdot 10^6 \text{ kg/h}$$

Exercícios

② Determinação dos Estados Termodinâmicos

$$\textcircled{1} \begin{cases} h_1 = 3348,4 \text{ kJ.kg}^{-1} \\ s_1 = 6,6586 \text{ kJ.kg}^{-1}\text{K}^{-1} \end{cases}$$

$$\textcircled{2} \begin{cases} p_2 = 0,7 \text{ MPa} \quad \text{e} \quad s_2 = s_1 \end{cases}$$

$$x_2 = \frac{s_2 - s_e}{s_g - s_e} = \frac{6,6586 - 1,9922}{6,708 - 1,9922} = 0,9895$$

$$\begin{aligned} h_2 &= h_e + x_2(h_g - h_e) = 697,22 + 0,9895 \cdot 2066,3 \\ h_2 &= 2741,8 \text{ kJ.kg}^{-1} \end{aligned}$$

$$\textcircled{3} \begin{cases} p_3 = 0,7 \text{ MPa} \quad \text{e} \quad T_3 = 440^\circ\text{C} \\ h_3 = 3353,3 \text{ kJ.kg}^{-1} \\ s_3 = 7,7571 \text{ kJ.kg}^{-1}\text{K}^{-1} \end{cases}$$

$$\textcircled{4} \begin{cases} p_4 = 0,008 \text{ MPa} \quad \text{e} \quad s_4 = s_3 \end{cases}$$

$$x_4 = \frac{s_4 - s_e}{s_g - s_e} = \frac{7,7571 - 0,5926}{8,2287 - 0,5926} = 0,9382$$

$$h_4 = h_e + x_4(h_g - h_e) = 2428,5 \text{ kJ.kg}^{-1}$$

$$\textcircled{5} \left\{ h_5 = 173,88 \text{ kJ.kg}^{-1} \text{ (liquido saturad)} \right.$$

$$\textcircled{6} \left\{ \begin{array}{l} h_6 = h_5 + v_5 (p_6 - p_5) \\ h_6 = 181,94 \text{ kJ.kg}^{-1} \end{array} \right.$$

$$\rightarrow a) \underline{W_{\text{eq}}} = W_{12} + W_{34} - W_{65}$$

$$\frac{\eta}{\%} = \frac{(h_1 - h_2) + (h_3 - h_4) - (h_6 - h_5)}{(h_1 - h_6) + (h_3 - h_2)} = \underline{0,403}$$

$$\rightarrow b) \underline{\dot{m}} = \frac{W_{\text{eq}}}{(h_1 - h_2) + (h_3 - h_4) - (h_6 - h_5)} = \frac{65,64 \text{ kJ/s}}{2,93 \cdot 10^5 \text{ J/kg}} = \underline{0,224 \text{ kg/s}}$$

$$\rightarrow c) \underline{\dot{Q}_{\text{cd}}} = \dot{m} (h_4 - h_5) = \underline{148 \text{ MW}}$$

Exercício 3

a) Determinação das propriedades

$$h_1 = 3348,4 \text{ kJ/kg}$$

$$h_2 = 2832,8 \text{ kJ/kg} ; p_2 = 6,8606 \text{ kJ/kg}\cdot\text{K}$$

$$h_4 = 173,9 \text{ kJ/kg}$$

$$h_3 = h_2 - \eta_t (h_2 - h_{3p}) \text{ com } p_{3p} = p_2$$

$$h_{3p} = 2146,3 \text{ kJ/kg} \Rightarrow h_3 = 2249,3 \text{ kJ/kg}$$

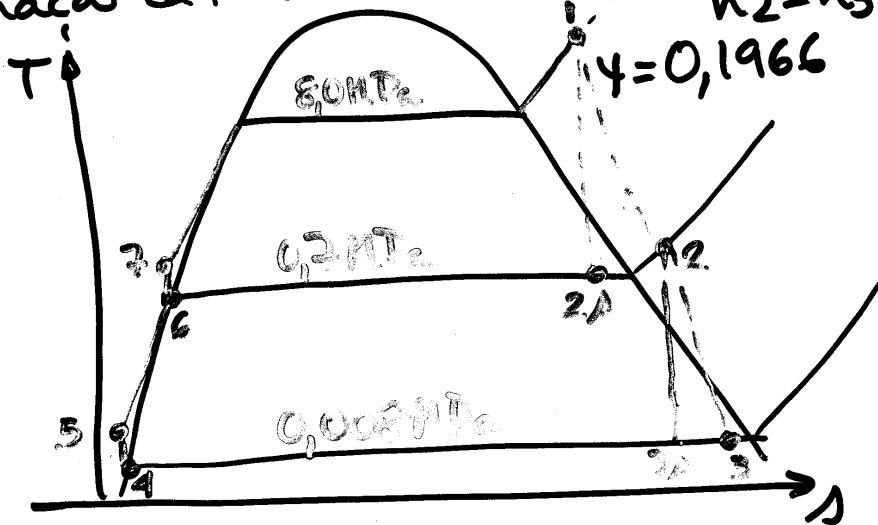
$$h_6 = 697,2 \text{ kJ/kg}$$

$$h_5 = h_4 + v_4(p_5 - p_4) = 179,6 \text{ kJ/kg}$$

$$h_7 = h_6 + v_6(p_7 - p_6) = 705,3 \text{ kJ/kg}$$

* fração de vapor extraída $y = \frac{h_6 - h_5}{h_2 - h_5}$

$$y = 0,1966$$



$$b) \frac{\dot{W}_t}{\dot{m}_1} = (h_1 - h_2) + (1-y)(h_2 - h_3) = 984,4 \text{ kJ/kg}$$

$$\frac{\dot{W}_b}{\dot{m}_1} = (h_7 - h_6) + (1-y)(h_5 - h_4) = 8,7 \text{ kJ/kg} \quad \leftarrow \text{"valor em módulo"}$$

$$\frac{\dot{Q}}{\dot{m}_1} = h_1 - h_7 = 2643,1 \text{ kJ/kg}$$

$$\eta = \frac{\dot{W}_t/\dot{m}_1 - \dot{W}_b/\dot{m}_1}{\dot{Q}/\dot{m}_1} = 0,369$$

$$c) \dot{W}_e = \dot{W}_t - \dot{W}_b \Rightarrow \dot{m}_1 = 3,69 \cdot 10^5 \text{ kg/h}$$

11-
④ Determinação de entalpias específicas

$$h_4 = 3479 \text{ kJ/kg}$$

$$h_a = 2793 \text{ kJ/kg}; \quad h_{a'} = 693,3 \text{ kJ/kg}$$

$$h_b = 2487 \text{ kJ/kg}; \quad h_{b'} = 435,4 \text{ kJ/kg}$$

$$h_k = 2026 \text{ kJ/kg}; \quad h_1 = 110,5 \text{ kJ/kg}$$

a) Extração de Vapor

$$\alpha_1 = \frac{h_{a'} - h_{b'}}{h_a - h_{b'}} = 0,1093 \text{ kg/kg vapor}$$

$$\alpha_2 = \frac{(1 - \alpha_1)(h_{b'} - h_1)}{h_b - h_1} = 0,1220 \text{ kg/kg vapor}$$

b) Trabalho específico da Turbina

$$w_T = (h_4 - h_a) + (1 - \alpha_1)(h_a - h_b) + (1 - \alpha_1 - \alpha_2)(h_b - h_k)$$

ou

$$w_T = (h_4 - h_k) - \alpha_1(h_a - h_k) - \alpha_2(h_b - h_k)$$

$$w_T = 1313 \text{ kJ/kg vapor}$$

$$c) \eta_{Reg} = \frac{w_T}{h_4 - h_{a'}} = 0,471 \text{ (Desperando bombeamento)}$$

$$\eta = \frac{h_4 - h_k}{h_a - h_1} = 0,432 \Rightarrow \frac{\Delta \eta}{\eta} = 0,09$$

Ciclo com Regeneração

